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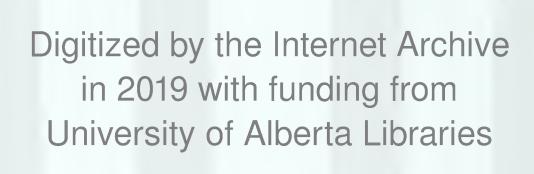
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THE UNIVERSITY OF ALBERTA

A MODEL STUDY OF AN ISOLATED NINE-SPOT

bу

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ABSTRACT

In analyzing secondary recovery projects, the fraction of the reservoir which is ultimately swept by the injected fluid is of paramount importance. Treatment of water flood behavior, and in particular areal sweep efficiency, can best be studied by scaled flow model experiments.

In the displacement of oil by water in these two-dimensional flow systems capillary forces exhibit considerable influence.

Laboratory results can only be utilized for field evaluations when capillary effects are overcome. A study conducted to determine the exact effect of these capillary forces disclosed that for sufficiently high injection rates the flooding behavior became independent of these forces and was considered stabilized.

Data was obtained on the performance of an isolated ninespot waterflood. A general nine-spot correlation for areal sweep
efficiency as a function of water injected was obtained for a wide
range of mobility ratios. High oil recoveries and sweep out patterns
were obtained for all mobility ratios studied.



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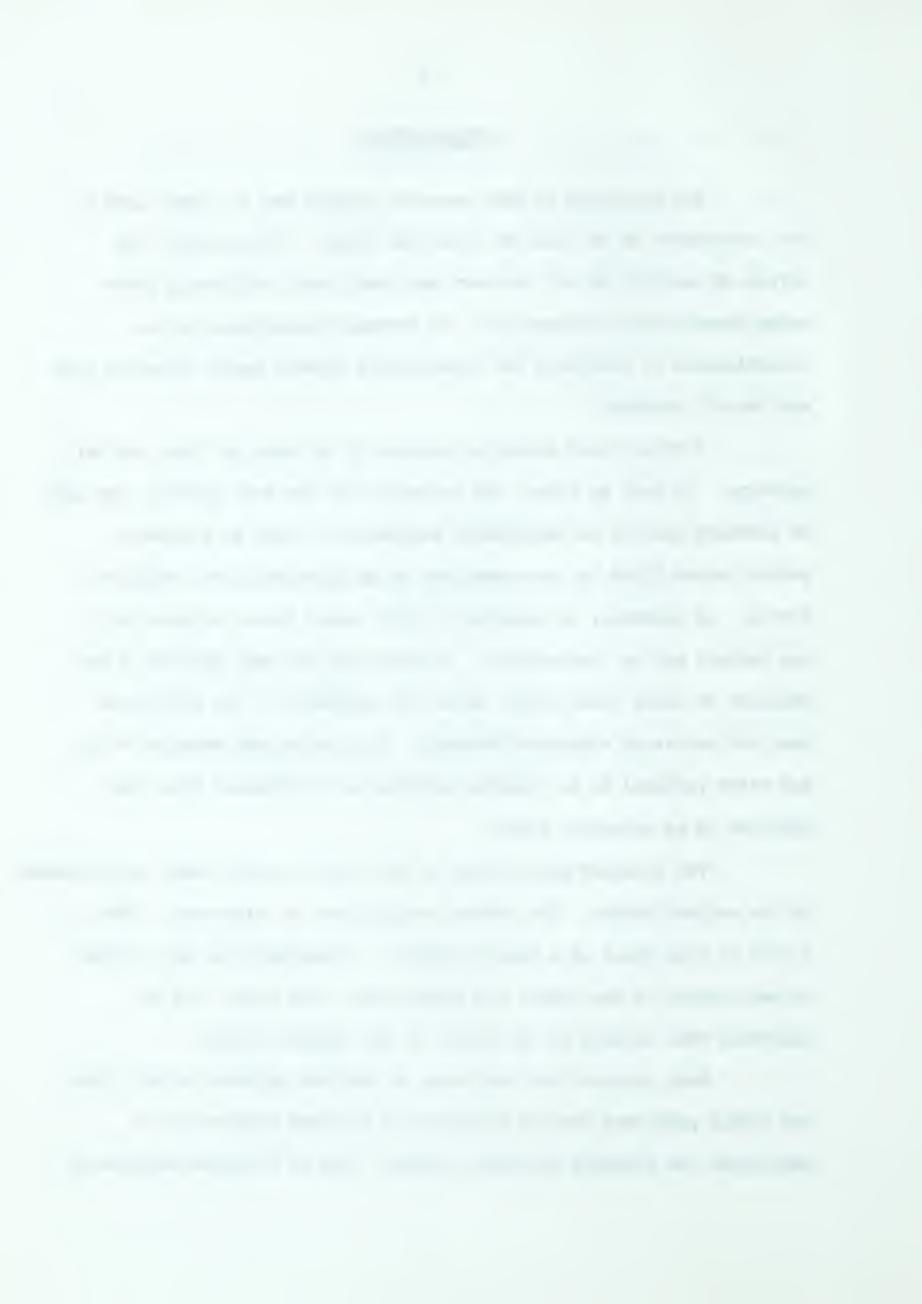
INTRODUCTION

The objective of this research project was to obtain data on the performance of an isolated nine-spot flood. In particular the effect of mobility on oil recovery and areal sweep efficiency after water breakthrough was examined. Of secondary importance was an investigation to determine the relationship between water injection rate and the oil recovery.

A water flood normally consists of an array of identical well patterns. In such an array, the perimeters of the well patterns are axes of symmetry and act as impermeable boundaries. Thus, an extensive pattern water flood can be visualized as an aggregation of "confined" floods. In contrast, an isolated or pilot water flood involves only one pattern and is "unconfined". In this case the well pattern is not balanced by other flood units; hence the perimeter of the pilot area does not act as an effective boundary. This causes the amounts of oil and water produced in an isolated pattern to be different from that produced in an extensive flood.

The isolated water flood is the type of system under investigation in the subject report. The pattern studied was the nine-spot. This is a unit of nine wells on a square pattern. Producing wells are located at each corner of the square and midway along each side, with the injection well located at the centre of the square pattern.

Much research has been done on confined patterns of all types but little published work is available on isolated systems and in particular the isolated nine-spot pattern. One of the main purposes of



an isolated or pilot water flood is to obtain advance knowledge about the performance of a large scale water flood development. Therefore the difference in behavior of a confined and unconfined system should be known.

The work presented is based of flow model experiments. One model was employed for the entire study. It consisted of a maximum density sand bed, packed between two transparent lucite sheets. The flood front was visually observed by using a fluorescent tracer dye and three ultraviolet lamps. Distilled water was used as the displacing phase and several different viscosity oils were used as the displaced phase.



FUNDAMENTAL MODEL PROPERTIES

CAPILLARY PRESSURE

Capillary forces in a porous medium are the results of the combined effect of surface and interfacial liquid tensions, pore size and shape, and the wetting properties of the reservoir rock. (19) Capillary pressure can be described as a measure of the tendency of the rock to imbibe the wetting fluid phase or to repel the non-wetting phase.

The displacement of one fluid by another in the pores of a porous medium is either aided or opposed by the surface forces of capillary pressure. (6) As a consequence, in order to maintain a porous medium partially saturated with non-wetting fluid, while the medium is also exposed to wetting fluid, it is necessary to maintain the pressure of the non-wetting fluid at a value greater than that in the wetting fluid. Denoting the pressure in the wetting fluid by $P_{\rm m}$ and that in the non-wetting fluid by $P_{\rm nw}$, we have

$$P_{nw} - P_{w} = P_{c} (S_{w})$$
 (1)

This is the defining equation for capillary pressure in a porous medium.

The fact that the capillary pressure-saturation curves of nearly all naturally occurring porous materials have many features in common has led to attempts to devise some general equation describing all such curves. Leverett (14) by utilizing dimensional analysis proposed the following relation,

$$J(S_{\mathbf{w}}) = \frac{P_{\mathbf{c}}}{\sigma \cos \theta} \sqrt{\frac{K}{\phi}}$$
 (2)

where $P_c = capillary pressure - dyne/cm²$



o = interfacial tension - dyne/cm

 $K = permeability - cm^2$

 \emptyset = fractional porosity

⊖ = contact angle

This J-function was originally proposed as a universal correlation for all porous media. However, subsequent work disclosed that it was only useful in correlating data connected with unconsolidated sands.

The evaluation of the capillary pressure versus saturation relation for the unconsolidated Ottawa sand (ASTM Designation C-109) system was carried out by Pritchard (20). He used a lucite tube fitted with screen electrodes throughout its length and packed with Ottawa sand. A capillary pressure drainage curve was obtained and converted into Leverett's J-function. The results are plotted in figure 1.

ABSOLUTE, EFFECTIVE AND RELATIVE PERMEABILITY

Permeability is that property of a porous material which characterizes the ease with which a fluid may be made to flow through the material by an applied pressure gradient. Permeability is the fluid conductivity of the porous material.

Permeability is defined mathematically by Darcy's Law:

$$K = \frac{Q\mu L}{A(\Delta P)} \tag{3}$$

where K = permeability in darcies

Q = flow rate in cc/sec



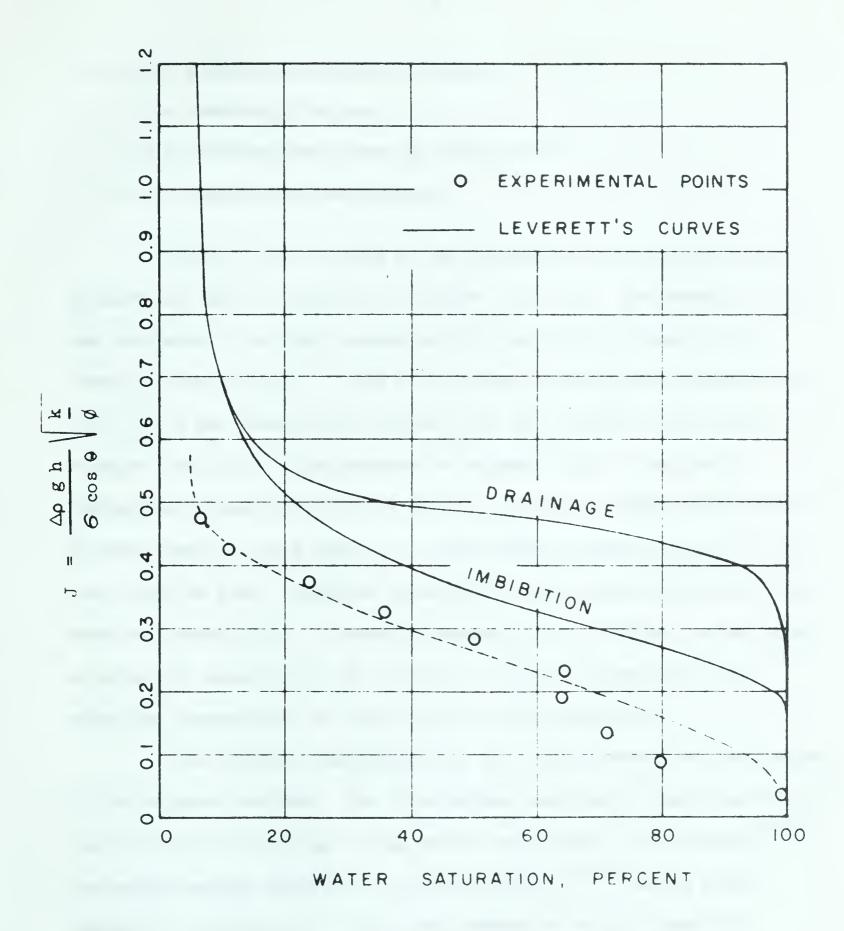


FIG. 1 CAPILLARY PRESSURE RESULTS COMPARED TO
LEVERETT'S J-FUNCTION (AFTER PRITCHARD)



 ΔP = pressure differential in atm.

L = core length in cm.

A = cross-sectional area of core in cm²

 μ = viscosity in centipoises

Darcy's Law is based on the assumption that only one fluid is present and that it completely saturates the rock. The permeability of the rock when it is fully saturated with one fluid is known as the "absolute permeability". When a fluid does not completely saturate the rock, as is the case in multi-phase flow, the ability of the rock to conduct that fluid in the presence of another fluid is called its "effective peremability" to the fluid in question. Since the presence of more than one fluid phase in a porous medium reduces the ability of each fluid to flow, effective permeabilities are always lower than the absolute permeability. "Relative permeability" is defined as the ratio of effective permeability to a fluid at a given saturation to the effective permeability to that fluid at 100% saturation.

The absolute permeability of the subject system was determined by two separate methods. The first method consisted of applying Darcy's Law to fluid flow through a sand packed lucite tube (See Pritchard (20)). The second method consisted of applying Muskat's (16) steady state, radial flow equation for a five-spot pattern to single fluid flow through the two-dimensional model. The calculations for the latter method are presented as Table 1 in Appendix A.

Pritchard (20) obtained effective and relative permeability data for the Ottawa sand by employing a steady state, desaturation



procedure. This method consists of introducing two fluids simultaneously into a linear system at a predetermined fluid ratio. The two fluids are injected through the core until steady state flow conditions are obtained and the existing saturations are stable. The saturations are determined by maintaining a volumetric balance of all fluids injected and produced. Once the saturation has been determined, the effective permeability of the two phases can be calculated by applying Darcy's Law to each phase individually. The effective permeabilities are present in Figure 2 and the relative permeabilities, as a ratio to the absolute permeability, are presented in Figure 3.

POROSITY

Porosity (effective) of a porous material is the fraction of the bulk volume occupied by interconnected voids.

The effective porosity of the model under study was determined by a simple material balance technique. The bulk volume of the model was calculated from the inside dimensions of the model. The model, containing dry sand, was saturated with water under vacuum and consequently all the pore spaces became completely filled with water (ie: one-hundred percent saturated with water). Thus by dividing the volume of the saturating fluid by the bulk volume the porosity was determined.

WETTABILITY

Rock surfaces can vary in their wettability, some being oil-wet and others water-wet. This factor of wettability enters into reservoir performance and also plays a primary role in laboratory investigations.

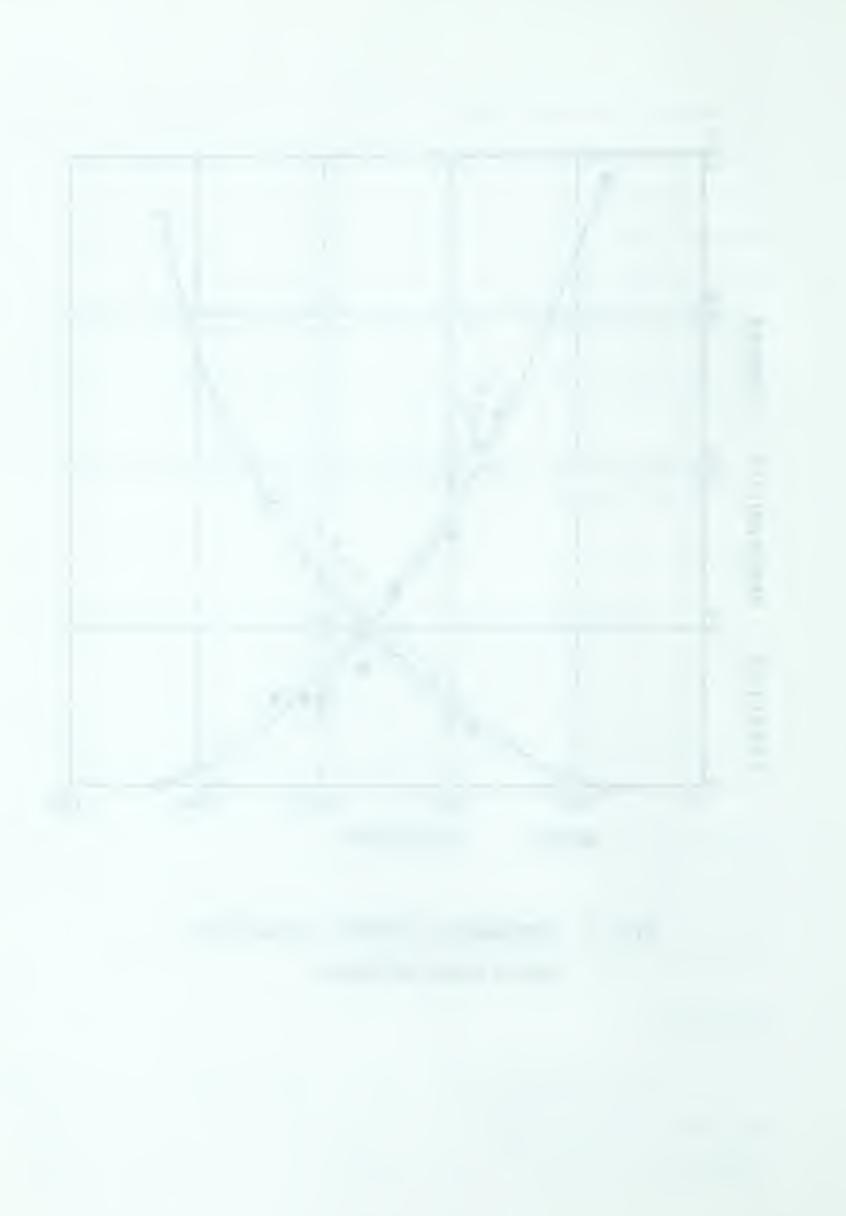


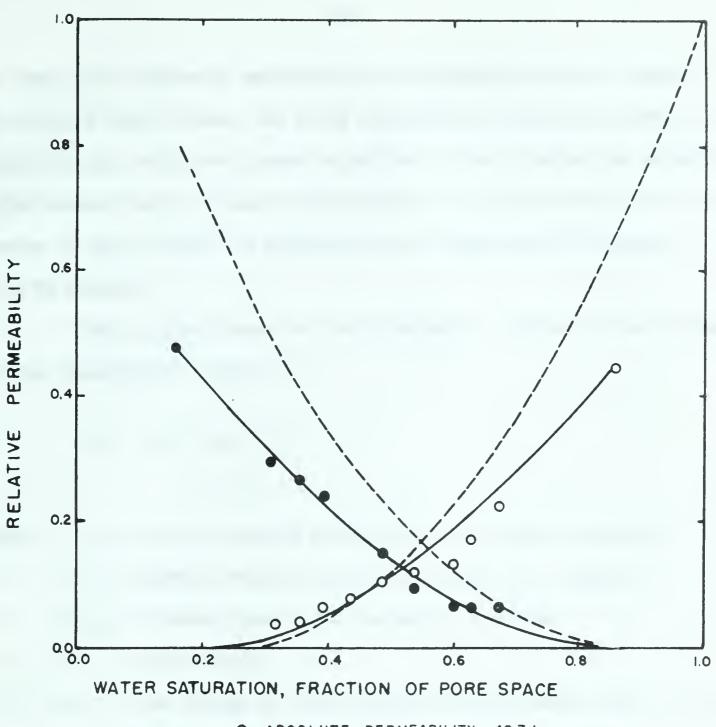
FIG. 2 EXPERIMENTAL EFFECTIVE PERMEABILITY

CURVES (AFTER PRITCHARD)

SATURATION

WATER



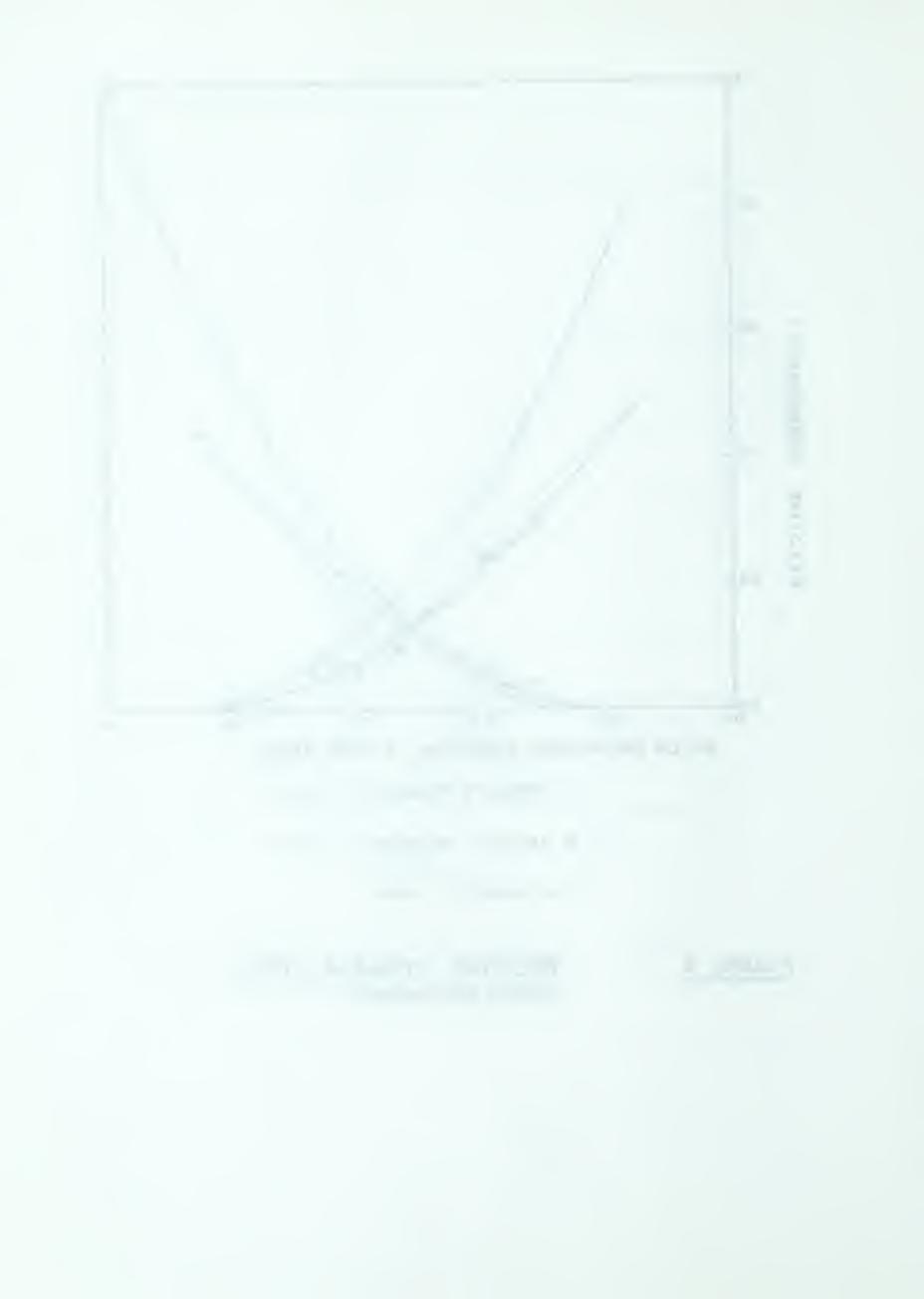


O ABSOLUTE PERMEABILITY = 40.7 d

ABSOLUTE PERMEABILITY = 40.7 d

--- LEVERETT'S CURVES

FIGURE 3 RELATIVE PERMEABILITIES (AFTER PRITCHARD)



In theory, the degree of wettability is frequently defined in terms of the contact angle between the fluid interface and the solid surface. A preferentially water-wet system is defined as one in which the advancing water contact angle is less than 90 degrees. A preferentially oil-wet system is one in which the advancing water contact angle is greater than 90 degrees.

The surface forces in a solid-water-oil system can be related by the Young-Dupree equation (1):

$$A_{SW} - A_{SO} = \sigma_{OW} \cos \theta$$

$$= -\Delta F \qquad (4)$$

where: A_{sw} = adhesion tension between solid and water - ergs/cm² A_{so} = adhesion tension between solid and oil - ergs/cm²

 σ_{ow} = oil-water interfacial tension - dynes/cm

 θ = contact angle

 ΔF = free energy of displacement of oil by water from a solid surface - ergs/cm²

If the contact angle is less than 90 degrees, the adhesion tension difference is positive and oil displacement by water from a solid surface will be spontaneous and favored by a high oil-water interfacial tension. If the angle is greater than 90 degrees the displacement will not be spontaneous but will require less energy the lower the oil-water interfacial tension. This behavior has been verified experimentally by Newcombe. (18)



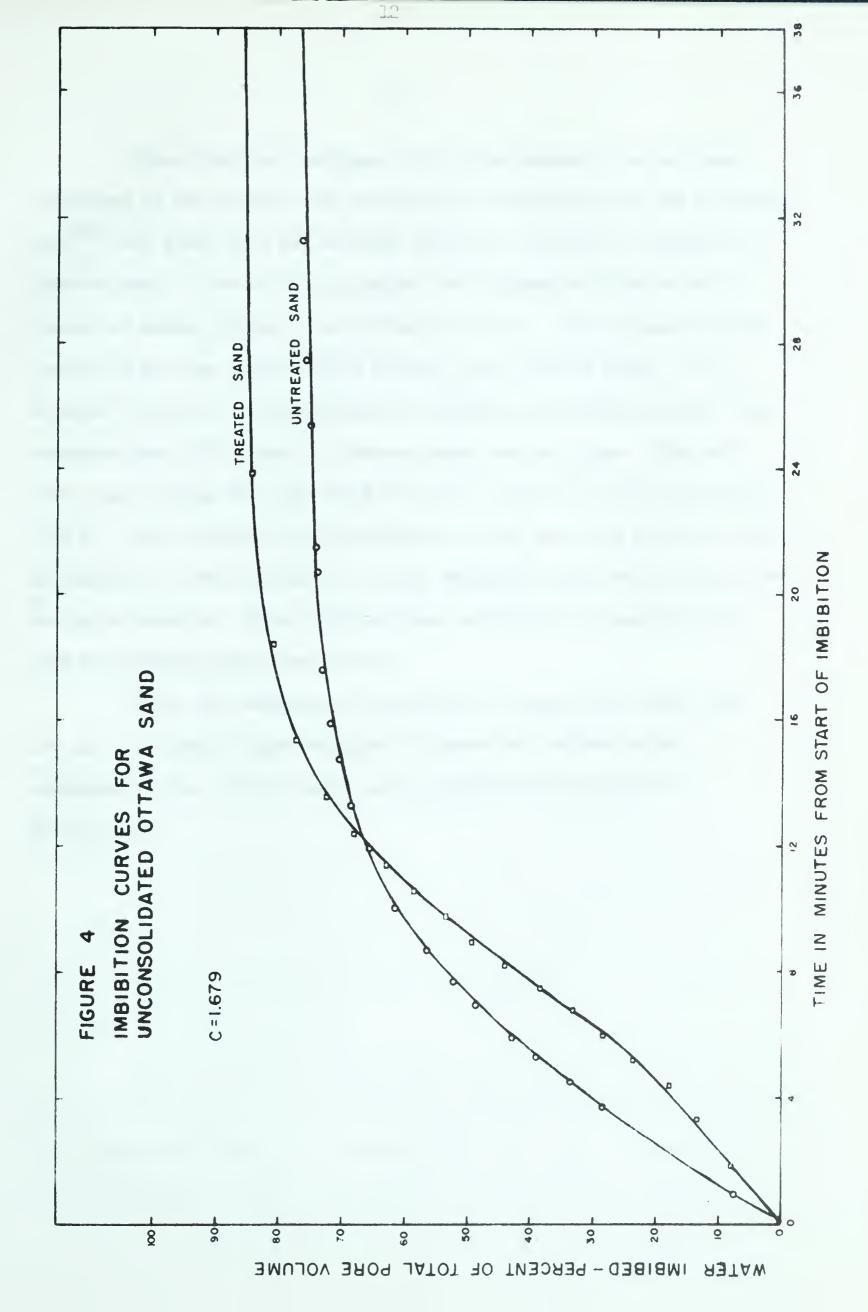
To ensure that the sand used in the subject study was preferentially water-wet, it was washed with concentrated chromic acid and fired at 1100°F for 12 hours. To verify that this technique produced a water-wet sand a procedure suggested by Bobek⁽²⁾ was employed.

Imbibition tests conducted on the Ottawa sand, using a volumetric apparatus identical to that used by Bobek, resulted in oil being spontaneously displaced from the sand by water. A plot of the volume of water imbibed versus time is presented as Figure 4. The reverse procedure of saturating the sand with water and having the oil act as the displacing phase resulted in no displacement. This latter test gave added assurance that the sand was definitely water-wet.

Figure 4 presents two curves which show the rate of imbibition for both the untreated and treated sand. The tests indicate that the imbibition process was more complete for the treated sand than for the untreated sand (ie: 86% to 76%). This indicates that the acid wash and heat treatment produced a more water-wet sand.

It should also be pointed out that the spontaneous displacement of oil by water from the treated sand would only occur after the treated sand was submerged in water for an extended period, dryed at room temperature and then saturated with oil. In addition the water used in the tests had to be slightly acidic. This was accomplished by adding a small amount of hydrochloric acid. Tests conducted on the treated sand immediately after the heat treatment resulted in only a small amount of water being imbibed (ie: less than 1% of the pore volume).







These limiting conditions which were necessary to initiate imbibition in the treated sand tests might be attributed to the following. Weyl (26) has shown that the surfaces of glass, silica, etc. consist of hydroxy-groups. These hydroxy-groups extend hydrogen bonds to such liquids as water, glycerol and sulfuric acid as a result these liquids completely wet the material thus giving a zero contact angle. It is believed that the treated sand was so completely dehydrated by the heat treatment that this layer of hydroxy-groups was destroyed. Thus with this layer missing the sand would be wet by the first liquid in contact with it. This proposal is substantiated by the fact that after the sand was exposed to water and dried at room temperature the imbibition process was again possible. This indicated that imbibition is possible only when the hydroxy-groups are present.

Since the sandpack was initially in contact with water and not oil, the treated sand retained its water-wet preference and consequently the ensuing tests were conducted in a water-wet porous media.



MODEL STUDIES

One model was used for the entire series of floods, however due to difficulties encountered in changing oils two separate sand packs were necessary. Reservoir properties of each pack and model dimensions are included in Table 2 in Appendix A. The flood front during each flood was visually observed by using a water soluble fluorescent tracer dye excited by ultraviolet light.

Data taken during each run consisted of water injected, oil and water produced and producing water-oil ratio. In addition the area contacted by the injected water was traced on the top of the model. The pattern was later photographed and the area found by planimetering.

DESCRIPTION OF APPARATUS

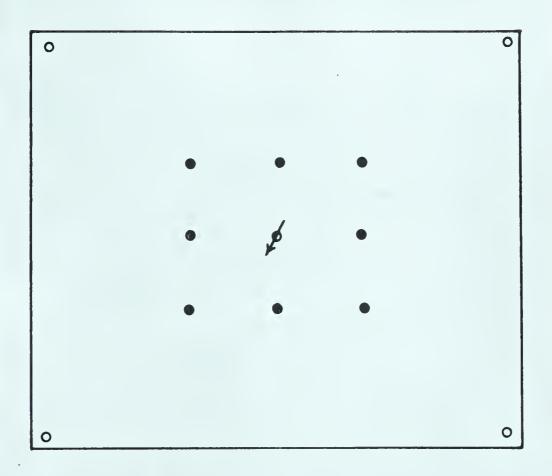
The model was a maximum density sand bed packed between two transparent lucite sheets. The maximum density pack was obtained by bolting the model to a "Syntron" electric vibrator (Model VP - 60), fitted with a wooden top, and vibrating the entire model for ten hours.

A schematic diagram (Figure 5) shows the pattern of injection and producing wells. In addition to Figure 5 a photograph of the entire apparatus, including the lighting arrangement, is presented in Figure 6.

Nine simulated oil wells are located on an isolated pattern.

There are also wells in the four outside corners of the model. Injection was maintained by means of a constant rate Ruska pump. A liquid filled mercury manometer fitted to the injection line served as a pressure







- PRODUCING WELL
- O SHUT-IN WELL

FIGURE 5
SCHEMATIC DIAGRAM OF ISOLATED NINE-SPOT WELL PATTERN





FIGURE 6. PHOTOGRAPH OF EQUIPMENT SHOWING

TWO-DIMENSIONAL MODEL, INJECTION

PUMP AND LIGHTING ARRANGEMENT.



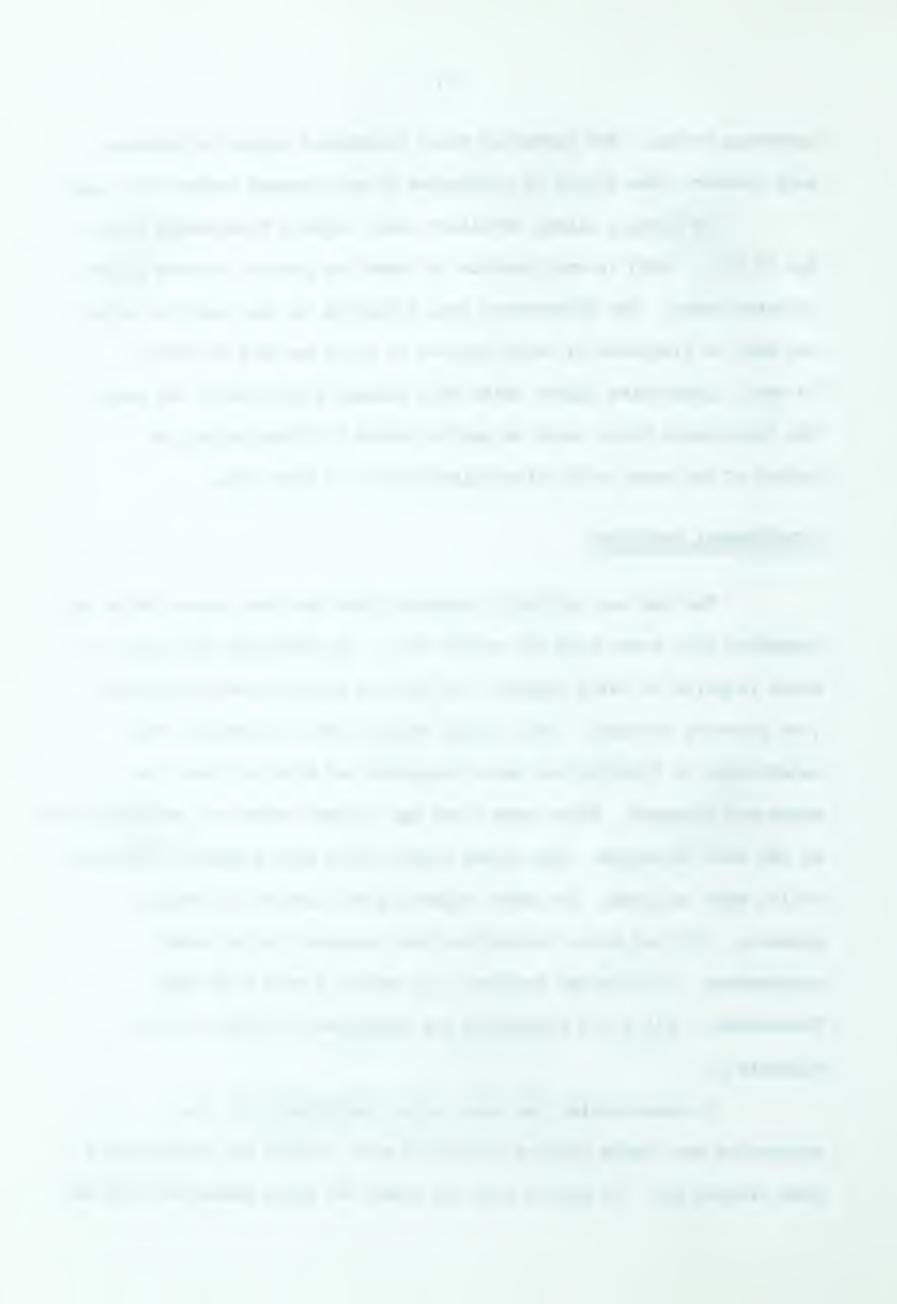
measuring device. The producing wells discharged against a constant back pressure (See Figure 6) maintained by an elevated outlet flow line.

By using a highly efficient water soluble fluorescent tracer dye (C.I.L. - LTS) it was possible to trace the pattern covered by the injected water. The fluorescent dye, dissolved in the injection water, was made to fluoresce by being exposed to light emitted by three, 40 watt, ultraviolet lights which were closely fitted under the model. The fluorescent water could be easily traced by illuminating the bottom of the model with ultraviolet light in a dark room.

EXPERIMENTAL PROCEDURE

The bed was initially evacuated from the four corner wells and saturated with water from the centre well. By measuring the amount of water required to fully saturate the bed the porosity was calculated (see porosity section). The initial connate water saturation was established by flooding the water saturated bed with oil until no water was produced. After each flood the connate water was re-established by the same procedure. Six floods using fluids with different viscosity ratios were employed. The water viscosity was altered by adding glycerol. Oil and water viscosities were measured using Oswald viscometers. Interfacial tensions were measured with a Du Nory Tensiometer. All fluid properties are summarized in Table 3 (see Appendix A).

In resaturating the model with a different oil, the saturation was always carried out with a more viscous oil displacing a less viscous oil. To ensure that the model was fully saturated with the



new oil, the viscosity of the effluent oil was measured and if it was the same as the viscosity prior to injection the model was considered fully saturated.

As previously stated a record was kept of water injected, water and oil produced and producing water-oil ratio during each flood. All floods were terminated when approximately 25 pore volumes of water had been injected. In all cases the terminating water oil ratio was greater than ten to one.

The location of the flood front during each flood was recorded by contouring the top of the model. Injection was temporarily terminated each time the location of the flood front was traced.

After each flood was completed a photograph of the entire flood pattern was taken. A typical flood pattern is illustrated in Figure 7. By enlarging the photograph of each flood the area contacted by the injected water was found by using a planimeter.

DEFINITION OF TERMS AND CALCULATION PROCEDURES

Definitions

Many of the fundamental properties that must be known to determine the merits of a secondary recovery operation can be evaluated by core analysis or linear flood investigation. However, to fully evaluate a secondary recovery project such information as area sweep efficiency, vertical sweep efficiency and total sweep efficiency must be evaluated. This can be done by using a three-dimensional model.





FIGURE 7. PHOTOGRAPH OF FLOOD 3-d ILLUSTRATING
THE LOCATION OF THE FLOOD FRONT DURING
VARIOUS STAGES OF INJECTION.



It has been found that the amount of recoverable oil can be determined by water flooding small core samples. When the amount of recoverable oil is expressed as a fraction of the pore volume, it is called the "displacement efficiency" to a water flood for that particular rock. Multiplying this displacement efficiency, for a particular sample, by the total pore volume of the hydrocarbon bearing rock will give the maximum possible recovery of oil by a water flood. This however, is only half the information required to calculate the expected oil recovery of a pattern flood. In addition to knowing the displacement efficiency, it is also necessary to be able to predict the areal fraction of the reservoir which will be invaded by water. By combining these two factors oil production can be calculated as follows:

Oil Recovery =
$$E_d \times E_{as} \times P.V._{res}$$
 (5)

where E_d is the displacement efficiency, E_{as} is the areal sweep efficiency and $P.V._{res}$ is the total pore volume of the oil reservoir (unit area). By dividing by $P.V._{res}$ the following relation is obtained:

$$E_{s} = E_{\hat{\mathbf{d}}} \times E_{\mathbf{a}s} \tag{6}$$

Here E_s is referred to as the total sweep efficiency. In actual fact the above relationships are not complete. The equations should also include a vertical sweep efficiency term. It is obvious that a non-homogeneous reservoir, such as one having strata of different permeability, will not be evenly or completely invaded on the vertical scale by the injected water. In the case of the sand packed reservoir the vertical sweep efficiency will be 100% due to its homogeneous nature. Consequently, the vertical term is not considered in the subject study.



The previous statements can be reiterated in the following brief definitions. Areal sweep efficiency is defined as the measure of the area of a reservoir which is contacted by the injected fluid at any time as compared to the unit area of the pattern. Displacement efficiency refers to the fraction of oil which is swept from the individual pores as compared with the amount of oil originally in place in the pores.

Many variables will affect the areal sweep efficiency of a water flood. The two factors exerting the most influence on the flood pattern were found to be the injection pattern and mobility ratio.

Mobility can be thought of as a measure of the ease with which the fluid will flow through the rock. The mobility as used in this study is defined as:

$$M = \frac{\text{Displacing phase mobility}}{\text{Displaced phase mobility}} = \frac{K_W/\mu_W}{K_O/\mu_O}$$
 or

$$M = \frac{K_{W}\mu_{O}}{K_{O}\mu_{W}} \tag{7}$$

where M is the fluid mobility; K_W , K_O are the effective permeability of the porous medium to water and to oil respectively and μ_W and μ_O are water and oil viscosities.

Calculation Procedures

All areal sweep efficiencies used in this report were obtained from direct measurement, as outlined in the previous section on experimental procedure. One exception to this is the areal sweep efficiency at



breakthrough. The breakthrough sweep efficiency values were calculated from:

$$E_{s} = E_{as} \times E_{d} \tag{6}$$

The total sweep efficiency (E_s) was calculated from the oil production at breakthrough. The displacement efficiency was also calculated and the procedure will be explained later. Thus knowing two terms of equation six the breakthrough efficiency was calculated.

All displacement efficiency terms referred to hereafter are calculated values. The displacement efficiency is simply the change in oil saturation in the swept zone. It is calculated by dividing the volume of oil recovered by the amount of oil originally in place in the zone swept by the injected fluid, up to the time in question. It is obvious that a saturation gradient exists from the injection well to the flood front and since there is no satisfactory method of determining this gradient, the calculated displacement efficiency must be regarded as representing an average value in the swept region.

The mobility ratios were calculated in the following manner:

1. The average saturation behind the flood front is obtained from the calculated displacement efficiency and the connate water saturation. Thus the saturation of the invading fluid behind the front is given by:

$$\overline{S}_{w} = S_{cw} + (1 - S_{cw})E_{d}$$
 (8)

where \overline{S}_{w} is the average water saturation behind the flood front, S_{cw} is the connate water saturation and E_{d} is the average displacement efficiency.



- 2. The effective (or relative) permeability to water at this saturation is read from the experimental effective (or relative) permeability curves.
- 3. The effective (or relative) permeability to oil is the value corresponding to the oil saturation at the flood front. It there is no gas phase, as is the case in this study, this will be the connate water saturation.
- 4. The values are substituted along with the respective viscosities into the equation:

$$M = \frac{K_W \mu_O}{K_O \mu_W} \tag{7}$$

where all terms are as defined previously.

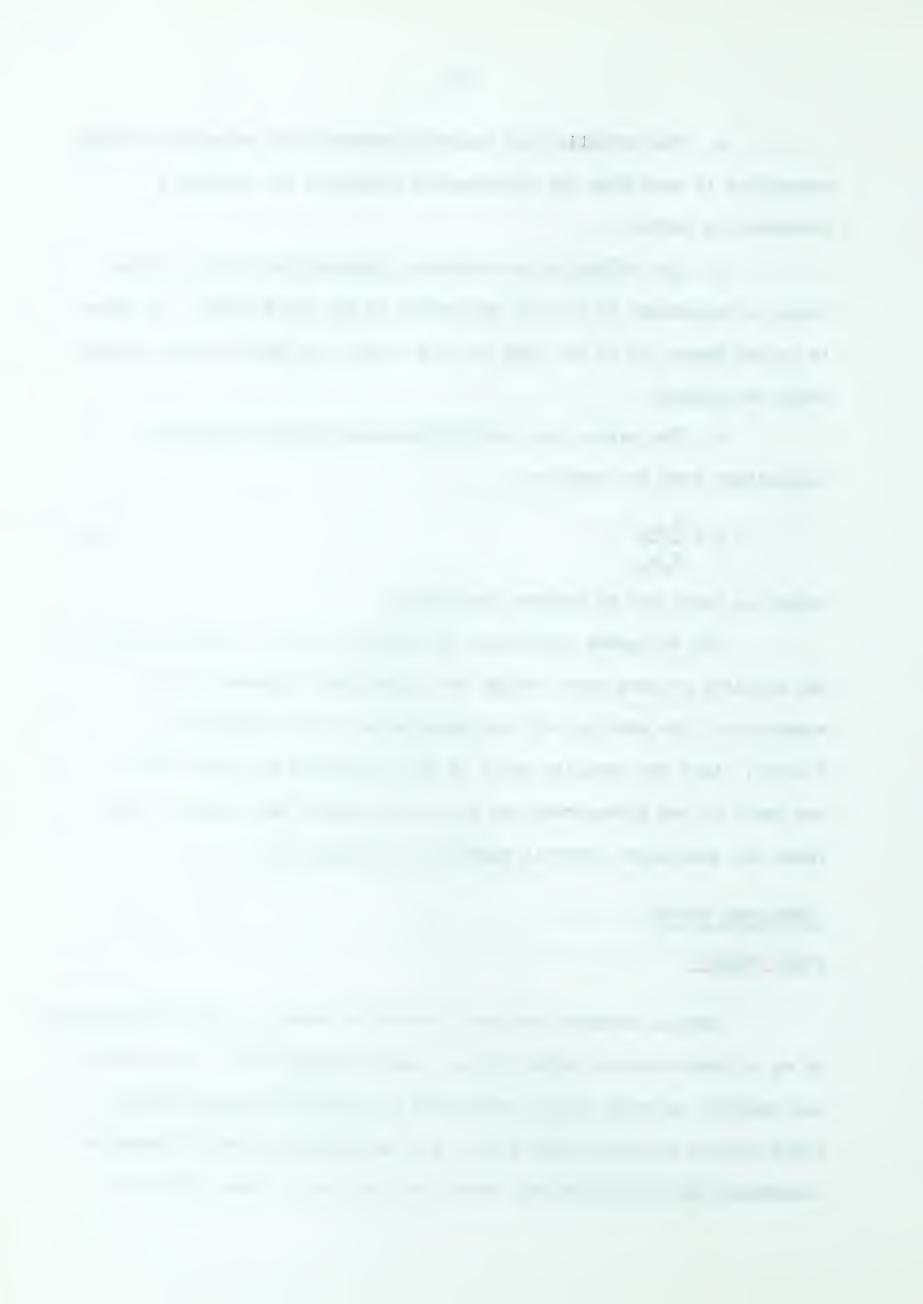
The stringent definition of mobility ratio is the summation of the mobility of each phase behind the flood front compared to the summation of the mobility of each phase ahead of the flood front.

However, since the mobility ratio of the oil behind the flood front was small it was disregarded and since the connate water ahead of the front was considered immobile equation 7 is applicable.

LITERATURE REVIEW

Model Studies

Several methods have been devised to study the sweep efficiencies of an oil-water-porous media system. Early workers (13,27) found that it was possible to model actual reservoirs by using the analogy between fluid flow in a porous media and flow of an electric current through a resistance bed (potentiometric model) or the flow of ions through a



conducting solution (electrolytic model). The use of such models is based on the fact that voltage distribution in electric conductors can be represented by Laplace's equation, which also can be used to represent the pressure distribution of steady state, incompressible fluid flow in a homogeneous porous media. Pressure drops are equated to voltage drops; flow rates to current rates; and other parameters are equated to resistances.

Sweep efficiencies have also been studied with the techniques of applied mathematics. Muskat⁽⁵⁾ has been the leading authority in this type of approach. However, even for simple systems the resulting mathematical equations are complex and difficult to solve.

Most of the above approaches are limited by the assumption that the invading and invaded fluids have the same flow properties (ie: unit mobility). Consequently dimensionally scaled models of reservoir elements, in which the properties of the rock and the fluids in the model are properly scaled to reservoir conditions, were introduced. Slobod and Caudle, (24) early workers in this field, introduced the X-ray shadowgraph model as a means of readily studying the effects of mobility on sweep efficiencies. The reservoir unit was a porous plate which was sealed on the top, bottom and edges. Variations in mobility ratios were obtained by varying the viscosity of the fluids. The injected fluid contained an X-ray absorbing material and the flood front was followed on a fluorescent screen or film.

Numerous papers outlining the effect of mobility ratio and other parameters on sweep efficiency have been published. Most of these papers only considered areal sweep efficiency up to breakthrough. Production after breakthrough was not considered.



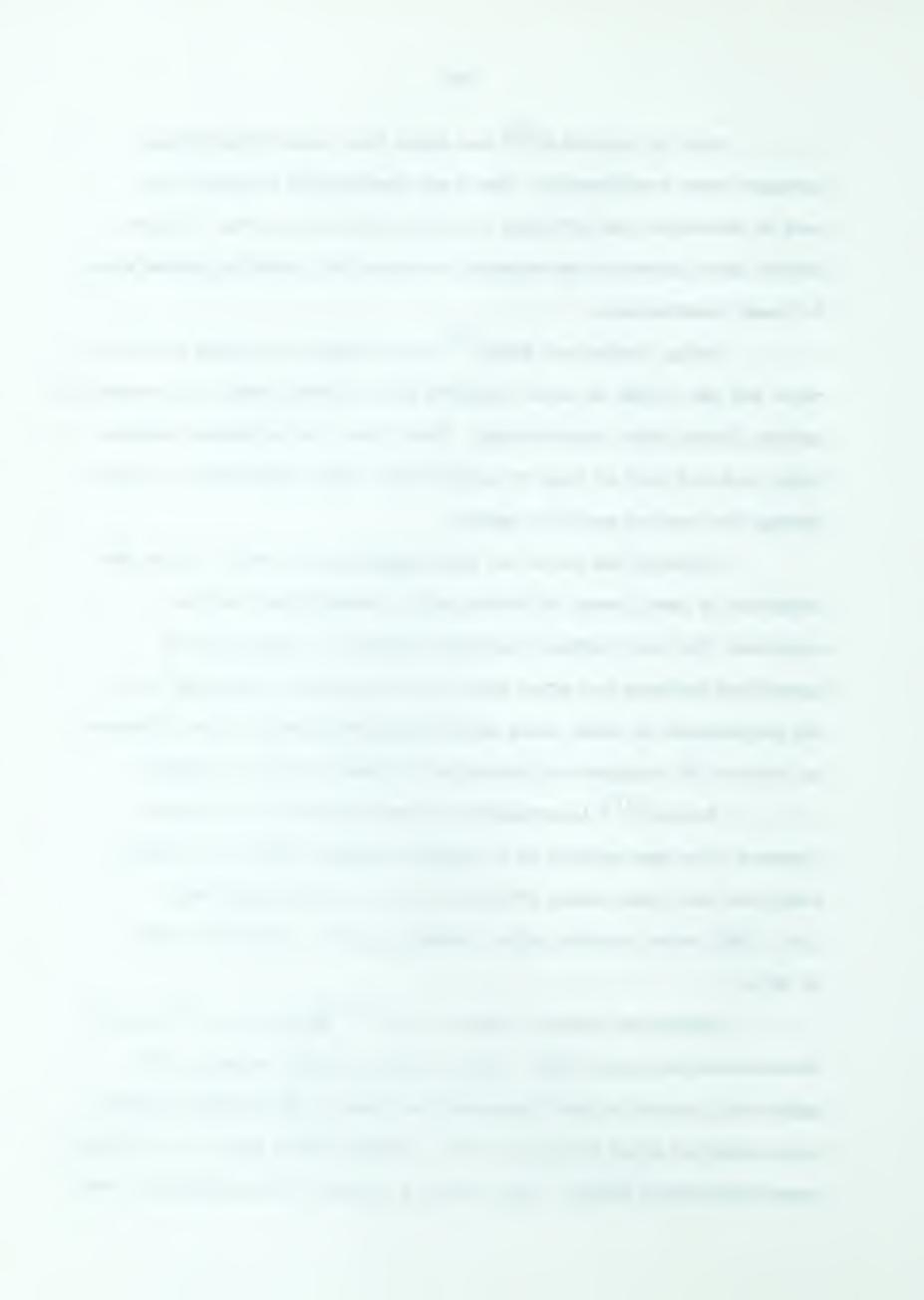
Work by Dyes et al⁽⁹⁾ has taken into account additional sweepout after breakthrough. The X-ray shadowgraph technique was used to determine the influence of fluid mobilities on the sweepout pattern when injection was extended to cover the producing period which followed breakthrough.

Craig, Geffen and Morse (7) investigated the effect mobility ratio and the volume of water injected had on areal sweep efficiencies in pattern floods after breakthrough. They found good agreement between their work and that of Dyes et al for areal sweep efficiency at breakthrough for various mobility ratios.

Although the above two investigations take into account the variation of areal sweep efficiency after breakthrough they were concerned with only pattern (confined) systems. Since pilot or unconfined patterns are often used to obtain advance knowledge about the performance of large scale water flood developments, the difference in behavior of confined and unconfined systems should be examined.

Neilson⁽¹⁷⁾ investigated the performance of an isolated, inverted five-spot pattern at a constant mobility ratio. The study disclosed that areal sweep efficiencies of very high magnitude (ie: 600%) were obtained after breakthrough for a water oil ratio of 20:1.

Additional work by Caudle et al, (4,5) palton et al (8) tend to substantiate Neilson's work. These papers are also concerned with additional production and increased areal sweep efficiencies obtained from undrilled areas of an oil field. These studies employed artificial consolidated sand models. The results disclosed that considerable area



outside the normal well pattern was contacted by the injected fluid and consequently contributed to production.

Critical Rate

There are numerous published papers concerned with the effect of water injection rates on oil recovery. Various investigators (10,11,12 15,18,20,21) have shown that oil recovery increased, decreased or remained stabilized with increases in the rate of injected water.

Rapoport and Leas $^{(21)}$ found that for a linear water flood, recovery varied with length, rate and the viscosity of the displacing phases; for a given porous media and a given water-oil viscosity ratio. They also found that for floods with the same $\text{Lv}\mu_w$ product, the production behavior was similar, that is equal injection volumes resulted in equal recoveries. This resulted in their proposal of $\text{Lv}\mu_w$ as a general scaling coefficient for model tests. They further discovered that at some critical value of $\text{Lv}\mu_w$, recovery was independent of this factor; this is referred to as the critical scaling coefficient and thus "v" as the critical rate.

Separate studies by Newcombe⁽¹⁸⁾ and Kyte⁽¹²⁾ support Rapoport's investigation. That is oil recovery in linear systems (regardless of preferential wettability) increased with increasing rate up to a point where further increases in rate resulted in no additional recovery.

Investigations conducted by Jones-Parra (11) and Engleberts (10) disclosed that oil recovery decreased with increasing injection rates. However this reverse behavior was attributed to viscous fingering.



All of the previously mentioned investigations were primarily concerned with the scaling of linear flow systems and hence are somewhat limited. Consequently the formulation of more general scaling laws, applicable to three-dimensional systems, was necessary. Rapoport (22) has derived scaling laws applicable to three-dimensional systems. The laws were established on a mathematical basis and are applicable to incompressible immiscible, two phase flow systems. Particular consideration was placed on the roles of capillary pressure functions and relative permeability.

A laboratory investigation conducted by Rapoport (23) employs the previously mentioned scaling laws. Theoretical consideration, verified by experimental work, disclosed that areal flooding behavior depends specifically upon the rate of injection per unit sand thickness. More generally, it was seen that the displacement of oil by water in a two-dimensional flow system was largely governed by the dimensionless group of parameters;

$$C_2 = \frac{q \mu_W}{\sigma_{oW} \cos \theta \sqrt{K\emptyset}} \tag{9}$$

where q is injection rate per unit sand thickness, μ_W is water viscosity, σ_{ow} oil-water interfacial tension, K is permeability and \emptyset is porosity. Derivation of the above equation is presented in Appendix B.

This group " C_2 " was designated as the "capillary pressure coefficient" because its value defined the relative importance of capillary forces in the displacement of oil by water. It was found that for a given value of C_2 all porous media of given geometry, operated



under similar boundary conditions, and characterized by the same oil-water viscosity ratio, the same fractional flow, relative permeability and J-functions, will yield the same flooding behavior (ie: the same relation between water injection and oil production).

As was the case in linear systems, a critical value of C₂ existed. When this critical value was exceeded the two-dimensional water-oil displacements became independent of rate and were qualified as stabilized.



EXPERIMENTAL RESULTS AND DISCUSSIONS

CRITICAL RATE STUDY

Results

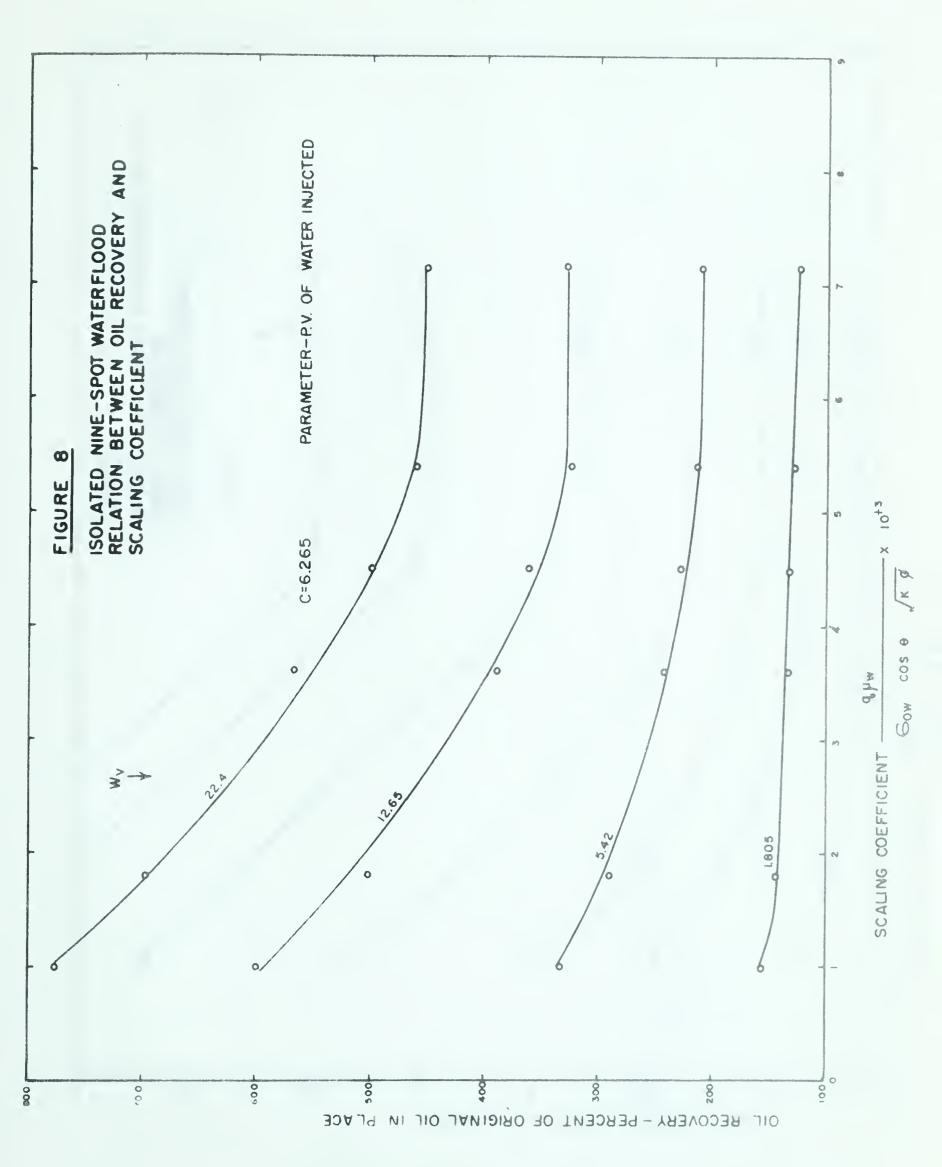
To ensure that the results obtained in this study would represent field behavior as close as possible, the influence that capillary pressure exerted on laboratory data had to be determined. To accomplish this a critical rate study was conducted. Two fluid systems of different viscosities were employed. The two systems are identified as follows:

Flood Series 3 - Oil-water viscosity ratio of 6.265
Flood Series 1 - Oil-water viscosity ratio of 1.679

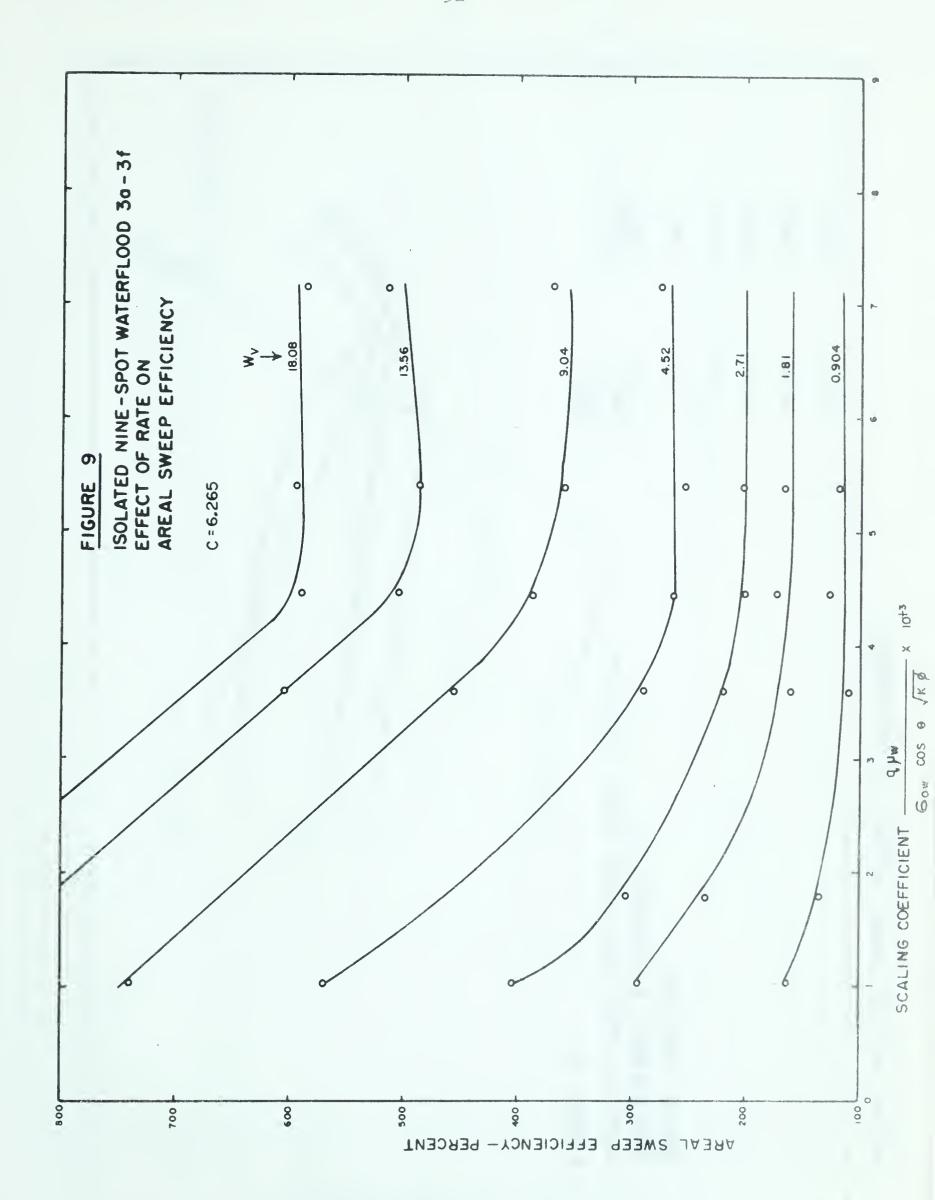
Since a two-dimensional system was employed in the subject study it was expected that areal sweep efficiency, displacement efficiency and total sweep efficiency (oil recovery) would be influenced by capillary forces. To determine the magnitude of this effect, numerous floods were conducted on the two systems at different injection rates. Injection rates varied from 2.31 B/D/ft (320 cc/hr) to 20.20 B/D/ft (2800 cc/hr). The production history of flood Series 1 and 3 are given in tables 4 to 15 inclusive. Areal sweep efficiencies and calculation of displacement efficiencies for the subject series of floods are presented in Tables 20 to 30 inclusive. The basic information presented in the previously mentioned Tables are graphically represented in Figures 8 to 14 inclusive.

In figures 8 and 12 oil recovery has been plotted against Rapoport's (22) two-dimensional scaling coefficient. All terms in the

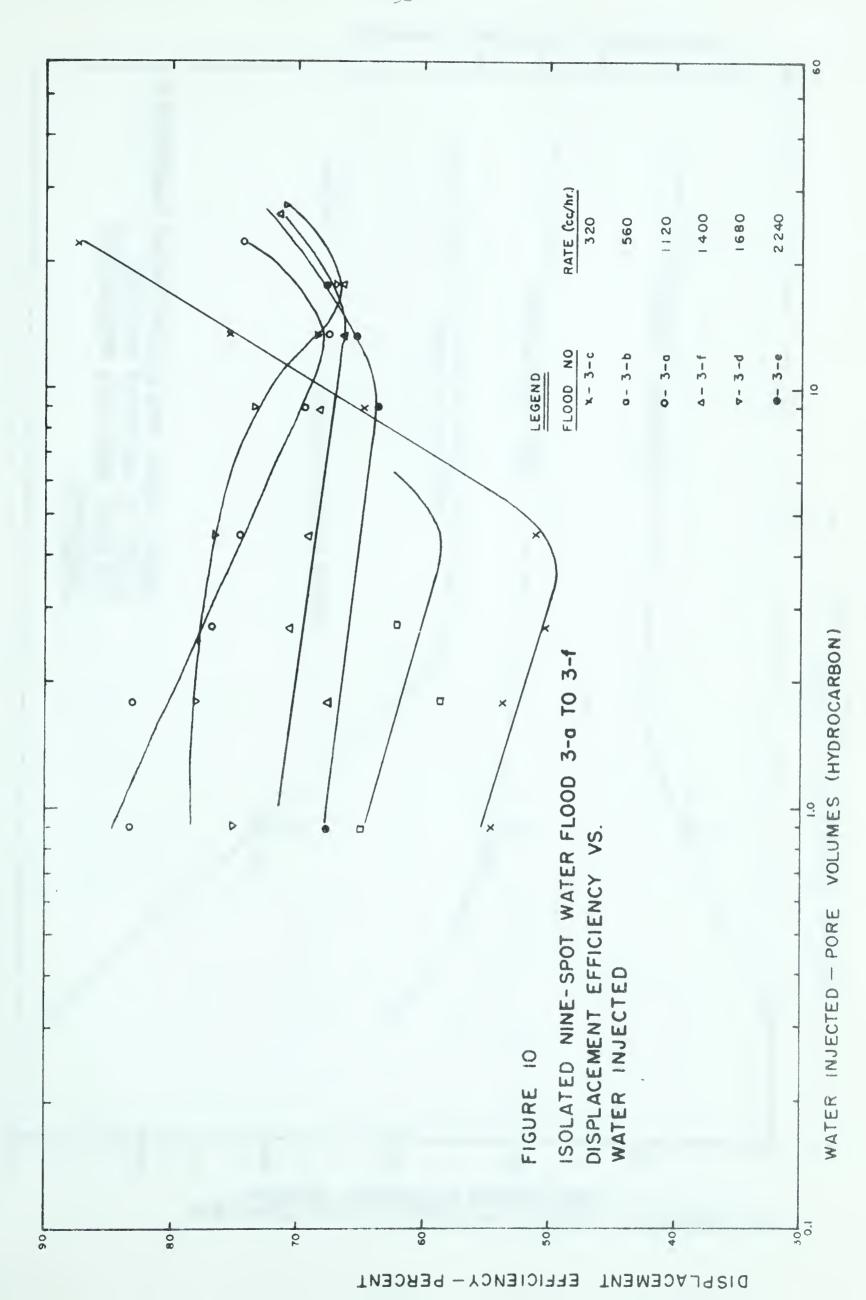




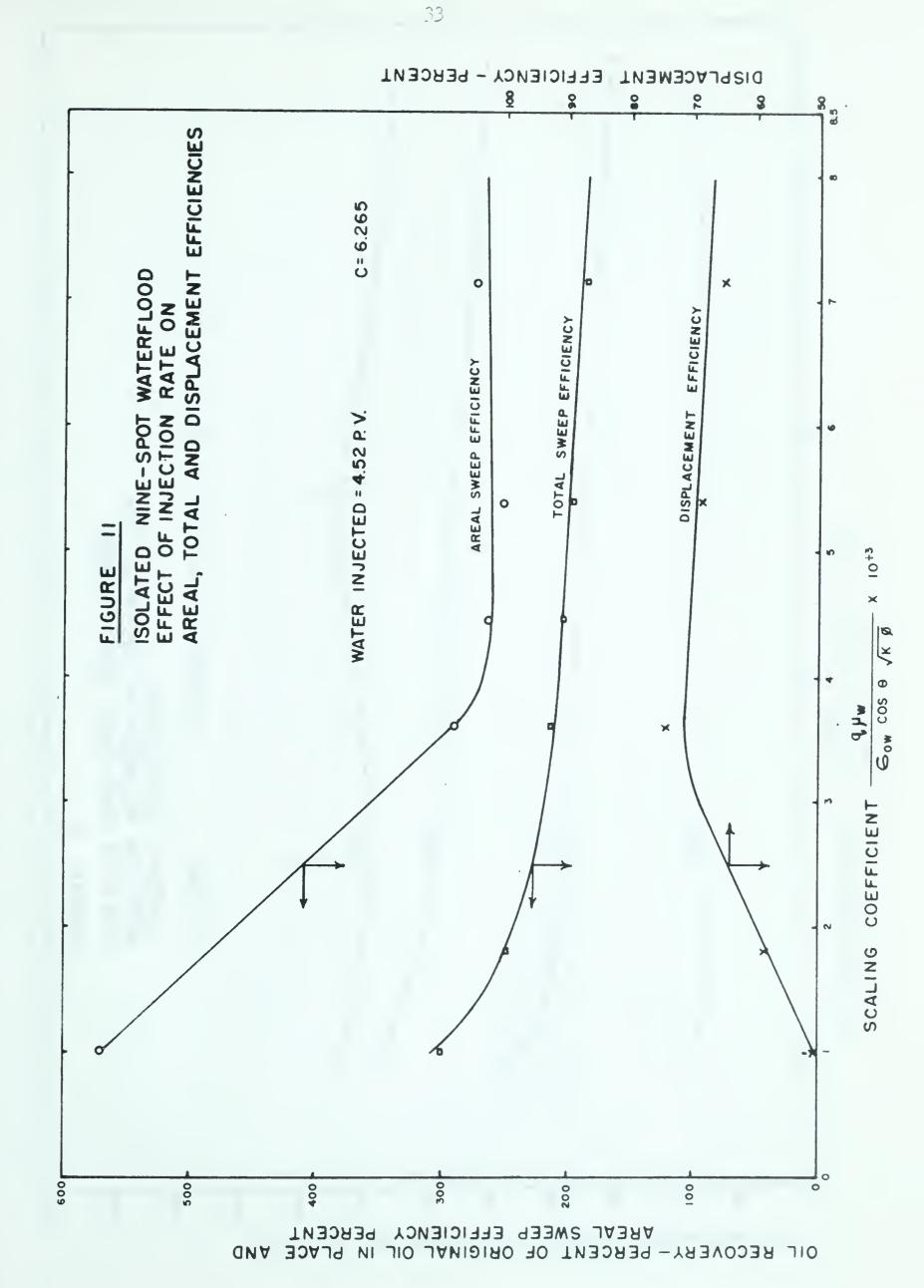




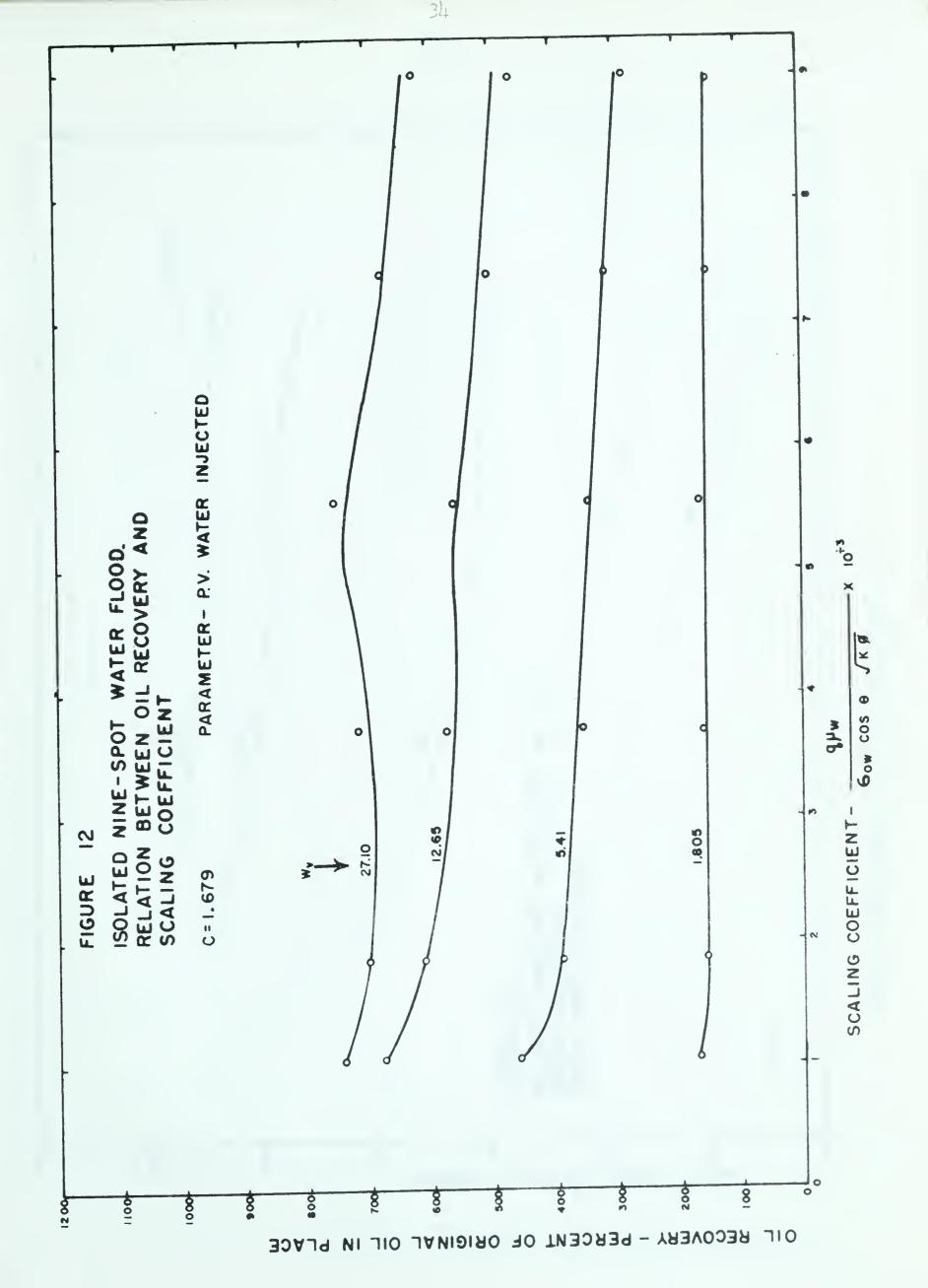


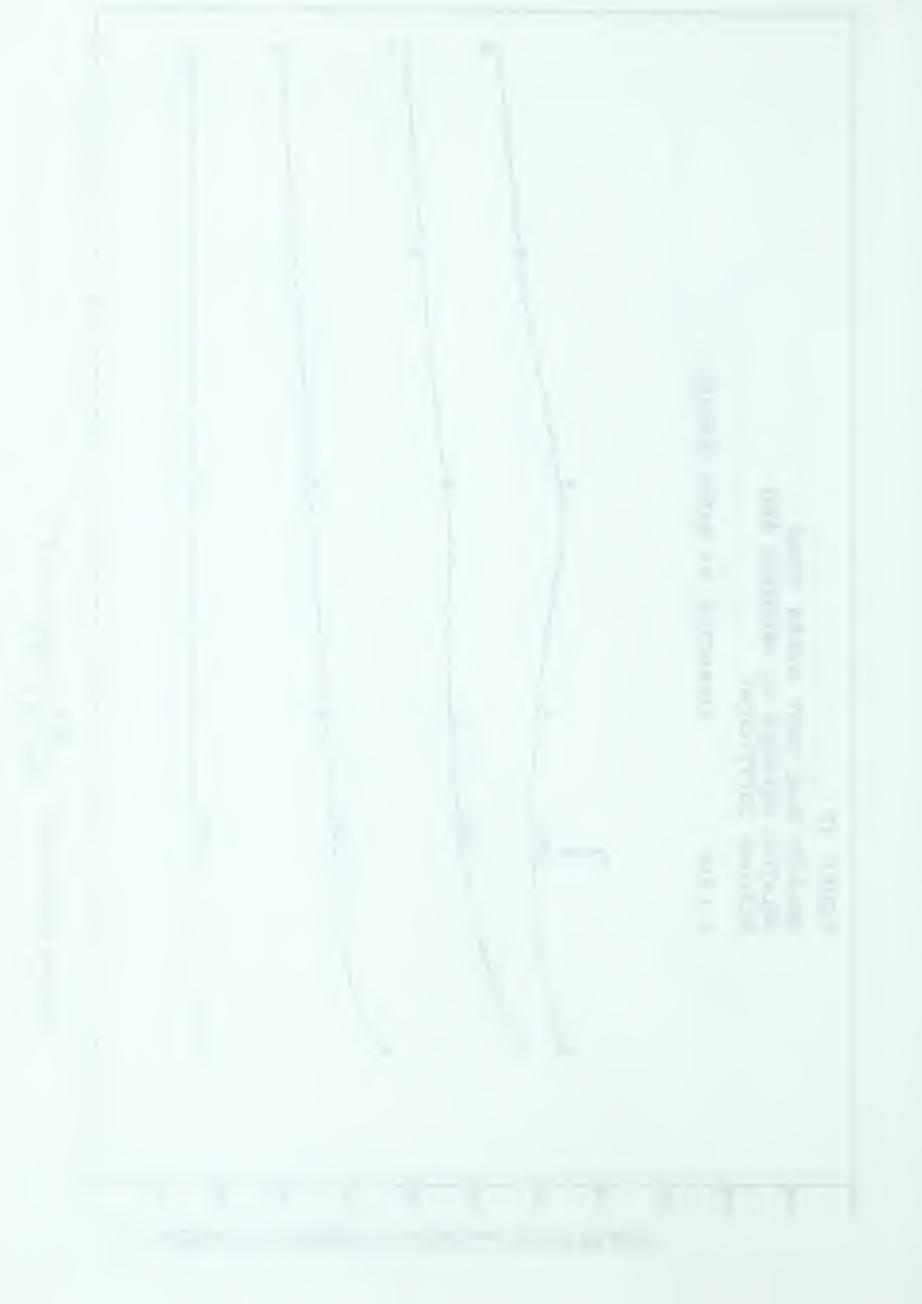


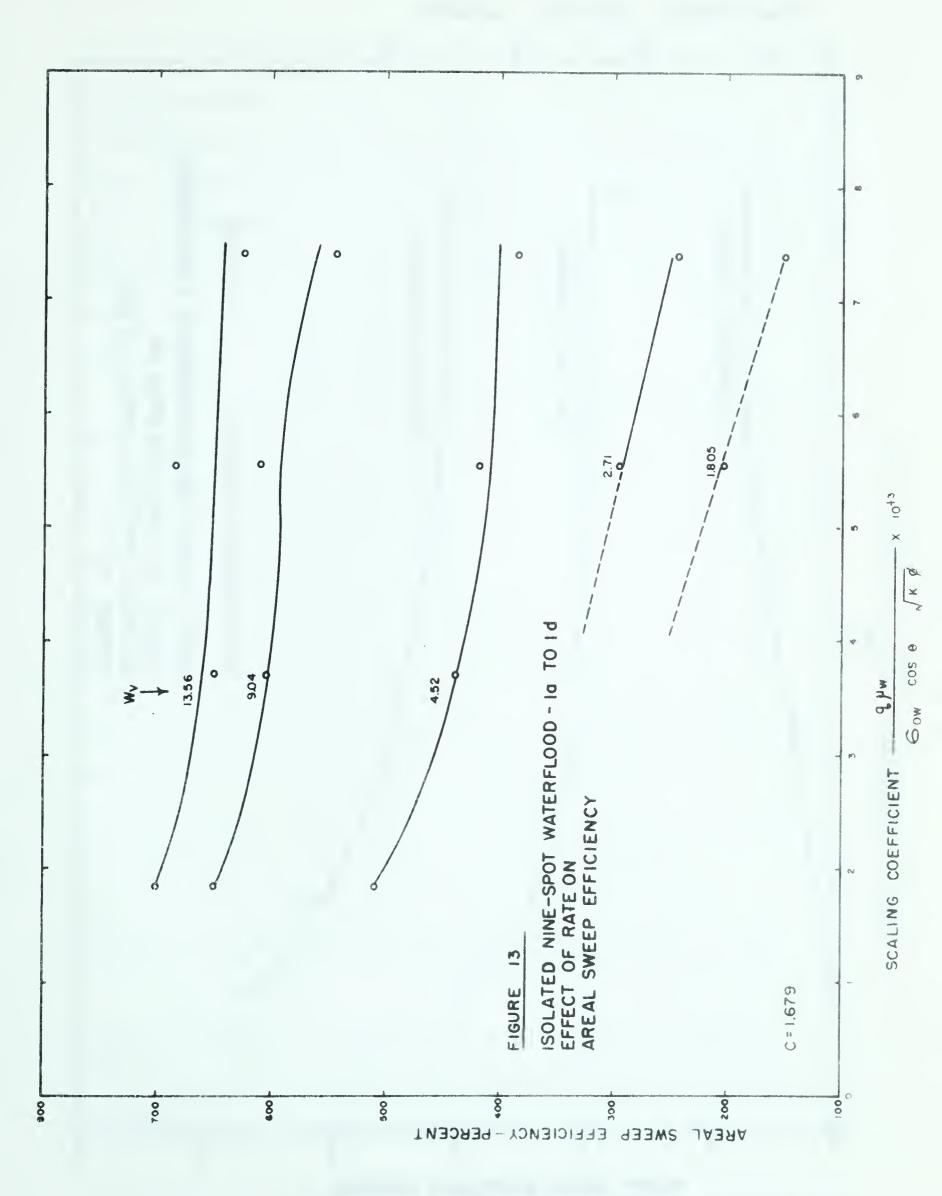




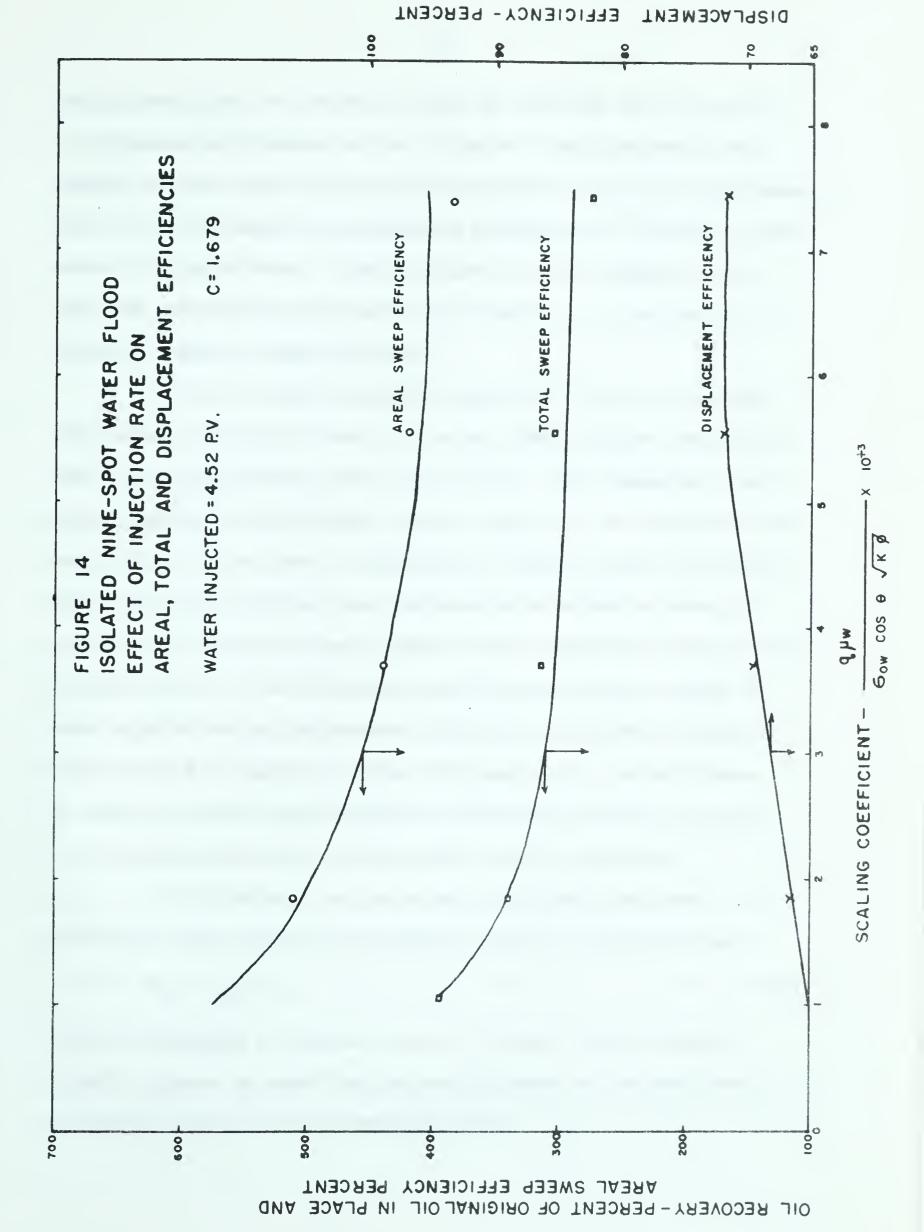














scaling coefficient are constant except the injection rate, therefore, it represents only changes in rate. Figures 9 and 13 represent the changes in areal sweep efficiency with injection rate for the two floods. Figure 10 shows changes in displacement efficiency as a function of the volume of injected water. Finally, Figure 11 and 14 compare areal, total and displacement efficiencies as a function of injection rate at 4.52 pore volumes of water injected.

As can be seen from Figures 8 and 12 oil recovery decreases with increasing injection rate up to a point where further increases in rate do not significantly affect oil recovery. This phenomena is much more pronounced in flood Series 3 than in Series 1. An explanation for this will be offered later. Examination of figures 9 and 13 discloses that areal sweep efficiency also decreases with increasing rates of injection and then stabilizes. Again the most significant changes occur in Flood Series 3. The effect that injection rate and the volume of water injected has on displacement efficiency is depicted in Figure 10. Figures 11 and 14 compare all three efficiencies for the two floods. In these two figures the displacement efficiency is seen to increase with injection rate up to a certain point and then stabilize.

It is important to note at this point that the three efficiencies are related, as pointed out earlier, by the following:

$$E_{s} = E_{as} \times E_{d} \tag{6}$$

Further examination of Figures 11 and 14 indicate that the rate of injection appears to exert the greatest influence on the areal sweep efficiency, making it the controlling factor.



Discussion

In both series of floods employed to study the effect of rate on the behavior of water flooding, the displacement efficiency (E_d) followed a pattern which has been put forth by several authors. (12,18,21) That is the displacement efficiency increased with the rate of injection up to a point where further increases in rate caused no further significant changes. (See Figures 11 and 14).

In studies by Rapoport, (21) Newcombe (18) and Kyte, (12) conducted on linear systems, all authors found that oil recovery (oil recovery is equivalent to displacement efficiency in a linear system since the areal sweep is 100%), increased with increasing rate up to a point where further rate increases resulted in no additional recovery. This behavior was found to hold true for both preferentially oil-wet and water-wet systems, provided capillary end effects were absent.

This phenomena of increasing displacement efficiency (or oil recovery for linear systems) with increasing injection rates in waterwet systems may be explained by the tendency of water to imbibe into the smaller, tighter channels. (18) At low flood rates, flow channels are established by imbibition through the smaller channels. At slightly higher rates more water pushes into larger channels as the flow capacity of the imbibition channels are exceeded. At still higher rates more injected water is carried by the larger channels with the result that

^{*} At low rates it would appear at first that both large and small channels would be flooded. However if the rate of imbibition is as great or greater than the rate at which water is being injected then all the water would flow through the smaller channels by-passing large channels.



some oil is trapped and by-passed in the tight channels. The maximum displacement efficiency occurs then at the injection rate where water flows at the same rate of linear advance through both large and small channels. Hence an optimum rate occurs at which displacement efficiency is a maximum. This has been reported by Maguss, (15) Pritchard (20) and Jones-Parra.

All literature is not in agreement with the above statements. Results of decreasing oil recovery (displacement efficiency) with increasing rates has been reported. (10,11) However, in all of these cases high oil-water viscosity ratios were involved. This behavior of decreasing displacement efficiency with increasing rate was attributed to fingering. Viscous fingering results from the situation that the inlet saturation distribution does not reach equilibrium at high rates. At low rates the capillary forces which tend to distribute the injected water over the entire cross-sectional area of a core or over the entire thickness of a bed are significant and prevent uneven saturation distribution at inlet conditions in high viscosity floods.

In the event that the subject flow system had been oil-wet a different explanation, as to the effect of rate on displacement efficiency, would have been necessary. In oil-wet systems water does not imbibe but must be forced into all flow channels. Less pressure is required to penetrate large channels, than small channels. At low rates water flows through large channels, while higher rates result in penetration of smaller channels. As a result displacement efficiency increases with rate. Displacement efficiency will increase with rate until the imposed pressure gradient is larger than the capillary pressure gradient which prevents water from entering small flow channels at low



rates. Once the capillary forces are overcome the displacement efficiency should stabilize.

Figure 10 also indicates that displacement efficiency increases with rate. In addition it discloses that displacement efficiency decreases as the volume of water injected increases for any particular flood. This decrease in displacement efficiency with increasing water injection continues until the flood front reaches the exterior boundary of the model. Once the exterior boundary is contacted the displacement efficiency begins to increase with increases in the volume of injected water. All six floods represented in Figure 10 follow this pattern.

Figures 9 and 13 indicate that areal sweep efficiency is greatly affected by the rate of injection. Both series of floods exhibited decreasing areal sweep efficiency with increasing rate up to a maximum rate, after which, further increases in rate do not affect the area swept.

As pointed out previously in the discussion on "displacement efficiency" it is believed that imbibition is the controlling factor at low rates in water-wet systems. If this fact is accepted as true, then it must be concluded that this imbibition phenomena is the reason for the very high areal sweep efficiency at low rates. The high oil recoveries (measured), also experienced at low rates, (oil recovery also decreased with increasing rate - See Figure No. 8 and No. 12) indicate that the sand pack was of a homogeneous nature, being composed of a high percentage of small uniform flow channels favorable for imbibition.



Increases in flood rates increase the "displacement efficiency" by pushing more water into larger channels, thus limiting the amount of water available for the smaller channels and providing a more uniform distribution of water throughout the bed. This occurrence leads directly to a reduction in areal sweep efficiency. The large amount of subordinate production at low rates also indicates that the displacement efficiency was initially low during floods conducted at low rates.

As can be seen from Figures 9 and 13 the water flood series conducted with the higher oil-water viscosity ratio (Series 3) exhibits a greater reduction in areal sweep efficiency per unit increase in the rate of injection, than the low viscosity floods (Series 1). This point can be explained as follows. A study by P.M. Blair (See Reference 6, page 165) disclosed that imbibition is not only a function of wettability but also of the viscosity ratio of the fluids employed. Blair has shown that imbibition is more complete (ie: penetrates more of the flow channels) for low viscosity fluids than for high viscosity fluids. Therefore it can be stated that in the case of the low oil-water viscosity floods (Series 1) the majority of the flow channels are flooded at the low injection rates. Thus increases in injection rates will provide only a small increase in displacement efficiency. In the case of the high viscosity floods (Series 3) the imbibition process is not as complete due to the high oil viscosity; consequently, increases in injection rates cause a greater percentage of flow channels to be flooded resulting in a faster increase in displacement efficiency and hence a faster decline in areal sweep efficiency. The larger subordinate production in the high viscosity series (see Figure 8 at low rates) as



compared to the subordinate production in low viscosity floods (See Figure 12) also indicates that spontaneous imbibition is not as complete in the high viscosity floods as in the low viscosity floods.

Since all three efficiencies are related by the following expression:-

Oil Recovery = E_{as} x E_{d} x P.V. of unit area (5) it is understandable that a particular behavior in one will be reflected in the others. It is obvious from the figures 11 and 14 that the imbibition phenomena or capillary forces exhibited a far greater influence on areal sweep efficiency than it did on displacement efficiency during the subject tests. As a consequence the resulting oil recovery (E_{s}) followed the pattern set by the behavior of the areal sweep efficiency term. That is, oil recovery decreased with increasing rate. This is contrary to results reported by Rapoport. (23) Rapoport's publication is the only known report which has investigated the effect of rate on oil recovery in two-dimensional systems. The fact that the system used by Rapoport was oil-wet is considered to be the reason that oil recovery increased with increasing injection rates rather than decrease, as was the case in the subject study.

In the water-wet system employed in this study, imbibition is considered as the reason for the very high areal sweep efficiencies and consequently the high oil recovery at low rate. Since water does not imbibe into oil-wet system but must be forced into all flow channels it is reasonable to assume that areal sweep efficiency should increase with increasing rate rather than decrease. Therefore with both areal sweep efficiency and displacement efficiency increasing with increasing injection



rate, oil recovery must follow the same pattern.

Re-examining the figures connected with this critical rate study indicates that Flood Series 3 stabilizes at approximately 12.1 B/D/ft (1680 cc/hr) which corresponds to a critical scaling coefficient of 5.4 x 10⁻³. Flood Series 1 appears to stabilize between 4.05 B/D/ft (560 cc/hr) and 8.1 B/D/ft (1120 cc/hr) which corresponds to a critical scaling coefficient of 2.8 x 10⁻³. It is interesting to note at this point that the above mentioned values of the critical scaling coefficient are approximately the same magnitude as those reported by Rapoport (23) (ie: between 3.5 x 10⁻³ and 7.4 x 10⁻³).

The fact that the two critical rate are different was expected. One of the basic principles of the concept of a critical scaling coefficient is that it applies only to systems with the same viscosity ratio. Thus, if the viscosity ratio changes, the rate at which a flood stabilizes must also change.

PRODUCTION AND INJECTION HISTORY

Results

Six floods were selected for use in the final correlations. They are identified as follows:

Flood No. 1-c - Oil-water viscosity ratio of 1.68

Flood No. 2 - Oil-water viscosity ratio of 3.25

Flood No. 3-d - Oil-water viscosity ratio of 6.27

Flood No. 4 - Oil-water viscosity ratio of 8.01

Flood No. 5 - Oil-water viscosity ratio of 12.41

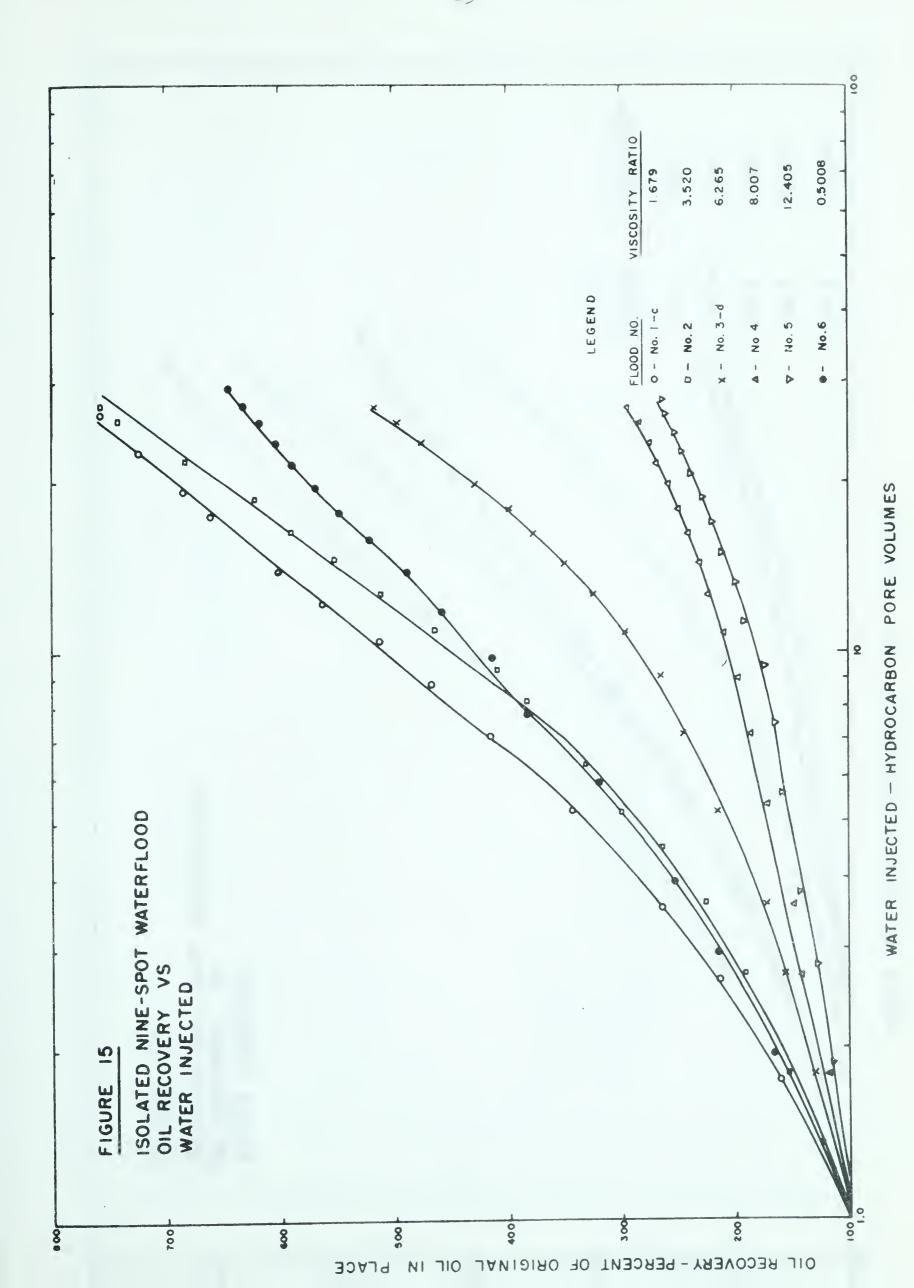
Flood No. 6 - Oil-water viscosity ratio of 0.5007



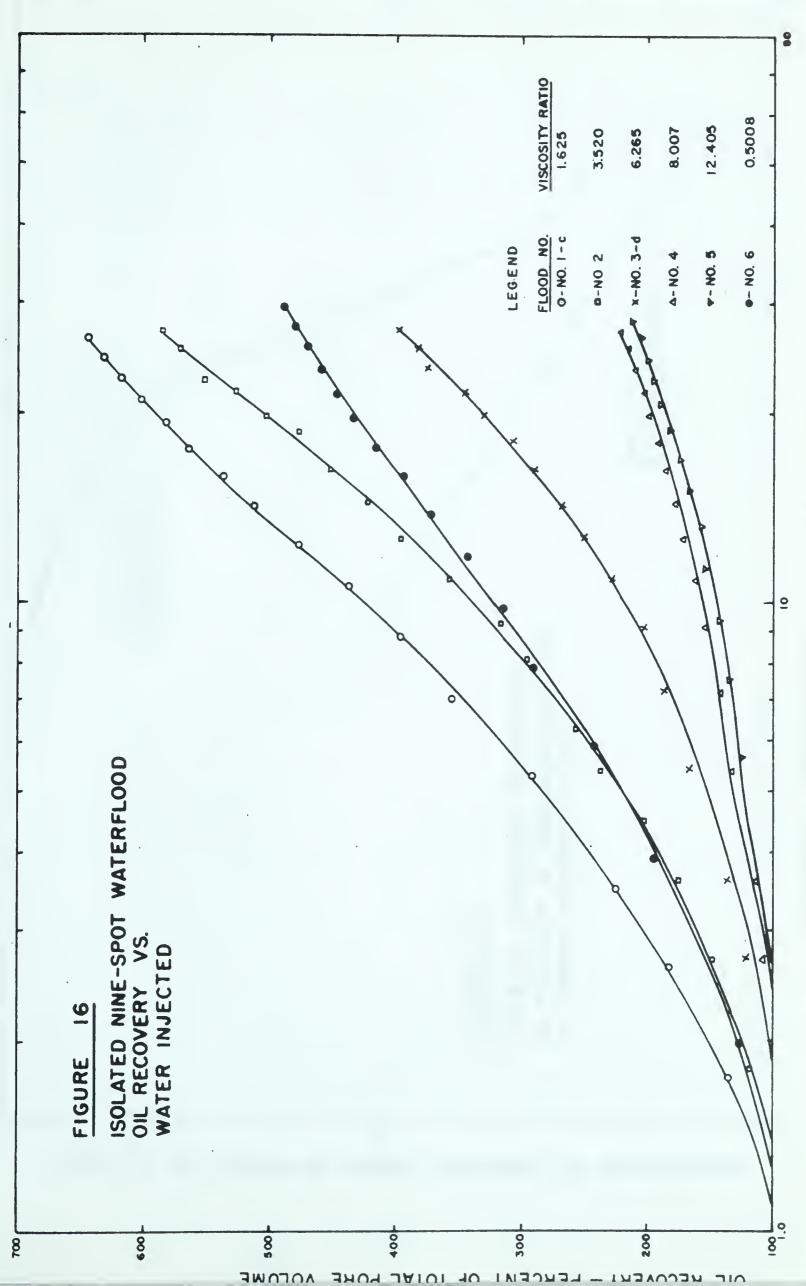
The production histories of the above floods are presented in Tables 7, 10, 14, 17, 18 and 19 respectively. Figures 15 and 16 present the oil recovery as a function of the viscosity ratio and volume of water injected for the various floods. Figure 15 expresses oil recovery as a percent of the original oil in place in the unit pattern. Figure 16 expresses oil recovery as a percent of the total pore volume of the unit pattern. Figures 18 to 23 inclusive show the producing water-oil ratio versus volume of oil recovered and volume of water injected. (See Appendix A).

Figures 15 and 16 disclose that oil recovery decreases with increasing oil-water viscosity ratio for any particular volume of water injected. The one exception to this pattern is Flood No. 6. The deviation of this flood will be explained later. Total recovery, after approximately 25 pore volumes of water were injected, varies from 750% to 260% of the original oil in place in the unit pattern. Since the effect of the viscosity ratio on oil recovery to water breakthrough is not discernable from Figures 15 and 16 another plot was employed. Figure 17 presents oil recovery at breakthrough versus the oil-water viscosity ratio. (Data presented in Table 34) Breakthrough recovery for both the direct offset and diagonal offset wells are represented. Both sets of wells indicate that oil recovery decreases with increasing oil-water viscosity ratio. Breakthrough recovery (at direct offsets) varies from 98.5% to 54.9% of the original oil in place over the viscosity range studied.









WATER INJECTED - HYDROCARBON PORE VOLUMES



OIL - WATER VISCOSITY RATIO



Discussion

The phenomena of decreasing oil recovery with increasing oilwater viscosity ratio can be theoretically explained by referring to the
simplified Buckley-Leverett (3) fractional-flow formula for water:

$$f_{W} = \frac{1}{1 + \frac{K_{O}\mu_{W}}{K_{W}\mu_{O}}}$$
 (10)

where f_w is the fraction of water flowing in the total flow stream. Other terms are as defined previously. Any increase in the oil viscosity results in a reduction in magnitude of the denominator thus increasing the fraction of water flowing in a system at any given saturation of the invading fluid. This behavior has been known since the early days of petroleum engineering and is an accepted fact.

All floods followed the above pattern except Flood 6. In order to conduct this flood under a favorable mobility ratio, glycerol was added to the injection water increasing the viscosity to three times that of the water employed in the other floods. According to Rapoport (23) an increase in the viscosity of the displacing phase results in a corresponding decrease in the rate of injection necessary for stabilization. This factor was not taken into consideration and thus inadvertently Flood 6 was conducted at a rate three times the rate indicated by the critical rate study. By employing such a high rate oil was trapped in the smaller channels resulting in oil recoveries which were too low. Consequently the results of Flood 6 are unrepresentative and therefore have been excluded from the remainder of the report.



Examination of the water-oil ratio graphs (Figure 18 to 23) indicate that a scattering of data points exists. This scattering tends to become worse as the oil-water viscosity ratio increases. This behavior can be explained by the fact that as the oil-water viscosity ratio increases the flood front becomes more irregular and even slight fingering occurs. This tends to produce irregular behavior of the water-oil ratio.

AREAL SWEEP EFFICIENCY

Results

Data obtained on areal sweep efficiency as a function of mobility ratio and volume of water injected is presented in Tables 22, 24, 28, 31, 32 and 33 and Figures 24 to 27 inclusive. The tabulated data consists of measured areal sweep efficiency figures, calculation of displacement efficiency and mobility ratio.

Figure 24 illustrates areal sweep efficiency at breakthrough versus the mobility ratio. Two curves, one representing breakthrough as it occurred at the direct offset wells and the other representing breakthrough at the diagonal offset wells, are shown. Figure 25 shows areal sweep efficiency as a function of mobility ratio and the number of pore volumes of water injected. This plot has been patterned after the work of Dyes. (9)

Figures 26 and 27 present areal sweep efficiency as a function of total volume injected as compared to the volume injected to breakthrough, $(Q/Q_{\rm BT})$ with the viscosity ratio being the parameter. The breakthrough volume in Figure 26 is the volume of fluid injected before



BREAKTHROUGH - PERCENT

EFFICIENCY

TA

SMEE

AREAL

MOBILITY - RATIO

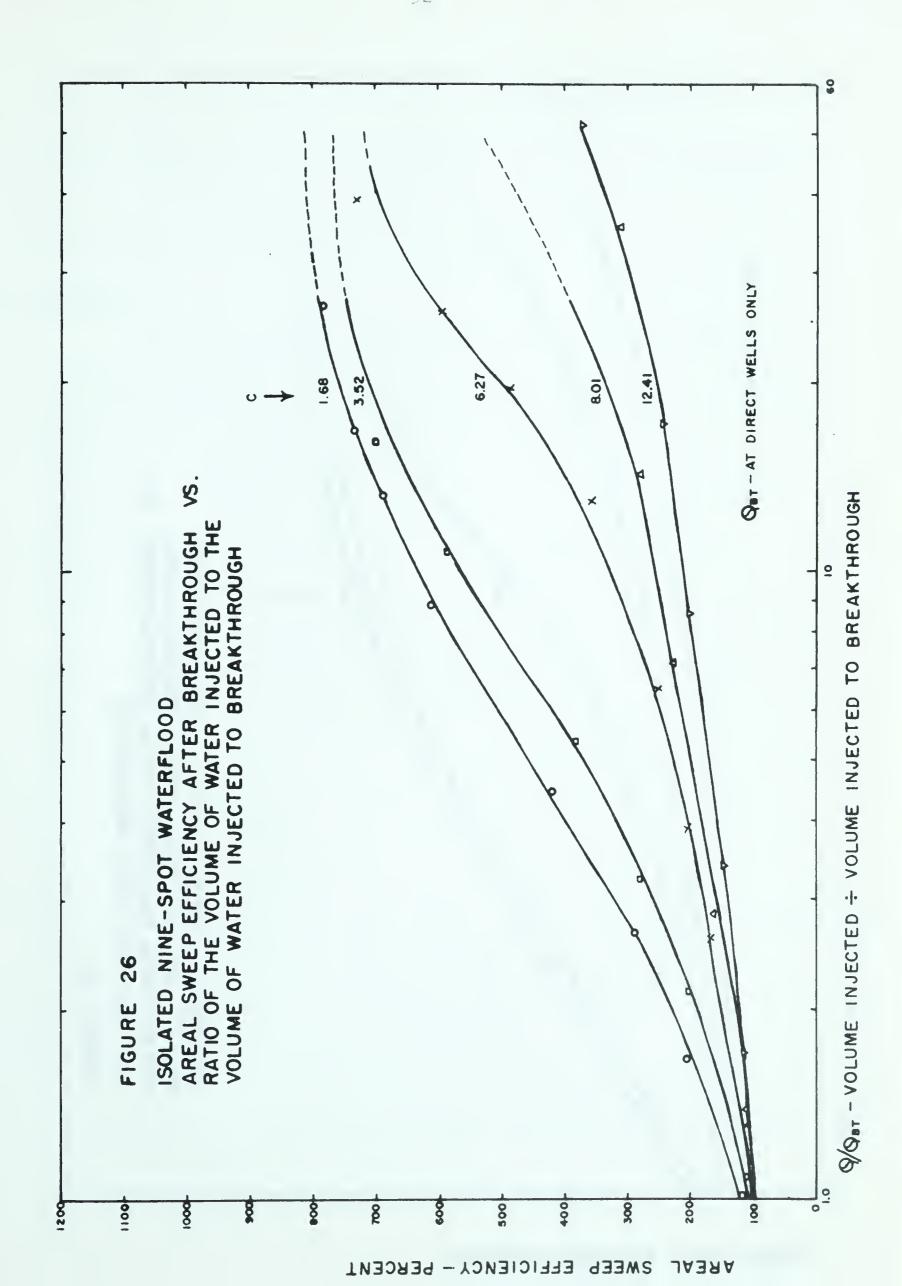


SMEEP EFFICIENCY - PERCENT

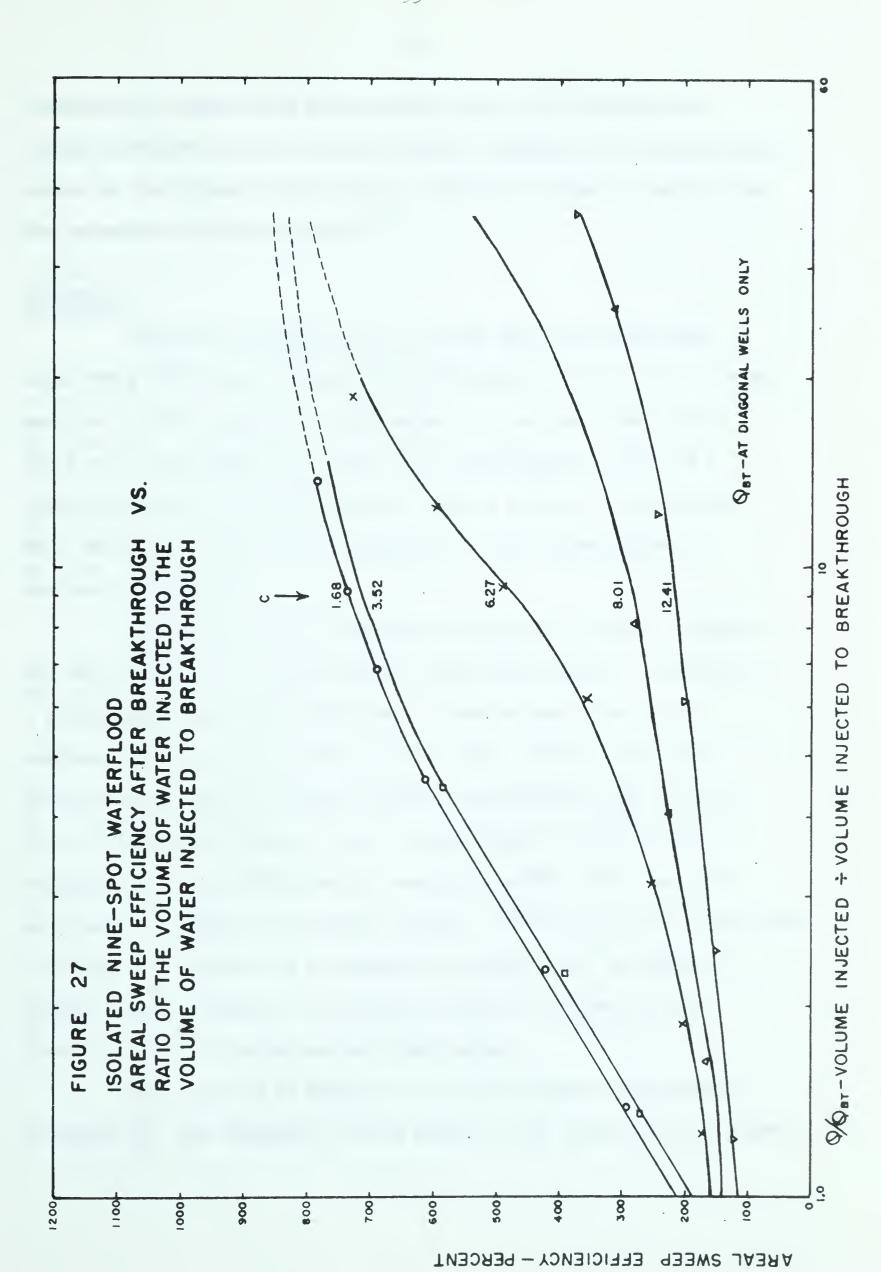
AREAL

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breakthrough occurs at the direct offset wells. The breakthrough volume in Figure 27 is the volume of fluid injected before breakthrough occurs at the diagonal offset wells. This type of plot is adapted from the procedure outlined by Craig. (7)

Discussion

Referring to Figure 24, it is seen that the breakthrough areal sweep efficiency increases with decreasing mobility ratio. Since mobility is often referred to as a measure of the ease with which a fluid will flow through the rock, it is understandable then that a larger area will be contacted by the injected fluid as the mobility ratio decreases. This type of behavior has been substantiated by numerous other authors.

Due to the lack of published literature on isolated systems it was very difficult to obtain data for comparison purposes. According to a confidential data source there are no results available for an isolated nine-spot such as used in this study. However, data was obtained on a confined nine-spot pattern (confidential data source). The areal sweep efficiency at water breakthrough for unit mobility, considering the direct offset wells, was given as 80%. This compares to a value of 120% from the subject system. However, since the comparison is between an isolated and a confined system and since the method of analysis used to evaluate the confined pattern is unknown, it is doubtful if the collation has any significance.

The same type of behavior as noted in Figure 24 is repeated in Figure 25. The parameter in this figure is the number of pore volumes

of injected water. Although high ultimate sweep out patterns are obtained for most mobility ratios, Figure 25 illustrates that considerably more area is swept at lower mobilities than at high mobilities for the same volume of water injected. Thus, from an economic standpoint the rate of oil recovery and the total amount of fluid to be injected cause the lower mobility floods to be much more favorable.

Figures 26 and 27 are essentially the same as Figure 25. The only difference is that the volume injected is expressed as Q/Q_{BT} and is plotted as the ordinate instead of being utilized as a parameter. The mobility ratio varies during a flood hence it could not be used as a parameter and therefore the viscosity ratio was introduced. As pointed out previously the difference between Figures 26 and 27 is in the definition of the volume injected to breakthrough. Both graphs yield identical results and thus either one can be used. This is clearly illustrated by the following example.

Assuming that the oil-water viscosity ratio of a hypothetical reservoir is approximately 3.52 and that the volume injected before breakthrough at the direct wells is 61.6 and at the diagonal wells is 128.5. The areal sweep efficiency at $Q/Q_{BT}=10.0$ is 330% from Figure 27. The total volume injected up to this time is 10 x 61.6 or 616. Thus the equivalent Q/Q_{BT} for the diagonal offset plot is 616 ÷128.5 or $Q/Q_{BT}=4.8$. The areal sweep efficiency at $Q/Q_{BT}=4.8$ for a 3.5 oil-water viscosity ratio (from Figures 27) is 320%. Thus, both figures yield approximately the same results.

Further examination of either Figure 26 or 27 discloses that the top three curves in both figures appear to be levelling off or



reaching a maximum. This levelling off can be attributed to a boundary effect. Up until this point the bed has acted essentially as an infinite reservoir. It is noticed that these three curves tend to level off at the same value of areal sweep efficiency ie: 650%. Reconverting this into areal coverage yields an area, which if considered as a circle, has a diameter approximately equal to the dimension of the model. The bottom two curves (ie: high viscosity floods) have not yet shown signs of levelling off. This is due to the fact that the areal coverage of the injected fluid has not as yet extended to the outer edge of the model.

PRACTICAL APPLICATION

In determining the economic worthiness of a secondary recovery project, the area of the reservoir which will be swept by the invading fluid is of great importance. Most literature pertaining to sweep efficiency has emphasized the pattern which is obtained at breakthrough of the invading fluid. However, the increase in areal sweep efficiency which occurs after breakthrough has been demonstrated to be of significant proportions. (7,9,17) This is particularly true in the case of an isolated system, as is demonstrated by the subject report. Thus, to accurately determine the economics of a system, one must know the sweep efficiency at breakthrough and also the continual enlargement of the pattern which occurs during production after breakthrough.

The data presented in the subject report can be applied to water flood calculations by using the technique proposed by Craig. (7)



This procedure utilizes Welge's (25) method in conjunction with laboratory data obtained on areal sweep efficiency after breakthrough for a five-spot pattern. By using Figures 24 and 26, to determine the manner in which the areal sweep efficiency changes with continued water injection, the calculations can be revised for an isolated nine-spot pattern.

It is also important to realize that the data obtained from the model used in this study represents a steady state injection operation in an entirely liquid filled reservoir. (ie: no free gas, above bubble point). In addition the model represents a reservoir of constant thickness with impermeable barriers above and below the producing zone. The porous media being represented by a unconsolidated sand pack with uniform permeability and porosity. The data presented only illustrates the effect of mobility ratio and volume of water injected on areal sweep efficiency. All other factors are constant.



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CONCLUSIONS

Treatment of water flood behavior in two-dimensional systems as encountered in the reservoir can best be studied by scaled flow model experiments. In the displacement of oil by water in these two-dimensional flow systems capillary forces are of paramount importance. In all cases, results obtained by this approach must be attained under conditions in which the water-oil displacement is no longer influenced by capillary effects.

The results of this study led to the following conclusions:

- l. The most important factor in scaling an oil field reservoir was found to be the capillary effects. This study has shown that for sufficiently high injection rates the flooding behavior can be expected to be rate independent or stabilized. Only under stabilized conditions can laboratory results be utilized for field evaluations.
- 2. The study of the effect of injection rate on the performance of a water-wet two-dimensional system has shown that oil recovery decreases with increasing rate until stabilized conditions are obtained.
- 3. Area much in excess of the unit pattern is swept by the invading fluid when production is continued to high water-oil ratios.
- 4. Oil recoveries far exceeding the amount of oil originally in place in the unit pattern is produced when production is continued to high water-oil ratios.
- 5. Lower oil recoveries and smaller areal coverage occurs when more viscous oils (ie: higher mobility ratio) are used as the displaced phase.



- 6. High ultimate sweep out patterns were obtained for all mobility ratios studied. However, considerably more area is swept at lower mobilities than at high mobilities for the same volume of water injected. Therefore from an economic standpoint the lower mobility floods are much more favourable.
- 7. This study has shown that isolated floods are very much different than confined water floods. Therefore it is essential that when a water flood development is under study recognition of the difference between the two patterns is imperative.
- 8. At high water-oil ratios, sufficient reservoir has been swept so that the isolated model pattern no longer acts as if it were an infinite reservoir and boundary effects influence the performance.



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APPENDIX A



Table 1

CALCULATION OF ABSOLUTE PERMEABILITY

Muskat's Equation:

$$Q = \frac{0.003541 \, \Delta \, P \, K \, h}{\mu_W \, \beta \, \left[\log \, d/r_W - 0.619 \right]}$$

For five-spot pattern.

where:

Q - injection rate in B/D

 ΔP - pressure differential in psi

K - permeability in millidarcys

h - formation thickness in feet

 $\boldsymbol{\mu}_{\boldsymbol{W}}$ - water viscosity in centipoises

 β - formation - volume factor (1)

d - distance from injection well to producing well in feet

r_w - well bore radius in feet

Model and Fluid Characteristics:

Q = 0.278 B/D
$$K = \frac{0.278 \times 1.0 \times 0.8837 \times (4.92 - .619)}{0.003541 \times 0.520 \times 0.0208}$$

h = 0.0208 ft $K = \frac{43,500 \text{ md}}{6}$
 $\mu_{W} = 0.8837 \text{ cp}$

Compares favorably with Pritchard's (20)

 $\mu_{W} = 1.0$
 $\mu_{W} = 4.92$



Table 2

GEOMETRIC AND RESERVOIR PROPERTIES OF THE MODEL

Length 32 inches

Width 32 inches

Thickness 1/4 inch

Length (Unit Area) 8 inches

Porosity Pack I - 44.07%

Pack II - 40.75%

Total Pore Volume of Unit Area Pack I - 115.55 cc

Pack II - 106.85 cc

Scaling Coefficient "C2" * Pack I - q x 4.58 x 10⁻⁴

Pack II - q x 4.42 x 10-4

*
$$c_2 = \frac{q \mu_W}{\sigma_{oW} \cos \Theta \sqrt{K \emptyset}}$$

where C_2 is employed on graphs

q - B/D/ft

 $\mu_{\mathbf{w}}$ - cp

 σ_{ow} - dyne/cm

K - md

Ø - fraction

 Θ - taken as 60°



Table 3

FLUID PROPERTIES

Flood No.	Visco Oil	water	Dens Oil	ity Water	Interfacial Tension
1	1.595	0.95	0.8098	1.000	32.14
2	3.342	0.95	0.8311	1.000	32.04
3	5.592	0.95	0.8463	1.000	31.34
4	7.607	0.95	0.8209	1.000	29.63
5	11.786	0.95	0.8469	1.000	32.04
6	1.595	3.185	0.8098	1.094	30.17

Viscosity is in centipoises

Density is in grams/cc

Interfacial tension is in dynes/cm



Table 4

Production History - Nine-Spot Flood I

Inject	ion Rate = 3	20 cc/hr	$S_{cw} = 20$	0.70% μ	o = 1.595
(1)	(2)	(3)	(4)	(5)	(6)
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Inst. W.O.R.	Oil Rec. in Hydro. P.V.	•
80 160 240	1 17 30	79 143 210	0.00125 0.250 0.194	0.945	0.945 1.895
320 400	46 66	27 ¹ 4 33 ¹ 4	0.250	3.24	3.78
480 560	91 123	389 437	0.455	4.60	5.67
640 720	156 214	484 506	0.703	5.72	7.57
800 880	271 3 3 4	529 546	2.480 3.700	6.25	9.45
960 1040	402 473	558 567	5.650 7.890	6.60	11.35
1120 1200	545 618	575 582	9.000	6.80	13.25
1280 1360	692 767	588 593	12.320 15.000	6.95	15.18
1440 1520	843 919	597 601	19.000	7.06	17.00
1600 1680	995 1072	605 608	19.000 25.650	7.15	18.92
1760 1840	11 ¹ 47 1222	613 618	15.000	7.25	20.08
1920 2000	1301 1378	619 622	79.000 25.650	7.26 7.40	22.70 24.60
2080 2160	1455 1532	625 628	25.650 25.650 39.000	7.44	26.50
2240 2320 2400	1610 1689 1768	630 631 632	79.000	7.48	28.40

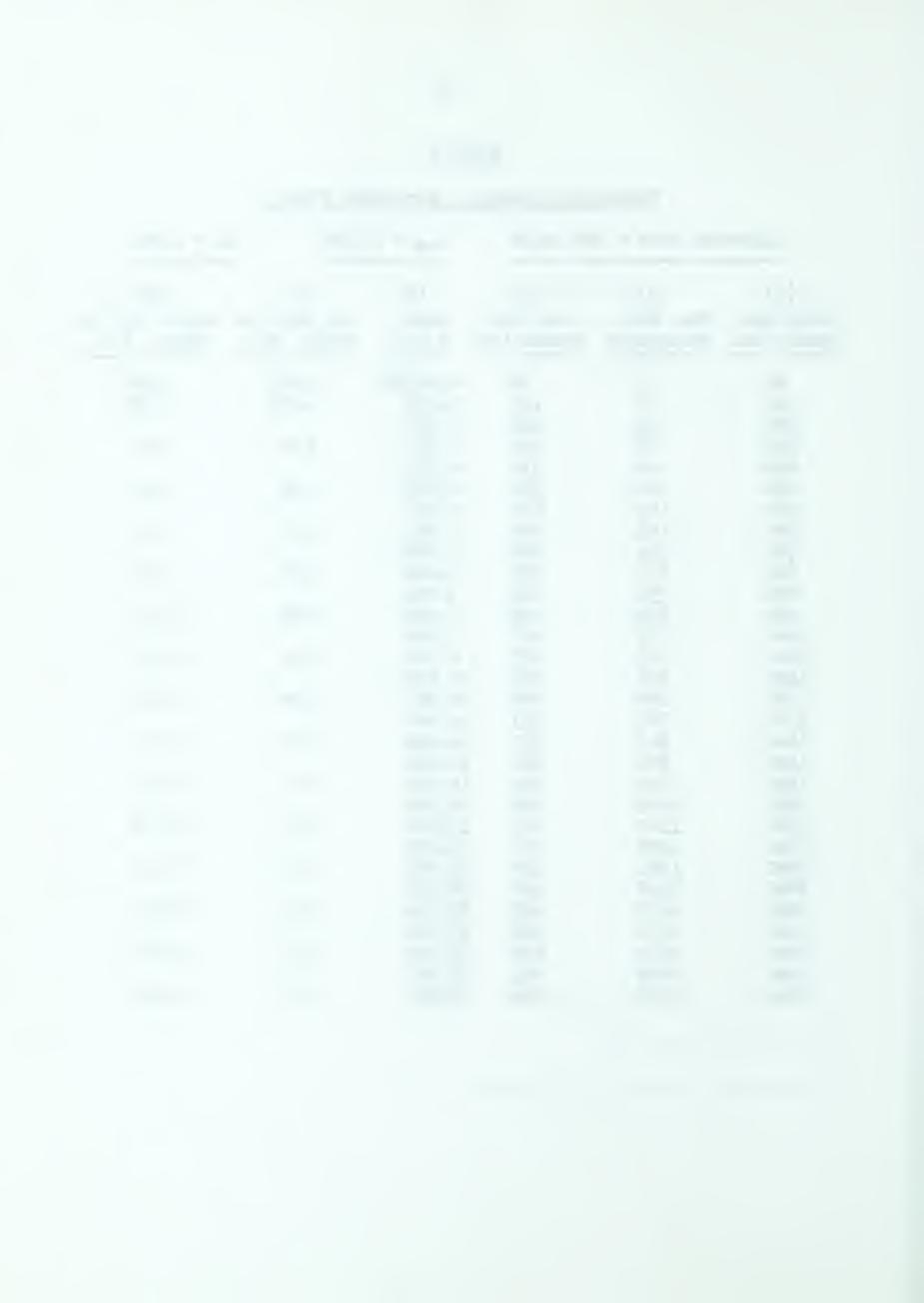


Table 5

Production History - Nine-Spot Flood I-a

Injection Rate = 560 cc/hr		$S_{cw} = 19$	$S_{cw} = 19.69\%$ $\mu_0 = 1.595$		
(1) Total Cum.	(2) Cum. Str.	(3) Cum. Oil	(4) Inst.	(5) Oil Rec. in	(6) Water Inj. in
Production	Production	Production	W.O.R.	Hydro. P.V.	Hydro. P.V.
80 160 240	25 48	80 135 192	0.000 0.455 0.404	0.932 1.575	0.932 1.870
320 400	79 111	241 289	0.632	2.81	3.72
480 560	145 184	335 376	0.738	3.90	5.60
640 720	232 2 8 3	408 437	1.500 1.760	4.76	7.46
800 880	3 38 398	462 482	2.200	5.37	9.32
960 1040	461 528	499 512	3.710 5.150	5.82	11.20
1120 1200	593 665	527 535	4.330 9.000	6.15	13.05
1280 1360	736 808	544 552	7.890 9.000	6.33	14.95
1440 1520	881 955	559 565	10.400	6.52	16.75
1600 1680	1030 1105	570 575	15.000 15.000	6.65	18.70
1760 1840	1181 1257	579 583	19.000 19.000	6.75	20.50
1920 2000	1332 1409	588 59 1	15.00 25.650	6.85	22.40
2080 2160	1485 1561	595 599	19.00 19.00	6.93	24.22
2240 2320	1639 1717	601 603	39.00 39.00	7.00	26.10
2400	1795	605	39.00	7.05	28.00

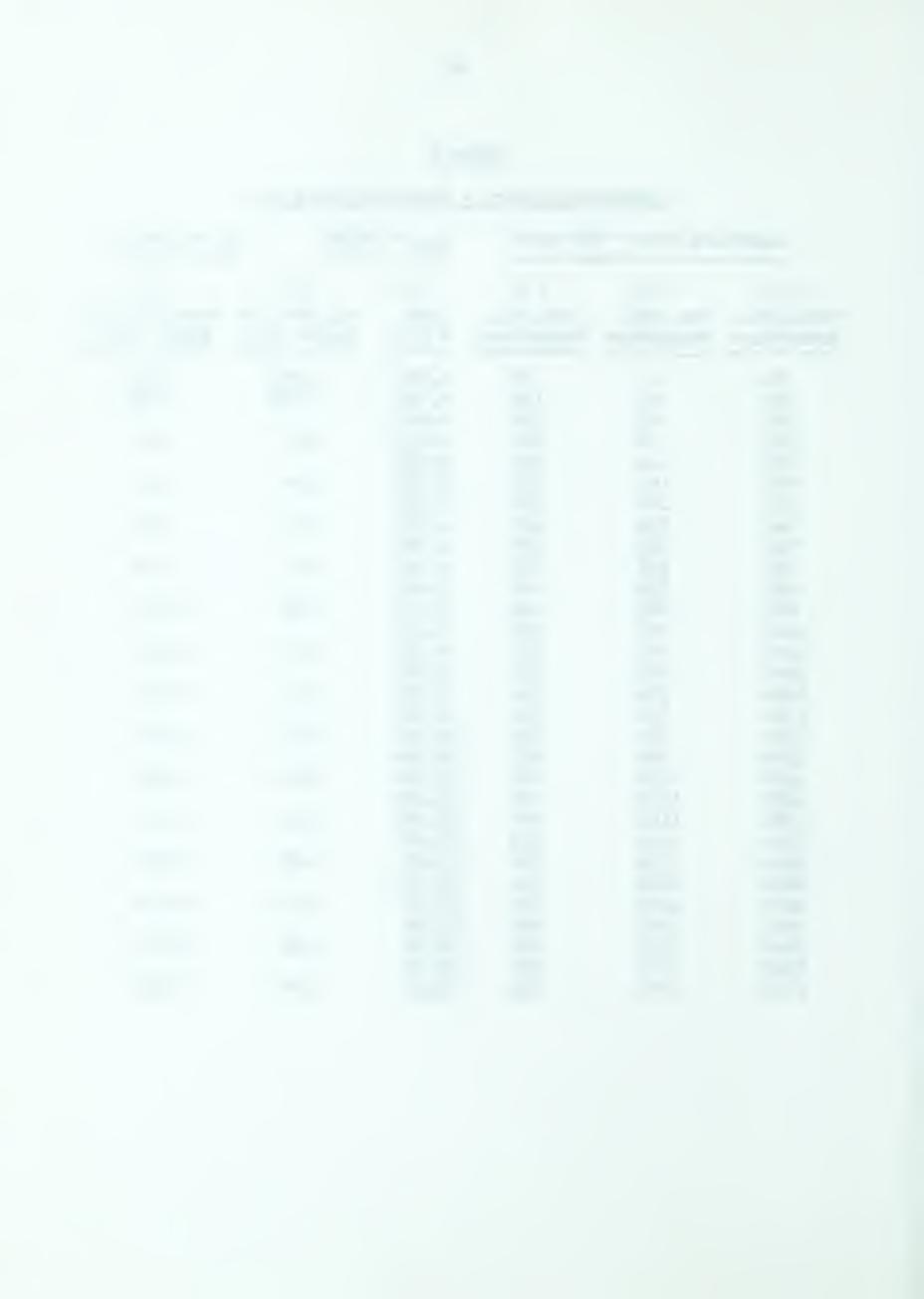


Table 6

Production History - Nine-Spot Flood I-b

Injection Rate = 1120 cc/hr		$S_{cw} = 17$	7.25% µ	o = 1.595 cp	
(1)	(2)	(3)	(4)	(5)	(6)
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Inst. W.O.R.	Oil Rec. in Hydro. P.V.	Water Inj. in Hydro. P.V.
80 160	18	80 142	0.000	0.9025	0.9025
240 320 400	43 79 123	197 241 277	0.455 0.819 1.221	2.72	3.61
480 560	162 206	318 354	0.952	3.59	5.42
640 720	257 31 0	383 410	1.760	4.32	7.22
800 880	367 424	433 456	2.480	4.89	9.03
960 1040	483 546	477 494	2.810	5.375	10.83
1120 1200	608 674	512 526	3.440	5.78	12.65
1280 1360	739 807	541 553	4.330 5.660	6.11	14.50
1440 1520	878 948	562 572	7.890 7.000	6.34	16.25
1600 1680	1018 1089	582 591	7.000 7.890	6.57	18.09
1760 1840	1164 1238	596 602	15.000 12.320	6.73	19.89
1920 2000	1311 1385	609 615	10.400	6.86	21.70
2080 21.60	1460 1535	620 625	15.000 15.000	7.00	23.56
2240 2320	1610 1687	630 633	15.000 25.650	7.11	25.25
2400	1761	639	12.320	7.21	27.10

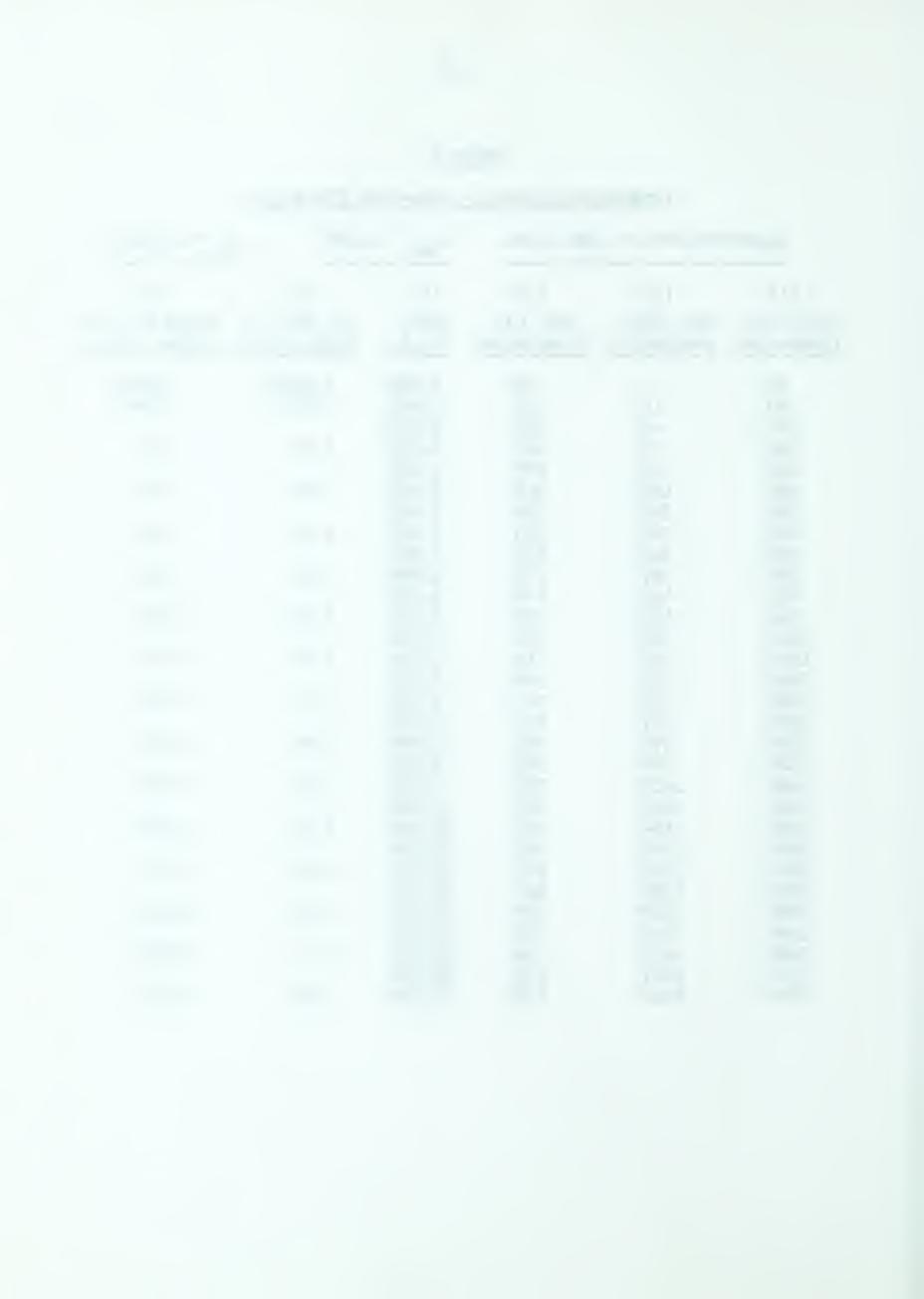


Table 7

Production History - Nine-Spot Flood I-c

Inject	ion Rate = 1	680 cc/hr	$S_{cw} = 15$	$S_{cw} = 15.07\%$ $\mu_0 = 1.595 \text{ cp}$		
(1) Total Cum. Production	(2) Cum. Wtr. Production	(3) Cum. Oil Production	(4) Inst. W.O.R.	(5) Oil Rec. in Hydro. P.V.	(6) Water Inj. in Hydro. P.V.	
80 160 240	 14 44	80 146 196	0.000 0.212 0.600	0.879	0.879 1.760	
320 400	78	242	0.740	2.66	3.51	
480	123 167	277 313	1.220	3,44	5.27	
560 640	213 261	347 379	1.352	4.16	7.04	
720 800	31.7 3 7 5	403 425	2.330 2.630	4.67	8.79	
880 960	432 484	448 476	2.480	5.13	10.55	
1040 1120	545 609	495 511	3.210	5.62	12.30	
1200 1280	670 733	530 547	3.210 3.710	6.00	14.10	
1360 1440	799 867	561 573	4.000 5.650	6.30	15.80	
1520 1600	935 1001	585 599	5.650 4.700	6.59	17.60	
1680 1760	1068 1138	612 622	5.150 7.000	6.84	19.35	
1840 1920	1210 1278	630 642	9.000 5.650	7.05	21.10	
2000 2000	1350 1421	650 659	9.000	7.24	22.85	
21.60 2240	1493 1566	667 674	9.000	7.40	24.60	
2320 2400	1642 1712	678 688	19.000	7.56	26.40	

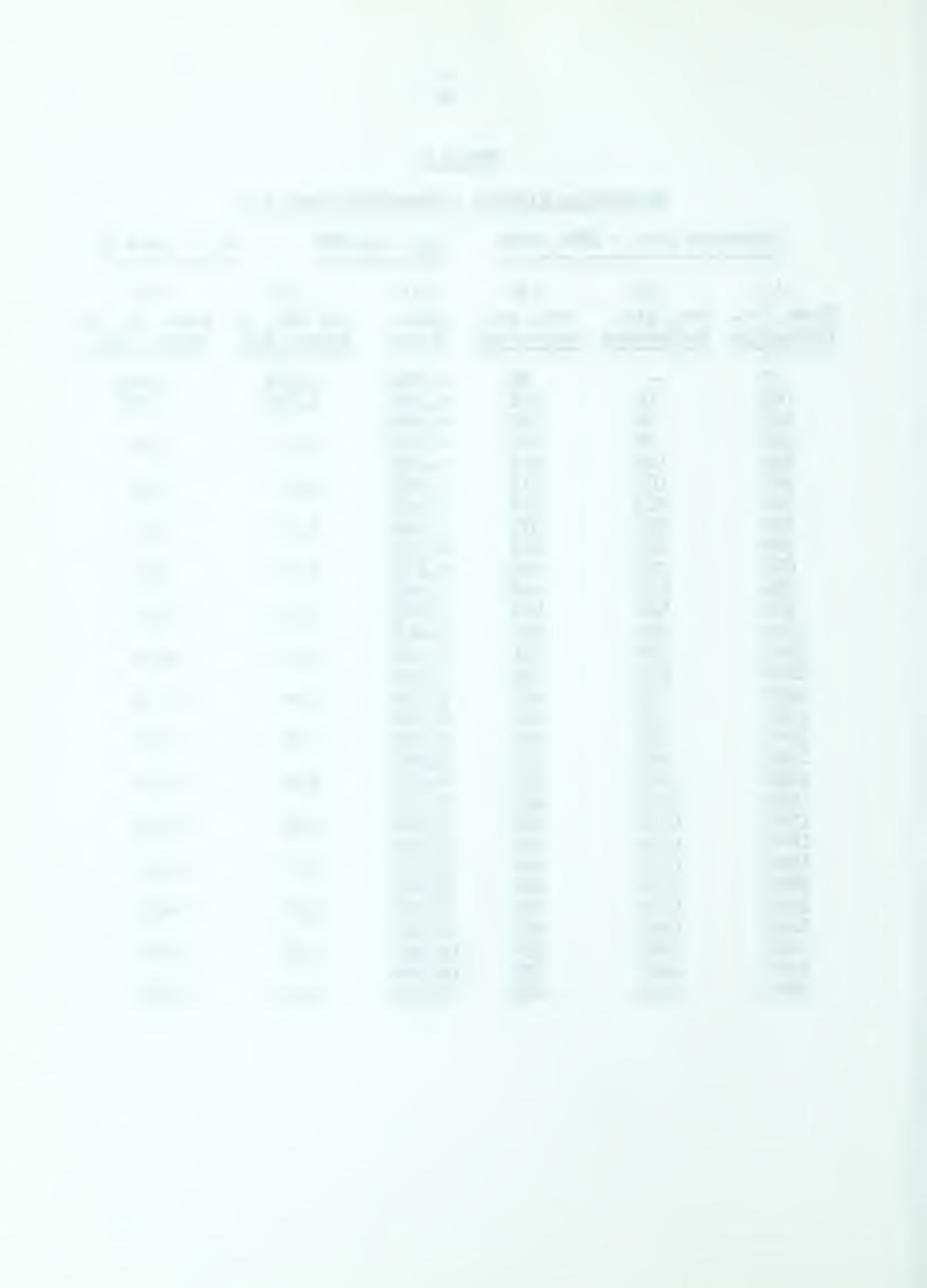


Table 8

Production History - Nine-Spot Flood I-d

Inject	ion Rate = 2	240 cc/hr	$S_{cw} = 18.82\%$		$\mu_{0} = 1.595 \text{ cp}$	
(1)	(2)	(3)	(4)	(5)	(6)	
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Inst. W.O.R.	Oil Rec. in Hydro. P.V.	Water Inj. in Hydro. P.V.	
80 160	0 30	80 130	0.000	0.921	0.921	
240 320 400	74 118 167	166 20 2	1.221 1.221 1.581	2.32	3.68	
480 560	210	233 270 297	1.162	3.11	5.52	
640 720	3 1 9 377	321 343	2.33 ⁴ 2.636	3.70	7.37	
800 880	436 494	364 386	2.810 2.636	4.19	9.21	
960 1040	554 617	406 423	3.000 3.700	4.68	11.05	
1120	683 747	437 453	4.714	5.03	12.80	
1280 1360	812 880	468 480	4.333 5.660	5.38	14.80	
1440 1520	946 1018	494 502	4.714 9.000	5.69	16.55	
1600 1680	1087 1155	513 525	6.272 5.660	5.91	18.95	
1760 1840	1 2 28 1301	532 539	10.400	6.13	20.30	
1920 2000	1373 1446	547 554	9.000	6.30	22.10	
2080 21,60	1519 1590	561 570	10.400	6.45	23.95	
2240 2320	1660 1742	574 578	19.000	6.61	25.80	
2400	1816	584	12.32	6.72	27.70	

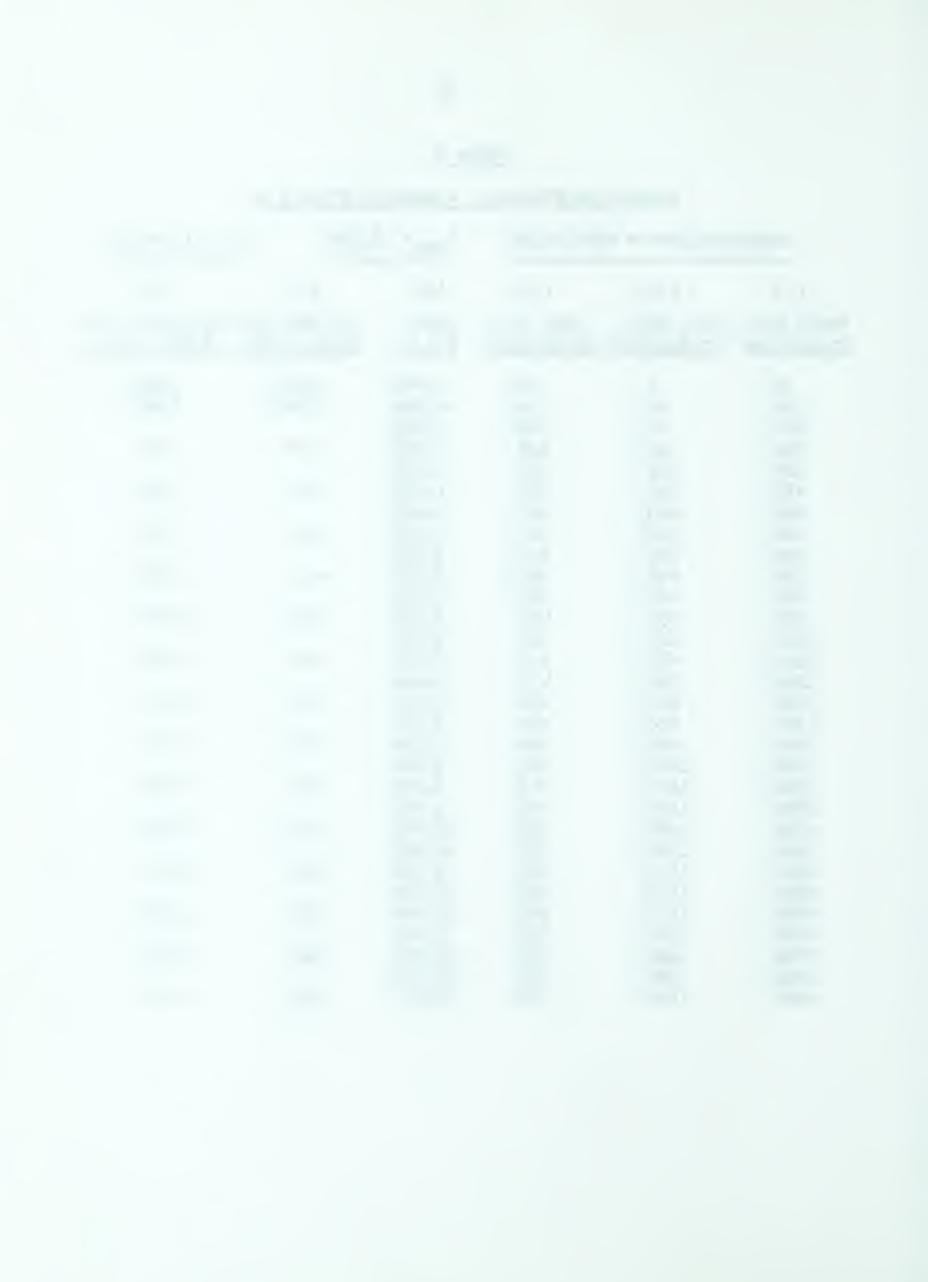


Table 9

Production History - Nine-Spot Flood 1-e

Injection 1	Rate = 2800	cc/hr S	= 20.25%	$\mu_{o} = 1.595 \text{ cp}$
(1)	(2)	(3)	(5)	(6)
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Oil Rec. in Hydro. P.V.	Water Inj. in Hydro. P.V.
80 160 320 400 480 640 800 880 1120 1200 1280 1440 1600 1680 1840 2000	34 123 190 239 355 478 535 726 790 857 997 1138 1208 1352 1498	80 126 197 210 241 285 322 345 394 410 423 443 462 472 488 502	0.939 1.480 2.318 2.83 3.34 3.78 4.63 4.96 5.20 5.42 5.74	0.939 1.880 3.75 5.63 7.52 9.39 13.15 15.00 16.90 18.80
2080 2240 2400	1572 1721 1872	508 519 528	5.97 6.09 6.20	24.45 26.30 28.20



Table 10

Production History - Nine-Spot Flood 2

Inject	ion Rate = 1	120 cc/hr	$S_{cw} = 23$	μ -5 % μ	$_{0} = 3.342 \text{ cp}$
(1)	(2)	(3)	(4)	(5)	(6)
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Inst. W.O.R.	Oil Rec. in Hydro. P.V.	Water Inj. in Hydro. P.V.
80 160 240	tr. 23	80 137	0.000	0.904 1.55	0.904 1.804
320 400	70 118 166	170 202 23 ¹ 4	0.510 1.500 1.500	2.28	3.61
480 560	210 264	270 296	1.220	3.04	5.41
640 720	322 378	318 342	2.64 2.33	3.59	7.23
800 880	437 491	363 389	2. 8 1 2.08	4.10	9.25
960 1040	547 609	413 431	2.33 3.45	4.67	10.80
1120 1200	666 73 ⁴	454 466	3.71 5.66	5.12	12.65
1280 1360	791 853	489 507	2.48 3.45	5, 52	14.45
1440 1520	917 983	523 537	4.00 4.71	5.90	16.25
1600 1680	1047	553 569	4.00	6.24	18.65
1760 1840	1175 .	585 598	4.00	6.60	19.85
1920 2000 2080	1310 1376 1443	610 624	5.66 4.71	6. 8 8	21.65
2160 2240	1510 1579	637 650 661	5.15 5.15 6.27	7.46	25.25
2320 2400	1655 1725	665 675	19.00	7.62	27.10
_,00		-17	1		

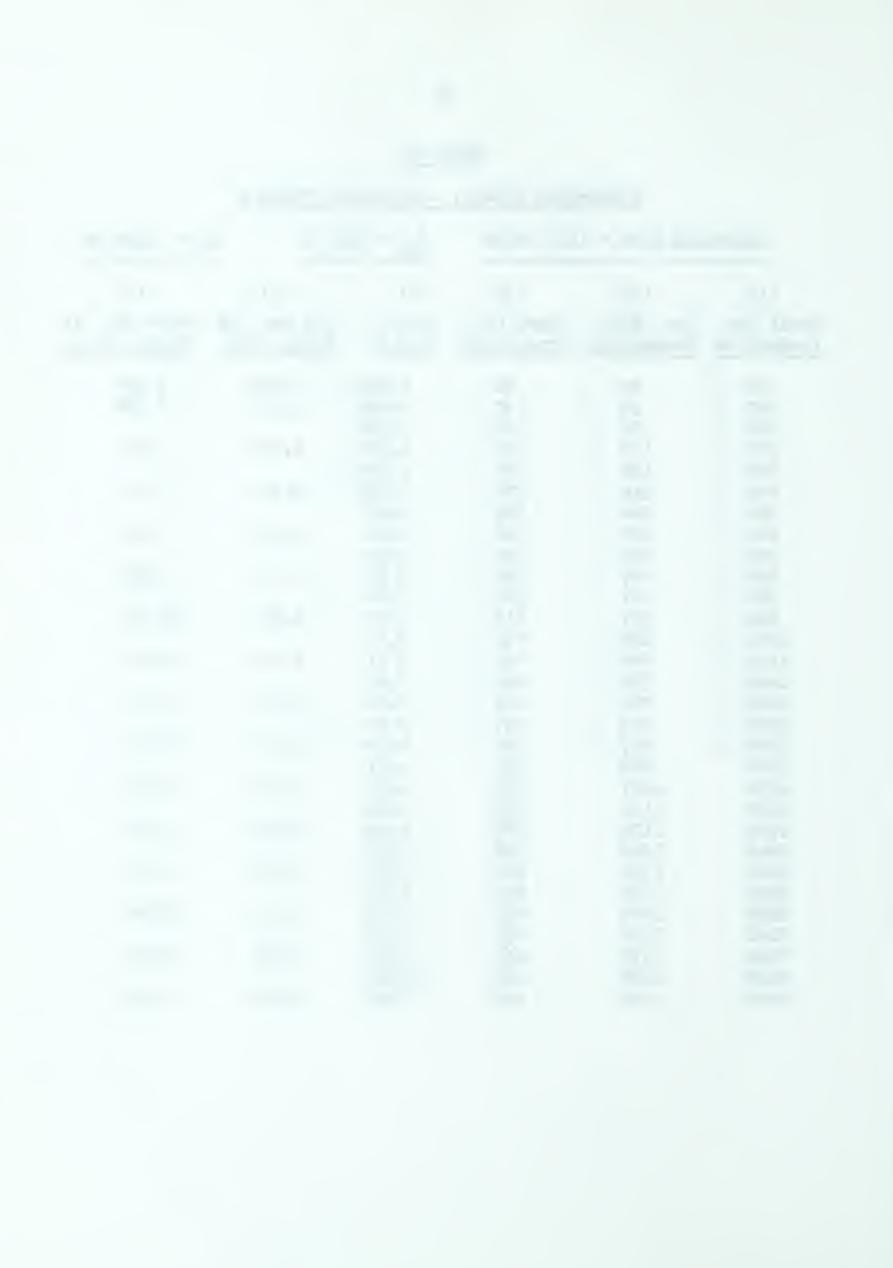
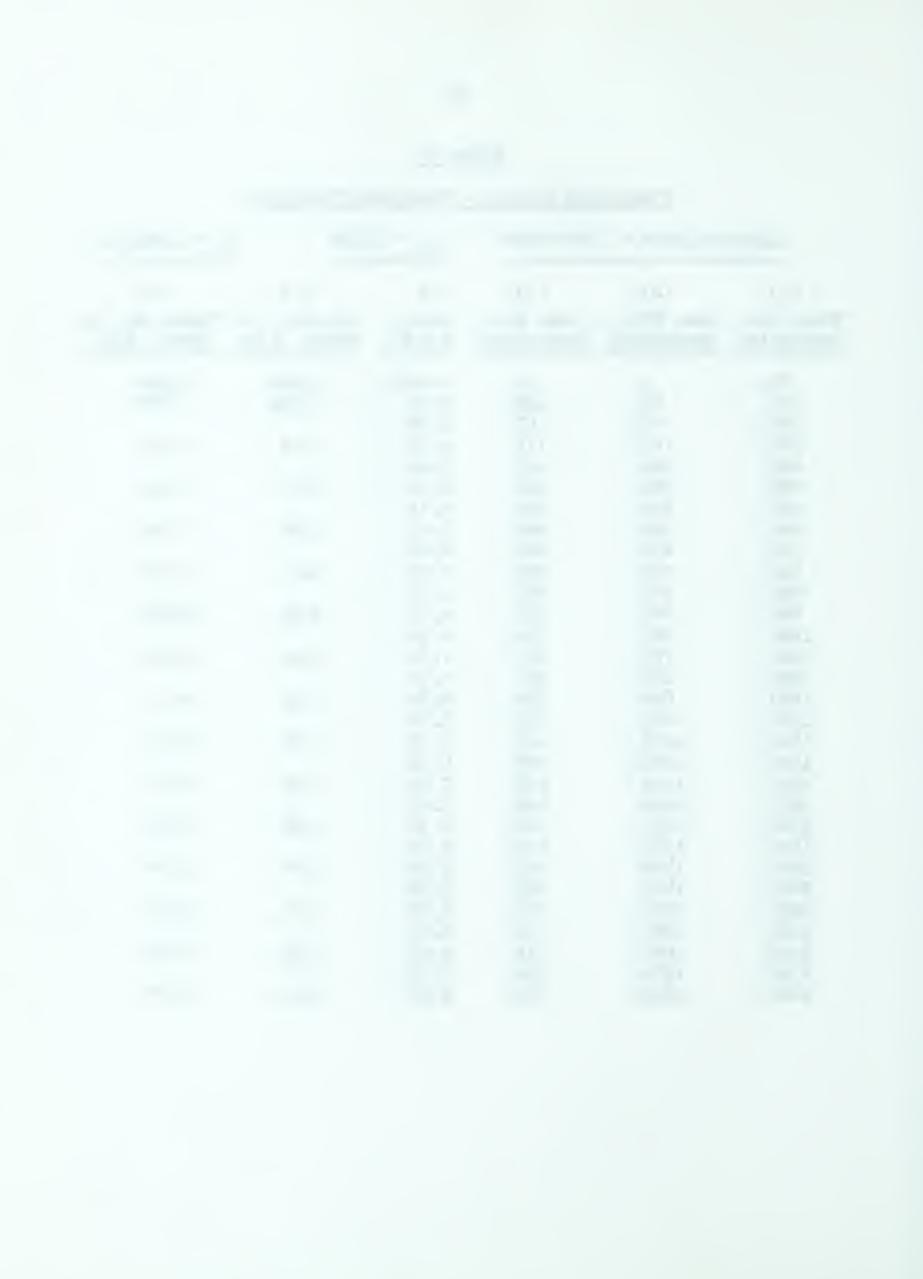


Table 11

Production History - Nine-Spot Flood 3-a

Inject	ion Rate = 1	120 cc/hr	$S_{cw} = 23$	3.5% μ	o = 5.592 cp
(1)	(2)	(3)	(4)	(5)	(6)
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Inst. W.O.R.	Oil Rec. in Hydro. P.V.	Water Inj. in Hydro. P.V.
80 160 240	1 40 93	79 120 147	0.0127 0.95 1.96	0.892 1.350	0.904 1.805
320 400	149 209	171	2.33	1.93	3.61
480 560	264 330	216 230	2.20 4.71	2.44	5.42
640 720	392 456	248 264	3.45	2.80	7.22
800 880	522	278	4.71 2.48	3.14	9.04
960 1040	579 643	301 317	4.00	3.58	10.80
1120	708 773	332 347	4.34	3.92	12.65
1200 1280	839 898	361 382	4.71 2.81	4.31	14.45
1360 1440	961 1030	399 410	3.70 6.25	4.63	16.25
1520 1600	1095 1163	425 436	4.34 7.90	4.92	18.05
1680 1760	1226 1291	454 469	3.45 4.34	5.30	19.85
1840 1920	1358 1429	482 491	5.15 7.90	5.54	21.70
2000	1497 1565	503 515	5.76 5.76	5.82	23.50
2160 2240	1629 1697	531 541	4.00	6.10	25.30
2320 2400	1770 1839	550 561	7.90 6.25	6.32	27.70



<u>Table 12</u>

<u>Production History - Nine-Spot Flood 3-b</u>

Inject	ion Rate = 5	60 cc/hr	$S_{ew} = 23$	β. 5% μ	o = 5.592cp
(1) Total Cum. Production	(2) Cum. Wtr. Production	(3) Cum. Oil Production	(4) Inst. W.O.R.	(5) Oil Rec. in Hydro. P.V.	(6) Water Inj. in Hydro. P.V.
80 160 240	1 32 73	79 128 167	0.0127 0.632 1.050	0.891 1.445	0.904 1.805
320 400	120 176	200 22 ¹ 4	1.425	2.26	3.61
480 560	222 276	258 284	1.35	2.91	5.42
640 720	330 389	310 331	2.08 2.81	3.50	7.22
800 880	445 499	355 381	2.34	4.00	9.04
960 1040	556 614	404 426	2.48 2.64	4.55	10.80
1120	675 736	445 464	3.21 3.21	5.01	12.65
1280 1360	795 859	485 501	2.81	5.47	14.40
1440 1520	925 986	515 53 ⁴	4.71 3.21	5.81	16.25
1600 1680	1052 1117	548 563	4.71 4.34	6.19	18.05
1760 1840	1182 1250	578 590	4.34 5.66	6.53	19.85
1920 2000	1320 1391	600 609	7.00	6.77	21.70
2080 2160	1460 1529	620 631	6.26 6.26	7.00	23.50
2240 2320	1601 1671	639 649	9.00	7.21	25.30
2400	1744	656	10.40	7.41	27.10

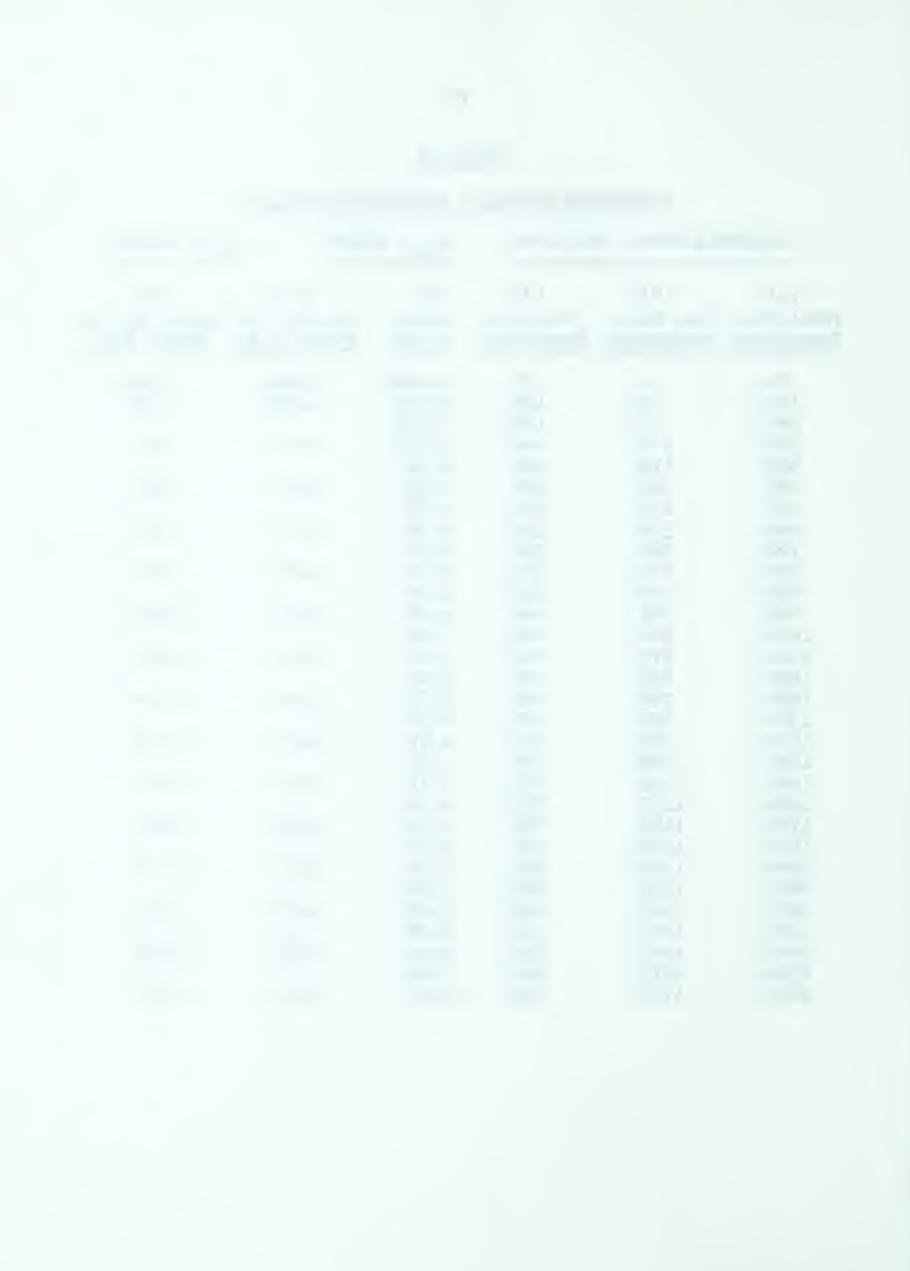


Table 13

Production History - Nine-Spot Flood 3-c

Inject	ion Rate = 3	20 cc/hr	$S_{cw} = 23$	3 · 5% µ	$_{0} = 5.592 \text{ cp}$
(1) Total Cum. Production	(2) Cum. Wtr. Production	(3) Cum. Oil Production	(4) Inst. W.O.R.	(5) Oil Rec. in Hydro. P.V.	(6) Water Inj. in Hydro. P.V.
80 160 240 320 400 480 560 640 720 800 880 960 1040 1120 1200 1280 1360 1490 1520 1600 1680 1760 1840	tr. 21 59 100 144 183 230 275 325 375 423 475 529 587 646 705 765 827 894 964 1031 1100 1170	80 139 181 220 256 297 330 365 395 425 457 485 511 533 554 575 595 613 626 649 660 670	0.000 0.356 0.904 1.050 1.22 0.95 1.42 1.285 1.665 1.665 1.50 1.86 2.08 2.64 2.81 2.81 3.00 3.44 5.15 7.00 5.15 6.27 7.00	0.904 1.56 2.04 2.48 2.99 3.35 3.72 4.12 4.46 4.80 5.47 6.02 6.50 6.92 7.19 7.45	0.904 1.805 2.71 3.61 4.52 5.42 6.32 7.22 8.12 9.04 10.82 12.65 14.45 16.28 18.05 19.85
1920 2000	1242 1314	678 686	9.00 9.00	7.66 7.75	21.70 22.60

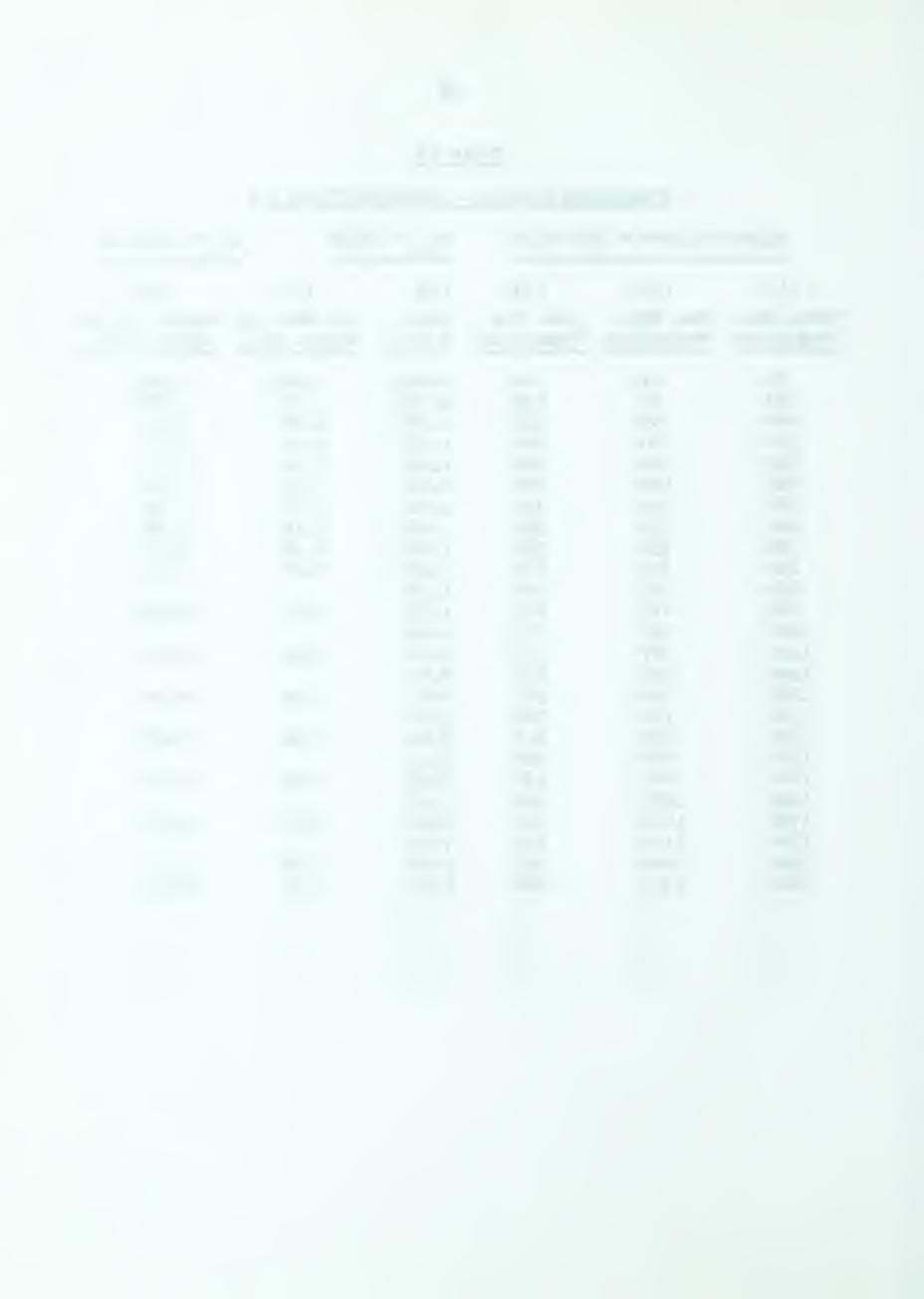


Table 14

Production History - Nine-Spot Flood 3-d

Inject	ion Rate = 1	680 cc/hr	$S_{cw} = 23$	β. 5% μ	o = 5.592 cp
(1)	(2)	(3)	(4)	(5)	(6)
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Inst. W.O.R.	Oil Rec. in Hydro. P.V.	Water Inj. in Hydro. P.V.
80 160 240	2 45	78 115	0.0256 1.16	0.87 1.30	0.904 1.805
320 400	101 165 228	139 155	2.33 4.00	1.75	3.61
480 560	288 356	172 192 204	3.71 3.00 5.66	2.165	5.42
640 720	424 492	216 228	5.66 5.66	2.44	7.22
800 880	566 630	234 250	12.35	2.64	9.04
960 1040	696 763	264 277	4.71 10.42	2.98	10.80
1120 1200	831 905	289 295	5.66 12.35	3.26	12.65
1280 1360	970 1037	310 323	4.34 5.15	3.50	14.40
1440 1520	1105	335 344	5.66 7.90	3.78	16.25
1600 1680	1246 1314	35½ 366	7.00 5.66	3.99	18.05
1760 1840	1379 1448	381 392	4.34 6.26	4.30	19.85
1920 2000	1523 1592	397 408	15.00 6.26	4.47	21.70
2080 21:60	1659 1726	421 434	5.15 5.15	4.75	23.50
2240 2320	1 7 98 1869	442 451	9.00 7.90	4.95	25.30
2400	1941	459	9.00	5.17	27.10

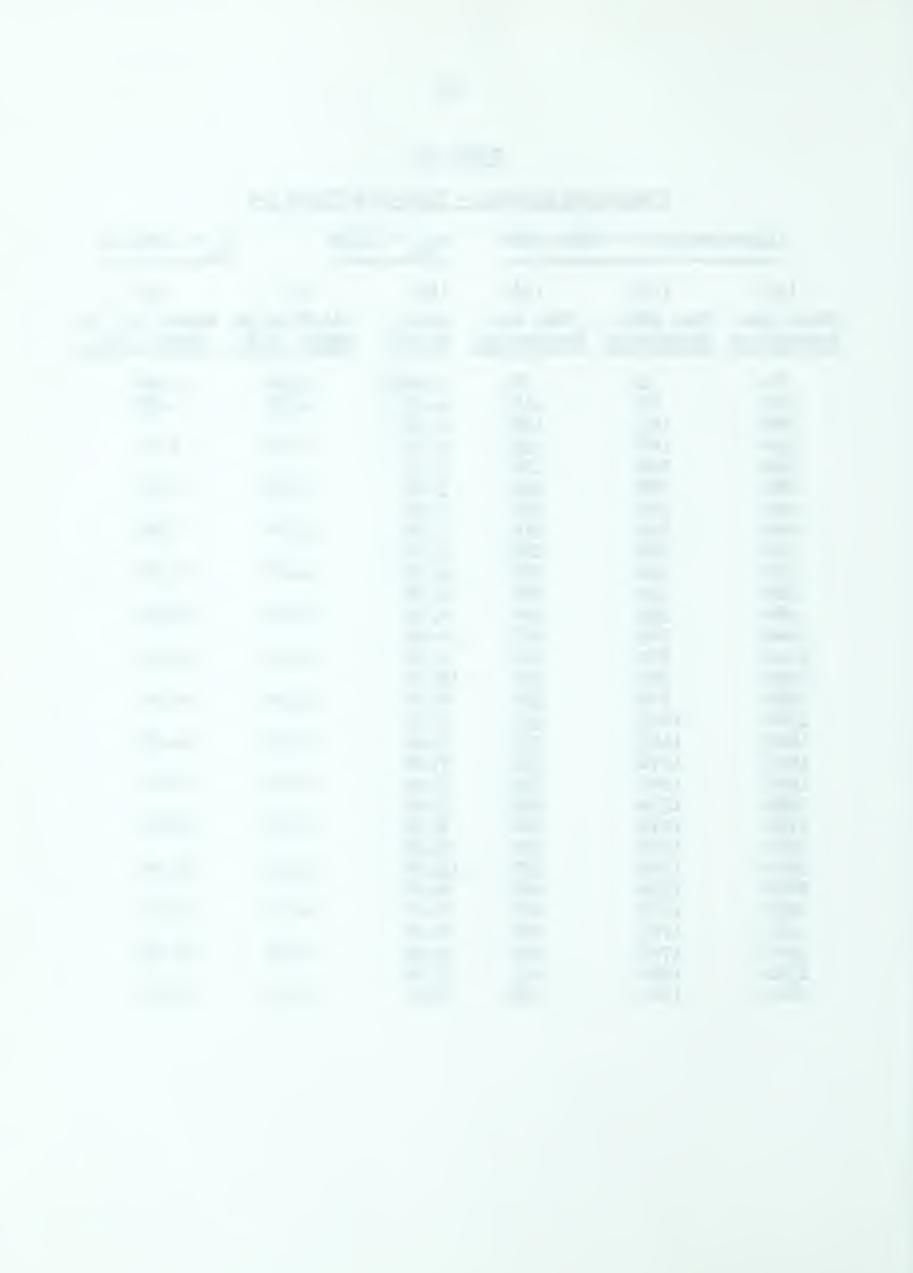


Table 15

Production History - Nine-Spot Flood 3-e

Injection Rate = 2240 cc/hr		$S_{ew} = 23.5\%$		o = 5.592 cp	
(1) Total Cum. Production	(2) Cum. Wtr. Production	(3) Cum. Oil Production	(4) Inst. W.O.R.	(5) Oil Rec. in Hydro. P.V.	(6) Water Inj. in Hydro. P.V.
80 160 240	4 49 106	76 111 134	0.0525 1.29 2.48	0.857 1.25	0.904
320 400	166 237	154 163	3.00 7.90	1.74	3.61
480 560	293 357	187 203	4.00	2.11	5.42
640 720	424 493	216 227	5.15 6.26	2.44	7.22
800 880	562 627	238 253	6.26 4.34	2.69	9.04
960 1040	692 758	268 282	4.34 4.71	3.02	10.80
1120	828 901	292 299	7.00 10.42	3.30	12.65
1280 1360	968 1036	312 324	5.15 5.66	3.52	14.40
1440 1520	1106 1175	334 345	7.00 6.26	3.77	16.25
1600 1680	1249 1317	351 363	12.35 5.66	3.96	18.05
1760 1840	1387 1455	372 385	7.00 5.66	4.20	19.85
1920 2000	1530 1601	390 399	15.00 7.9	4.40 4.50	21.70 22.60

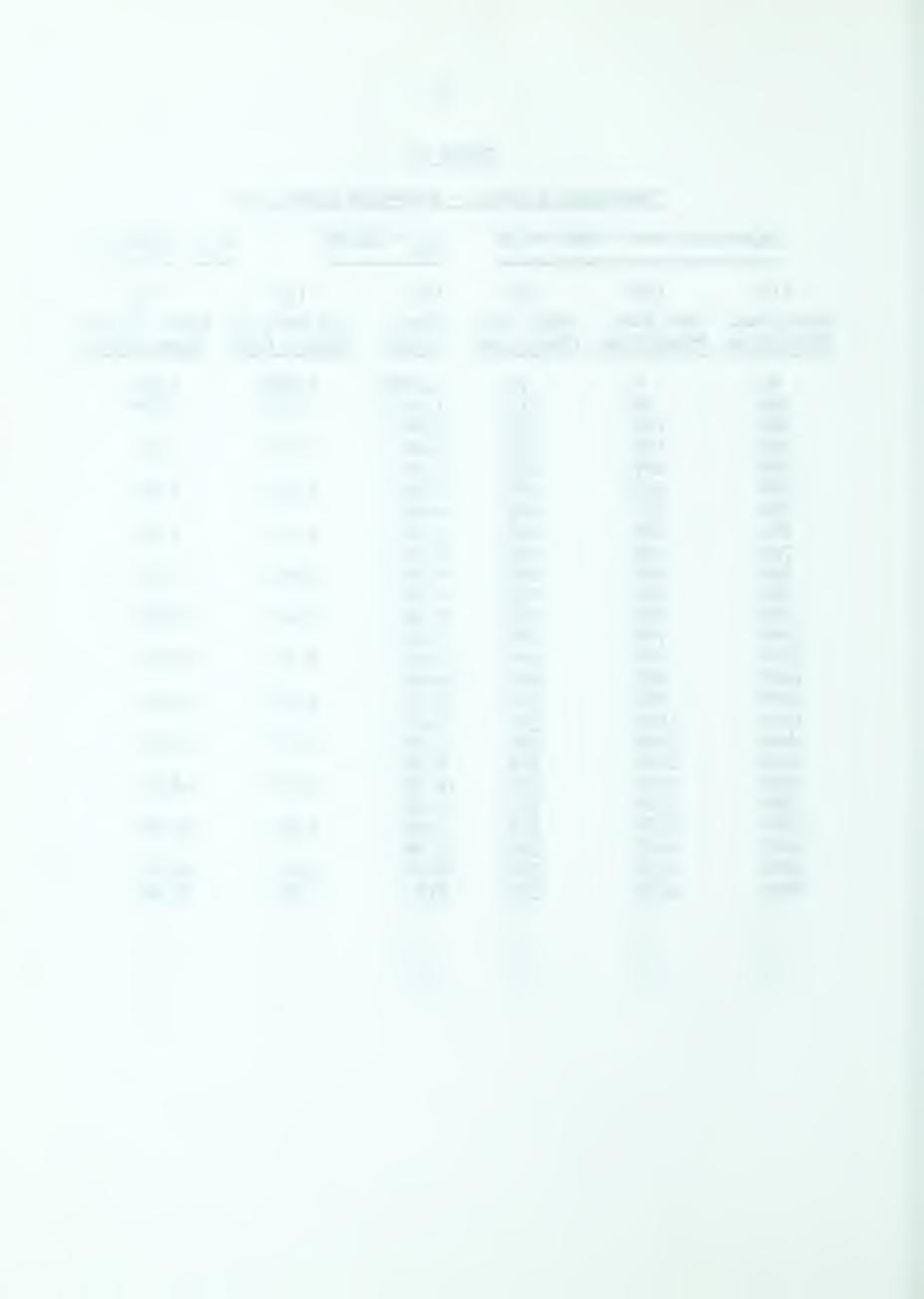


Table 16

Production History - Nine-Spot Flood 3-f

Injection Rate = 1400 cc/hr		$S_{cw} = 23.5\%$ $\mu_{o} = 5.592$		o = 5.592 cp		
(1) Total Cum. Production	(2) Cum. Wtr. Production	(3) Cum. Oil Production	(4) Inst. W.O.R.	(5) Oil Rec. in Hydro. P.V.	(6) Water Inj. in Hydro. P.V.	
80 160 240	2 40 90	78 120 144	0.0256 0.905 2.34	0.88 1.355	0.904 1.805	
320 400	156 217	1 <i>6</i> 4 183	3.00 3.21	1.85	3.61	
4 8 0 560	276 336	204 224 238	204 2.81 224 3.00 238 4.71 252 4.71 264 5.66	2.81	2.30	5.42
640 720	402 468			2.68	7.22	
800 880	536 598			2.87	9.04	
960 1040	662 731	298 309	4.00 6.26	3.37	10.80	
1120 1200	798 866	322 334	5.15 5.66	3.64	12.65	
1280 1360	9 32 998	348 362	4.71 4.71	3.93	14.40	
1440 1520	1069 1137	371 383	7.40 5.66	4.19	16.25	
1600 1680	1207 1275	393 405	7.00 5.66	4.43	18.05	
1760 1840	1342 1412	418 428	5.15 7.00	4.72	19.85	
1920 2000 2080	1482 1556 1625	438 444 455	7.00 12.35 6.26	4.95 5.14	21.70	
2160 2240	1696 1769	464 471	7.90 10.42	5.32	25.30	
2320 2400	1829 1911	481 489	7.00	5.52	27.10	

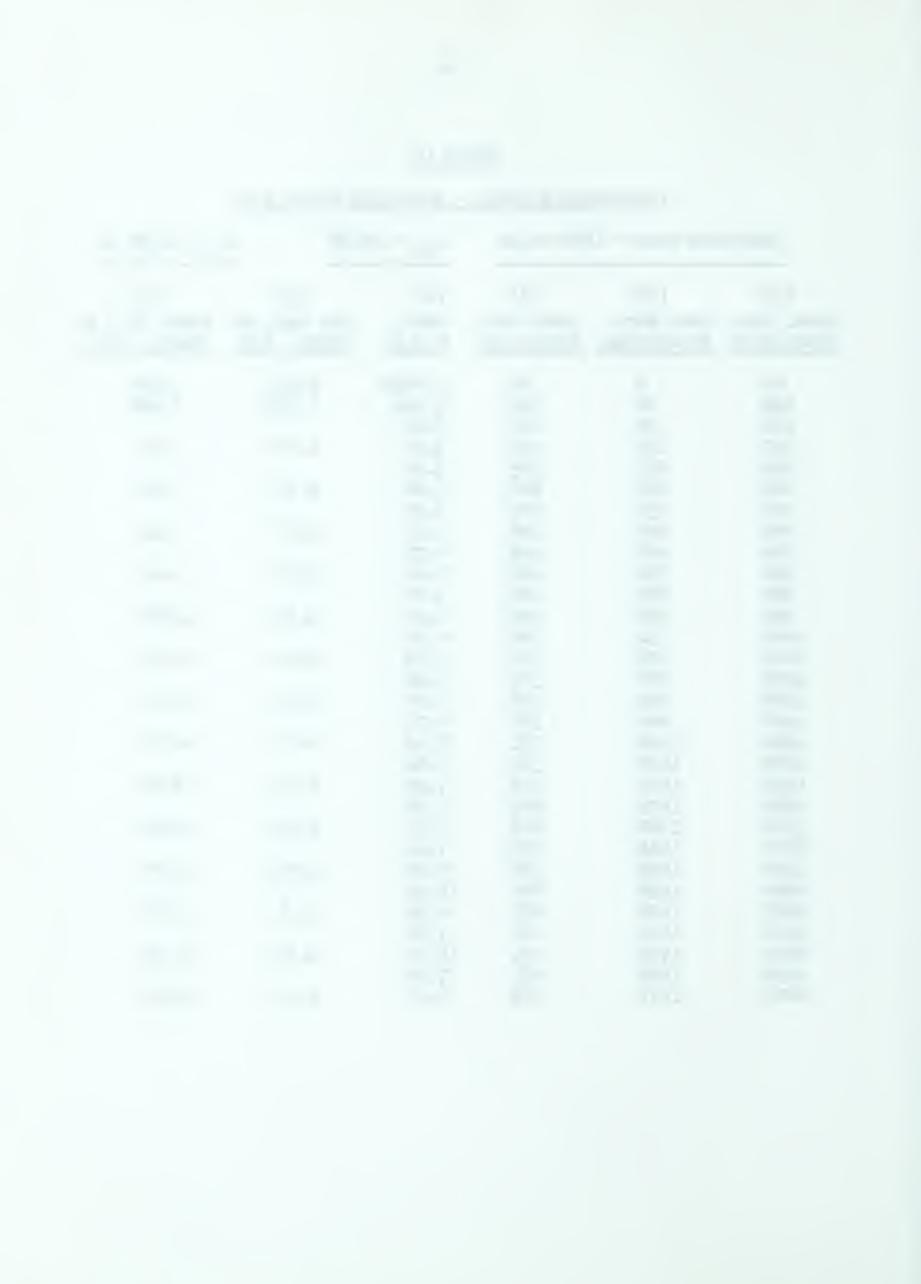


Table 17

Production History - Nine-Spot Flood 4

Injection Rate = 1680 cc/hr			$S_{cw} = 23.5\%$ μ_c		o = 7.607 cp
(1) Total Cum. Production	(2) Cum. Wtr. Production	(3) Cum. Oil Production	(4) Inst. W.O.R.	(5) Oil Rec. in Hydro P.V.	(6) Water Inj. in Hydro. P.V.
80 160 240 320	4 55 116 190	76 105 124 130	0.0526 1.760 3.21 12.32	0.858 1.185	0.904 1.805
400 480 560 640 720 800 880	260 328 403 474 548 625 698	140 152 157 166 172 175 182	7.00 5.66 15.00 7.89 12.32 25.60 10.45	1.715	5.42
				1.875	7.22 9.04
960 1040 1120 1200	774 848 923 999	186 192 197 201	19.00 12.32 15.00 19.00	2.10 2.24	10.80
1280 1360 1440	1075 1151 1225	205 209 215 216	19.00 19.00 12.32	2.31	14.40 16.25
1520 1600 1680 1760	1304 1379 1455 1531	221 225 2 29	79.00 15.00 19.00 19.00	2.492.58	18.05 19.85
1840 1920 2000 2080	1606 1682 1761 1837	234 238 239 243	15.00 19.00 79.00 19.00	2.68 2.74	21.70
2160 2240 2320	1914 1989 2066	246 251 254	25.60 15.00 25.60	2.83	25.30
2400	2143	257	25.60	2.97	27.10

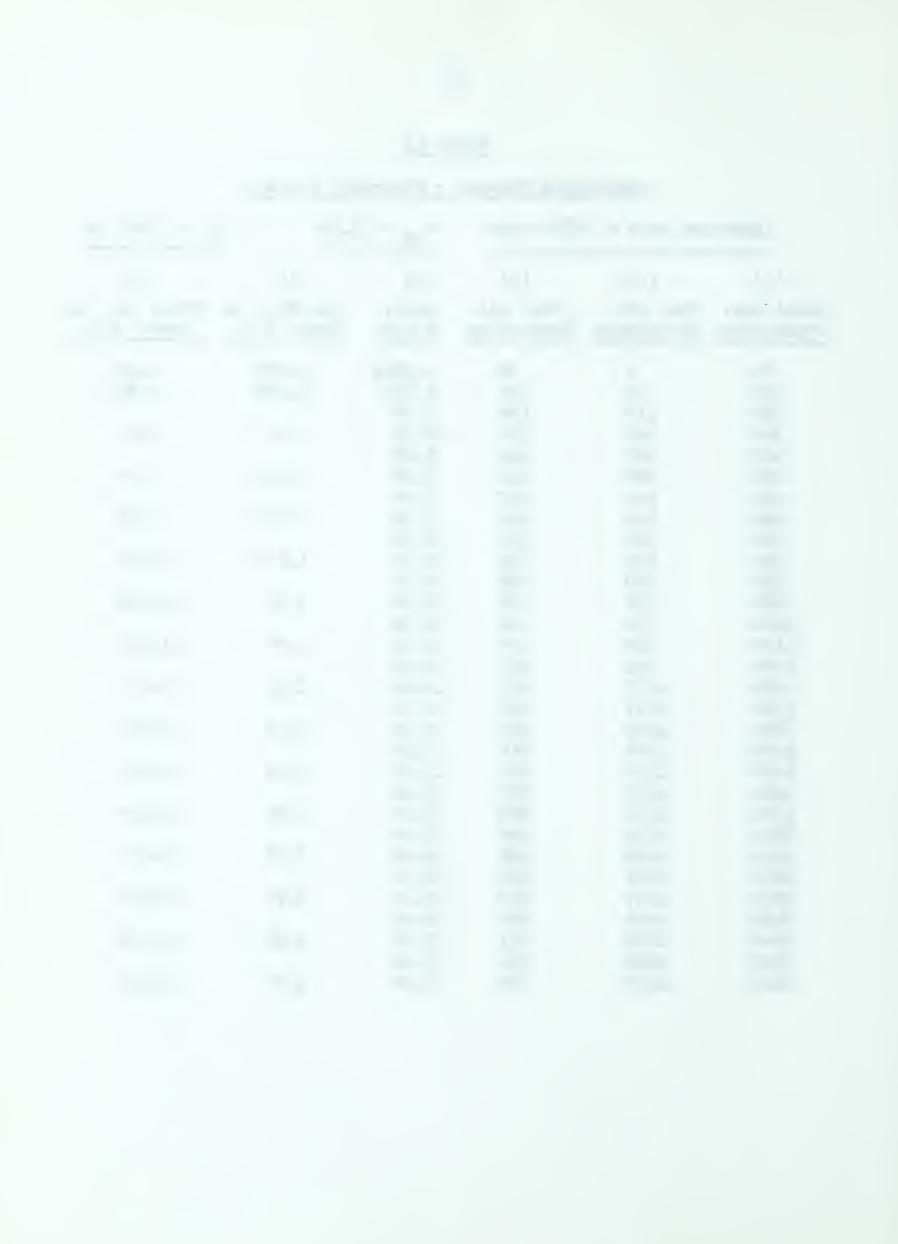


Table 18

Production History - Nine-Spot Flood 5

Injection Rate = 1680 cc/hr			$S_{cw} = 20$	D.5% µ	o = 11.786 cp
(1)	(2)	(3)	(14)	(5)	(6)
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Inst. W.O.R.	Oil Rec. in Hydro. P.V.	Water Inj. in Hydro. P.V.
80 160 240	8 64 130	72 96 110	0.110 2.33 4.71	0.846 1.13	0.942 1.880
320 400	197 274	123 126	5.15 25.65	1.45	3.77
480 560	3 ⁴ 5 419	135 141	7.89 12.32	1.59	. 5.65
640 7 20	495 571	145 149	19.00	1.66	7.52
800 880	00 647 153 19.00 80 722 158 15.00 60 796 164 12.30 40 871 169 15.00 20 951 169 00 1024 176 10.40 80 1100 180 19.00	00 647 153 19.00	1.755	9.42	
960 1040		796 164	12.30	1.930	11.30
1120		1120 951 169 1200 1024 176 1 1280 1100 180 1		1.990	13.20
					2.12
1440 1520	1252 1329	188	25.65 25.65	2.21	16.95
1600 1680	1405 1480	195 200	19.00 15.00	2.29	18.80
1760 1840	1555 1633	205 207	15.00 39.00	2.41	20.70
1920 2000	1710 1788	210 212	25.65 39.00	2.47	22.60
2080 2080 2160	1866 1944	214 216	39.00 39.00	2.52	24.40
2240	2020 2098	220 222	19.00	2.59	26.40
2320 2400	2176	224	39.00	2.64	28.20



Table 19

Production History - Nine-Spot Flood 6

Injection Rate = 1680 cc/hr		$S_{cw} = 23$	3.8%	$\mu_0 = 1.595 \text{ cp}^*$			
(1)	(2)	(3)	(4)	(5)	(6)		
Total Cum. Production	Cum. Wtr. Production	Cum. Oil Production	Inst. W.O.R.	Oil Rec. in Hydro. P.V.	Water Inj. in Hydro. P.V.		
80 160	0 24	80 136	0.000	0.9825 1.67	0.9825 1.963		
240 320	66 114	174 206	1.105	2.53	3.93		
400 480 560	168 219 273	232 261 287	2.08 1.76 2.08	3.20	5.89		
640	328 400	312	2.20 9.00	3.83	7.85		
720 800 880	464 336	355 371 386 399	464 336 525 355 589 371 654 386	4.00	4.125	9.825	
960 1040	589			371	4.00 4.33	4.55	11.80
1120 1200	721			5.15 7.00	4.88	13.75	
1280 1280 1360	857 924	423 436	4.72 5.15	5.20	15.75		
1440 1520	994 1065	446 456	7.00	5.47	17.65		
1600 1680	1137	463 472	10.40	5.68	19.65		
1760 1840	1280	480 485	9.00	5.89	21.60		
1920	1355 1428	492 497	10.40	6.03	23.60		
2000	1503 1577	503	15.00 12.32	6.18	25.60		
2160 2240	1651 1725	509 515 518	12.32 12.32 25.65	6.31	27.50		
2320 2400	1802 1876	524	12.32	6.43	29.50		

^{*} $\mu_{\rm W} = 3.185 \, \rm cp$

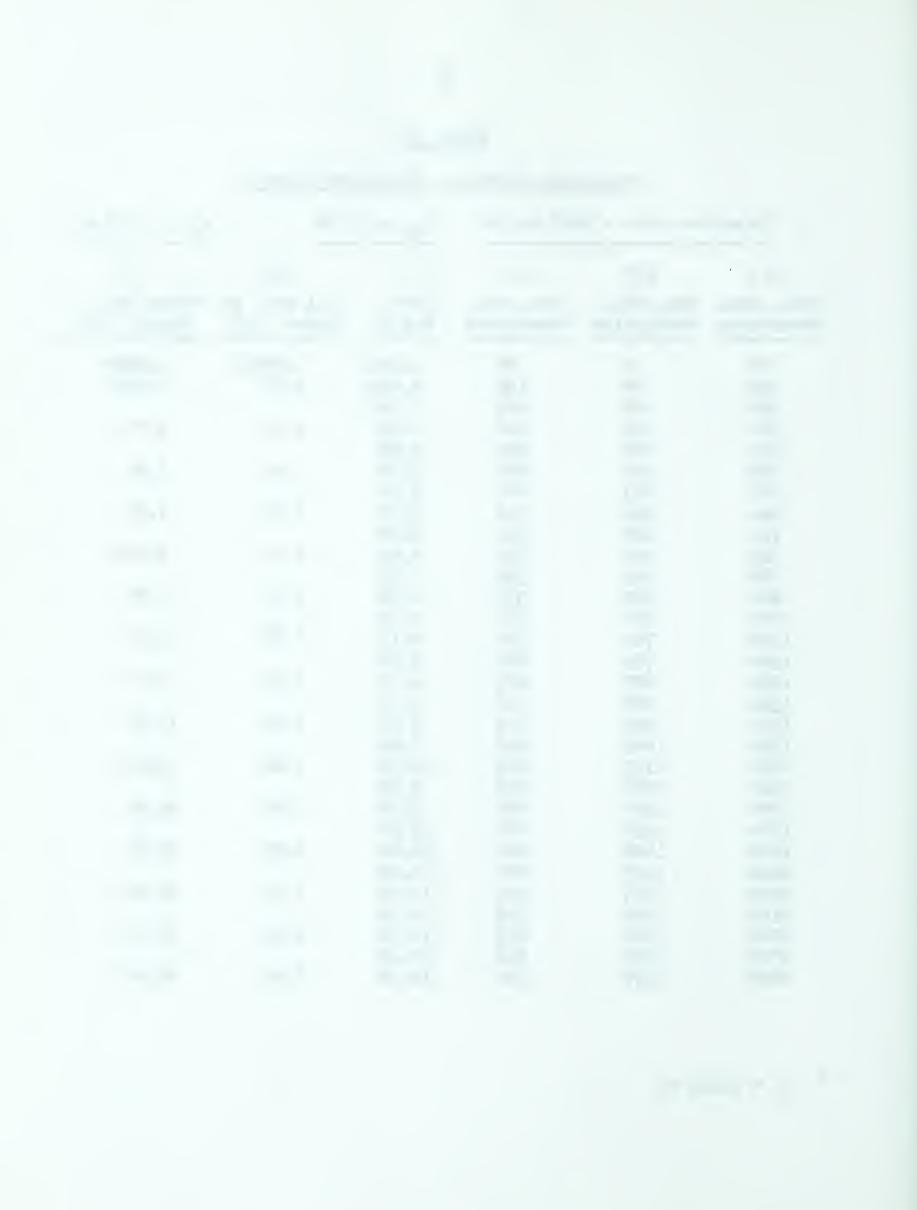
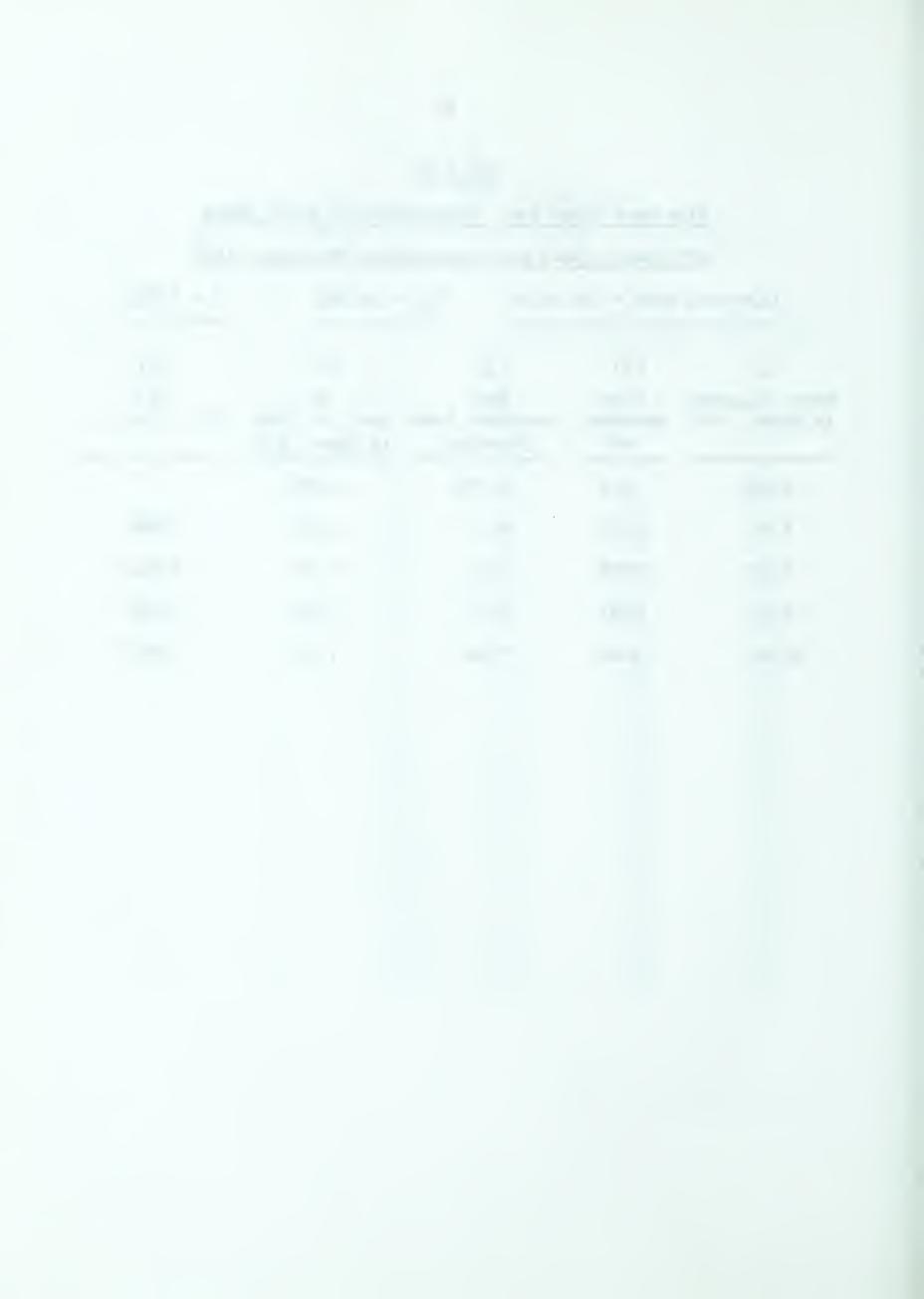


Table 20

Nine-Spot Flood 1-a: Calculation of Areal Sweep

Efficiency (Eas) and Displacement Efficiency (Ed)

Injection	Rate = 560	cc/hr S _{cw}	= 19.69%	C = 1.679
(1)	(2)	(3)	(4)	(5)
Water Injected in Hydro. P.V.	Area Measured cm ²	Eas. Area/Unit Area Fraction	Es Cum. Oil Prod. in Hydro. P.V.	Ed Col. 4/Col. 3
0.932	315	0.763	0.932	
4.66	2110	5.10	3.37	0.660
9.32	2698	6.53	5.37	0.821
14.00	2880	6.97	6.24	0.891
28.00	3000	7.26	7.05	0.970



<u>Table 21</u>

<u>Nine-Spot Flood 1-b: Calculation of Areal Sweep</u>

<u>Efficiency (Eas) and Displacement Efficiency (Ed)</u>

Injection Rate = 1120 cc/hr S _{cw} = 17.25% C = 1.679								
(1) Water In in Hydro	jected	(2) Area Measured cm ²	(3) Eas Area/Unit Ar Fraction	Es ea Cum. Oil Prod. in Hydro. P.V.	(5) Ed Col. 4/Col. 3			
0.90	25	296.5	0.718	0.9025				
4.01	3	1820	4.41	3.13	0.710			
9.02	25	2485	6.02	4.89	0.815			
13.55		2680	6.49	5.94	0.918			
18.09		2830	6.85	6.57	0.962			
27.10		2960	7.16	7.21	1.000			

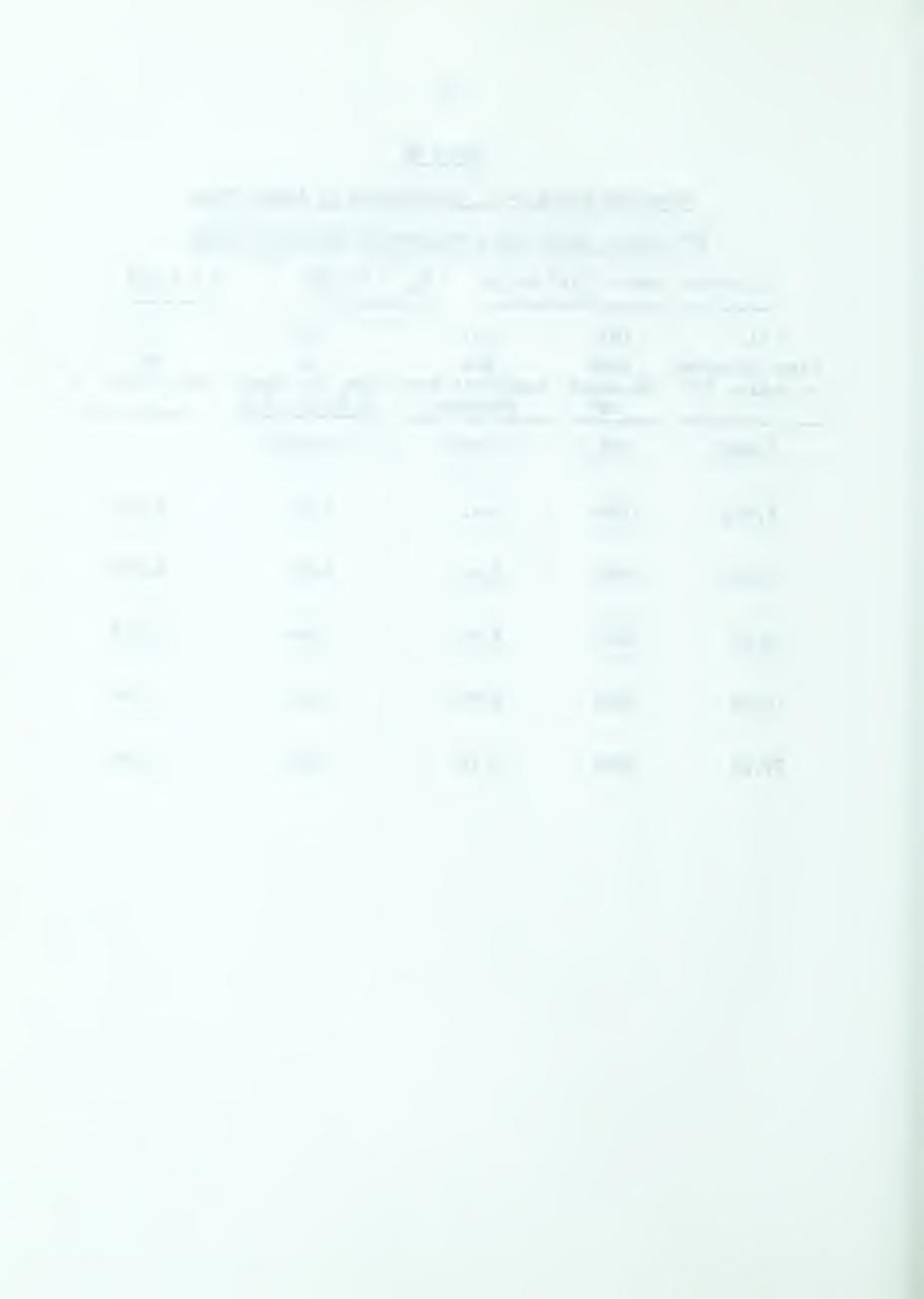


Table 22

Nine-Spot Flood 1-c: Calculation of Areal Sweep Efficiency (Eas),

Displacement Efficiency (Ed) and Mobility Ratio (M).

c = 1.679	(6)	$M = \frac{K_{TW}^{\mu}}{K_{ro}^{\mu}}$	1.732	1.225	1.225	1.225	1.330	1.679	1.975	2.585
[(8)	K rw	0.495	0.350	0.350	0.350	0.380	0.480	0.565	0.740
	(7)	Kro	0.48	0.48	0.48	0.48	0.48	0.48	0.48	0.48
	(9)	™ *	0.886	0.768	191.0	0.765	0.795	0.873	0.917	196.0
$S_{CW} = 15.07\%$	(5)	Ed Col. 4/Col. 3	0.865	0.726	0.725	0.722	0.756	0.850	0.901	0.956
	(4)	Area Eas Measured Area/Unit Area Cum. Oil Prod. cm² Fraction in Hydro. P.V.	0.879	1.605	2.15	3.04	19.4	5.83	6.59	7.56
Injection Rate = 1680 cc/hr	(3)	Eas Area/Unit Area Fraction	1.018	2.07	2.98	4.22	6.17	98.99	7.34	7.84
ion Rate =	(2)	Area Measured cm ²	420	855	1229	1745	2550	2839	3030	3240
Inject	(1)	Water Inj. HydroP.V.	0.879	1.760	5.64	04.4	8.80	13.20	17.60	26.40

 $* \overline{S}_W = S_{CW} + (1 - S_{CW}) Ed$



<u>Table 23</u>

<u>Nine-Spot Flood 1-d: Calculation of Areal Sweep</u>

<u>Efficiency (Eas) and Displacement Efficiency (Ed)</u>

Injection	C = 1.679			
(1)	(2)	(3)	(4)	(5)
Water Injected in Hydro. P.V.	Area Measured cm ²	Eas Area/Unit Area Fraction	Es Cum. Oil Prod. in Hydro. P.V.	Ed Col. 4/Col. 3
0.921	351.5	0.85	0.921	
1.845	612	1.48	1.50	
2.77	1020	2.47	1.91	0.776
4.61	1585	3.84	2.68	0.700
9.21	2240	5.43	4.19	0.775
13.84	2575	6.24	5.22	0.839
18.45	2752	6.67	5.91	0.887
27.70	2939	7.11	6.72	0.945



Table 24

Nine-Spot Flood 2: Calculation of Areal Sweep Efficiency (Eas),

Displacement Efficiency (Ed) and Mobility Ratio (M).

3.520	(6)	$M = \frac{K_{TW}^{\mu\nu}}{K_{ro}^{\mu\nu}}$	49.4	3.655	3.18	2.98	3.11	3.52	4.16	5.42
c = 3.520	(8)	Krw	0.515	0.405	0.340	0.330	0.345	0.390	0.462	009.0
	(4)	K_{TO}	0.39	0.39	0.39	0.39	0.39	0.39	0.39	0.39
	(9)	\Q_*	0.895	0.819	0.759	0.748	0.762	0.803	0.864	0.929
$S_{cw} = 23.5\%$	(5)	Ed Col. 4/Col. 3	0,860	0.764	0.685	0.671	0.689	747	0.822	706.0
	(4)	Es Cum. Oil Prod. in Hydro. P.V.	0.925	1.55	1.92	2.64	4.10	5.25	· 6.24	7.62
Injection Rate = 1120 cc/hr	(3)	Area Eas Measured Area/Unit Area cm ² Fraction	1.05	2.03	2.81	3.95	5.97	7.10	7.62	8,40
ion Rate =	(2)	Area Measured cm ²	435	839	1160	1630	2465	2930	3145	3475
Injecti	(1)	Water Inj. Hydro. P.V.	406.0	1.804	2.71	4.52	9.25	13.55	18.65	27.10

$$\tilde{S}_{W} = S_{CW} + (1-S_{CW})Ed$$

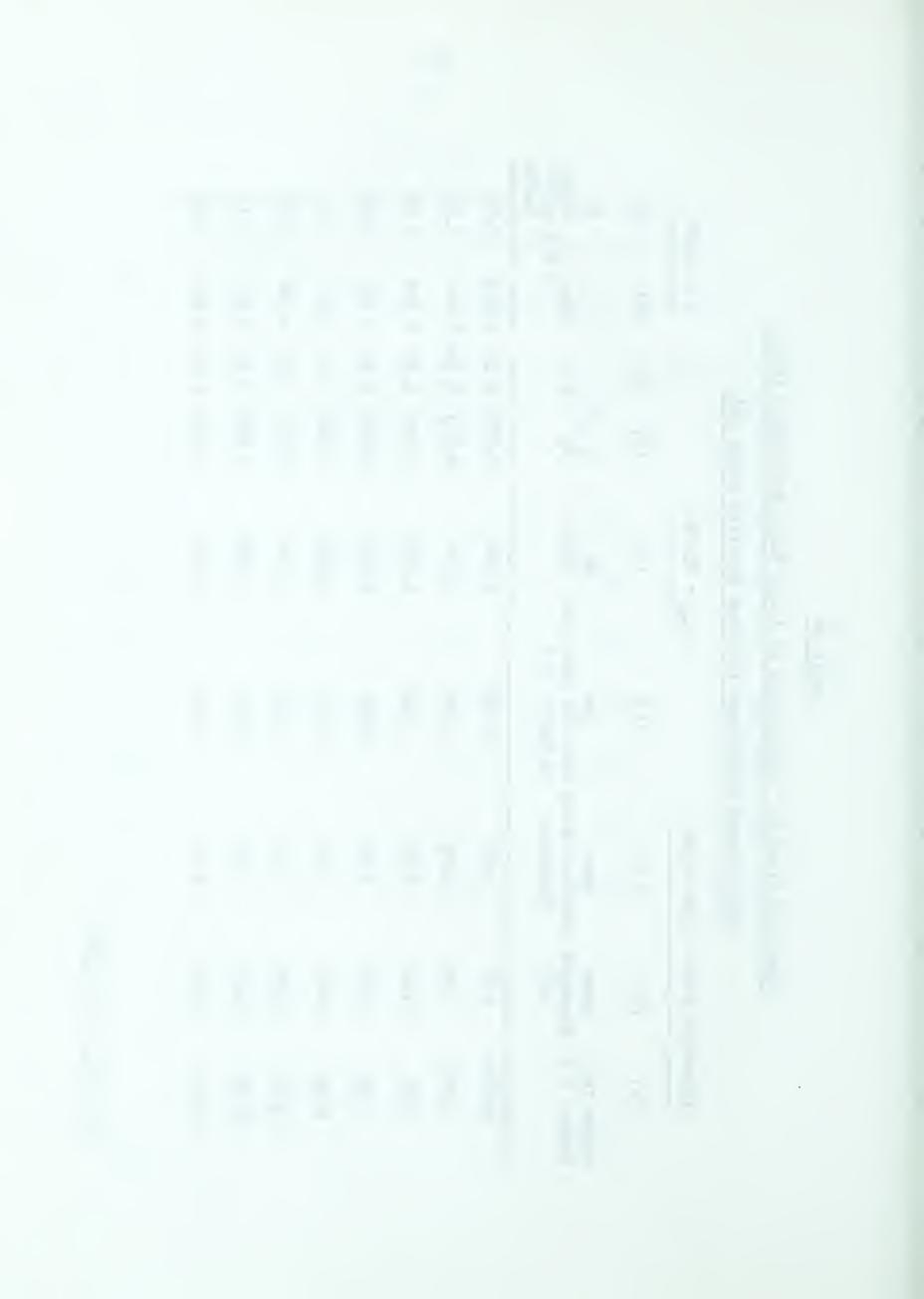


Table 25

Nine-Spot Flood 3-a: Calculation of Areal Sweep

Efficiency (Eas) and Displacement Efficiency (Ed)

Injection Rate = 1120 cc/hr $S_{cw} = 23.5\%$ $C = 6.265$								
(1)	(2)	(3)	(4)	(5)				
Water Injected in Hydro. P.V.	Area Measured cm ²	Eas Area/Unit Area Fraction	Es Cum. Oil Prod. in Hydro. P.V.	Ed Col. 4/Col. 3				
0.904	<u>ነ</u> ተ ያተ ያተ	1.075	0.892	0.832				
1.805	678	1.64	1.350	0.829				
2.71	895	2.165	1.66	0.768				
4.52	1198	2.90	2.15	0.745				
9.04	1870	4.53	3.14	0.695				
13.55	2500	6.05	4.07	0.675				
22.60	3160	7.65	5.68	0.745				

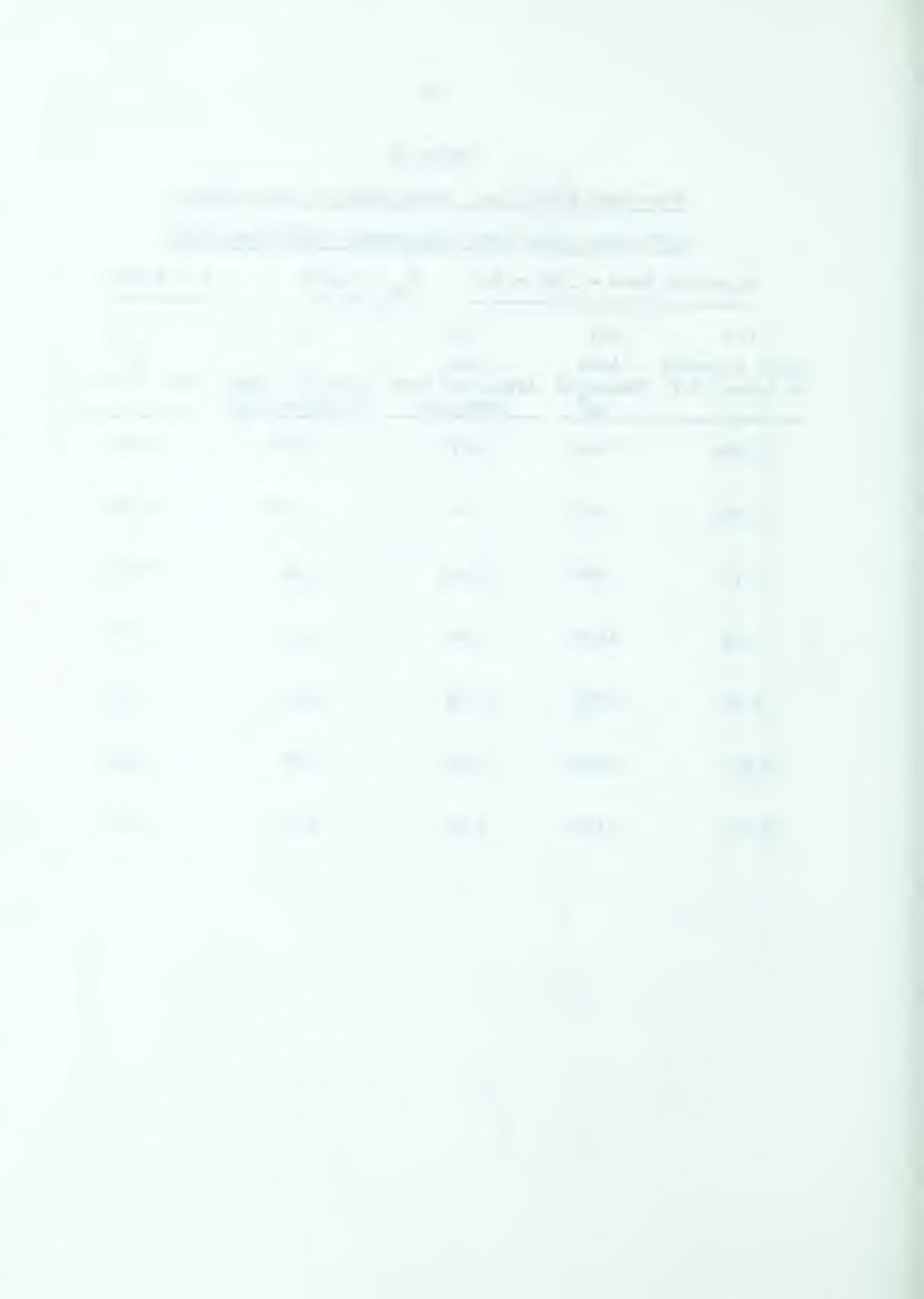


Table 26

Nine-Spot Flood 3-b: Calculation of Areal Sweep

Efficiency (Eas) and Displacement Efficiency (Ed)

Injection	Rate = 560	cc/hr S _{cw}	= 23.5%	C = 6.265
(1)	(2)	(3)	(4)	(5)
Water Injected in Hydro. P.V.	Area Mea s ured cm ²	Eas Area/Unit Area Fraction	Es Cum. Oil Prod. in Hydro. P.V.	Ed Col. 4/Col. 3
0.904	566	1.37	0.904	0.653
1.805	971	2.35	1.445	0.587
2.71	1253	3.03	1.885	0.623



Table 27

Nine-Spot Flood 3-c: Calculation of Areal Sweep

Efficiency (Eas) and Displacement Efficiency (Ed)

Injection	Rate = 320	cc/hr S _{cw}	= 23.5%	C = 6.265
(1) Water Injected in Hydro. P.V.	(2) Area Measured cm2	(3) Eas Area/Unit Area Fraction	(4) Es Cum. Oil Prod. in Hydro. P.V.	(5) Ed Col. 4/Col. 3
0.904	684	1.655	0.904	0.546
1.805	1216	2.94	1.56	0.535
2.71	1680	4.07	2.04	0.503
4.52	2350	5.69	2.99	0.510
9.04	3050	7.39	4.80	0.651
13.55	3441	8.33	6.25	0.752
22.60	3680	8.91	7.75	0.873

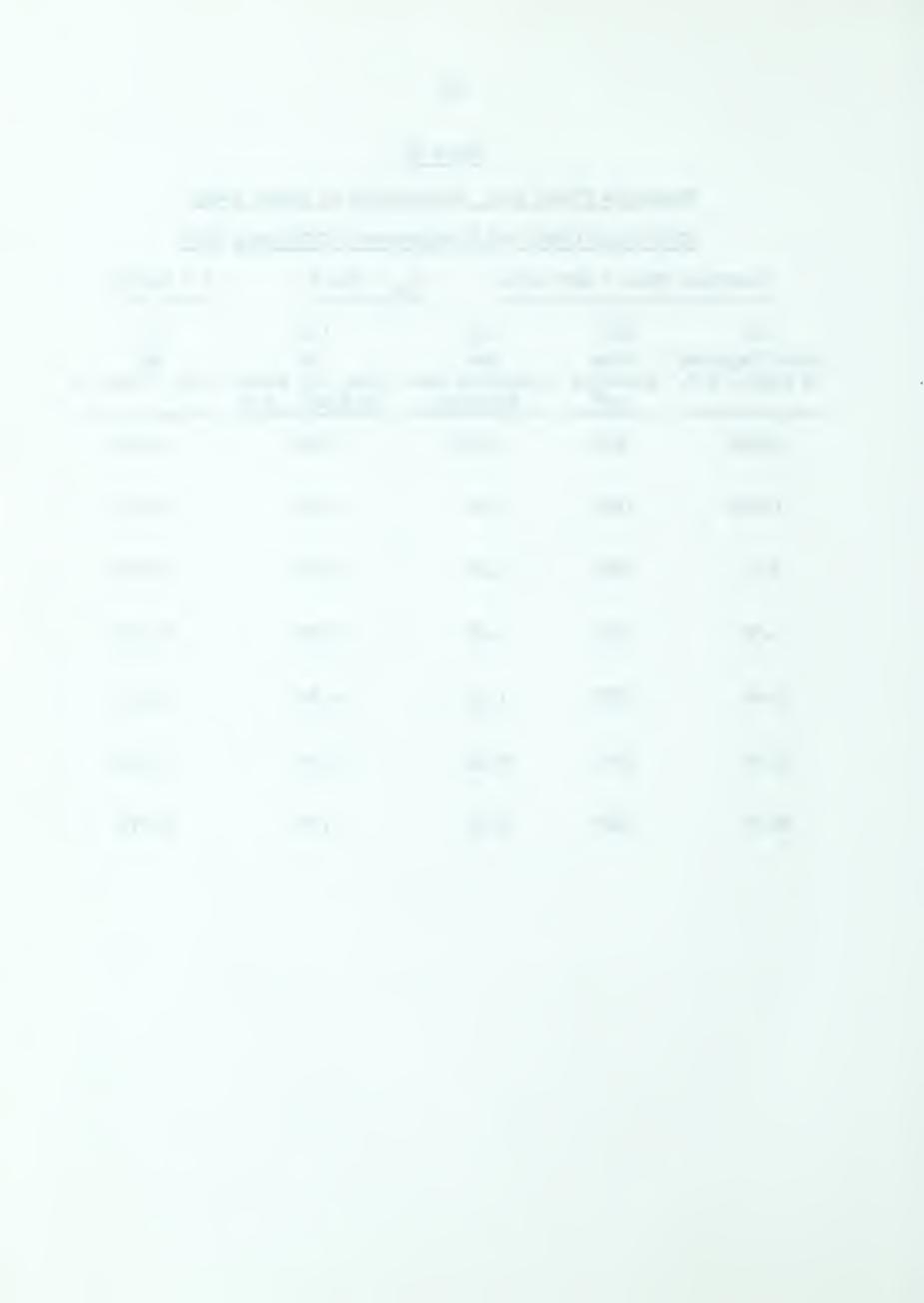


Table 28

Nine-Spot Flood 3-d: Calculation of Areal Sweep Efficiency (Eas),

Displacement Efficiency (Ed) and Mobility Ratio (M).

c = 6.265	(9) $M = \frac{K_{rw}^{\mu}}{K_{o}^{\mu}}$ K_{ro}^{μ}	6.42	6.75	29.9	479.9	6.18	2.47	5.30	5.78
ll D	(8) Krw	0,40	0.42	0.415	0.413	0.385	0.34	0.33	0.36
	(7) K ro	0.39	0.39	0.39	0.39	0.39	0.39	0.39	0.39
	(6) ***	0.811	0.831	0.825	0.823	0.799	0.759	0.750	0.779
$s_{cw} = 23.5\%$	(4) (5) Es Ed Oil Prod. Col. 4/Col. 3 dro. P.V.	0.754	0.780	0.770	0.768	0.736	0.685	0.673	0.710
	احرا	0.87	1.30	1.57	1.94	2.64	3.33	3.99	5.17
Injection Rate = 1680 cc/hr	Area Eas Measured Area/Unit Area Cum.	1.17	1.67	2.04	2,53	3.59	4,88	5.95	7.31
ion Rate =	(2) Area Measured	†8†	688	844	1045	1485	2015	2459	3020
Inject	(1) Water Inj. Hydro. P.V.	406.0	1,805	2.71	4,52	40.6	13.52	18.05	27.10

 $* \frac{s}{S_W} = S_{CW} + (1 - S_{CW}) Ed$



<u>Table 29</u>

<u>Nine-Spot Flood 3-e: Calculation of Areal Sweep</u>

<u>Efficiency (Eas) and Displacement Efficiency (Ed)</u>

(1)	(2)	(3)	(4)	(5)
Water Injected in Hydro. P.V.	Area Measured cm ²	Eas Area/Unit Area Fraction	Es Cum. Oil Prod. in Hydro. P.V.	Ed Col. 4/Col. 3
4.52	1130	2.76	1.84	0.675
9.04	1744	4.22	2.69	0.638
13.52	2135	5.17	3.375	0.655
18.05	2425	5.87	3.96	0.675

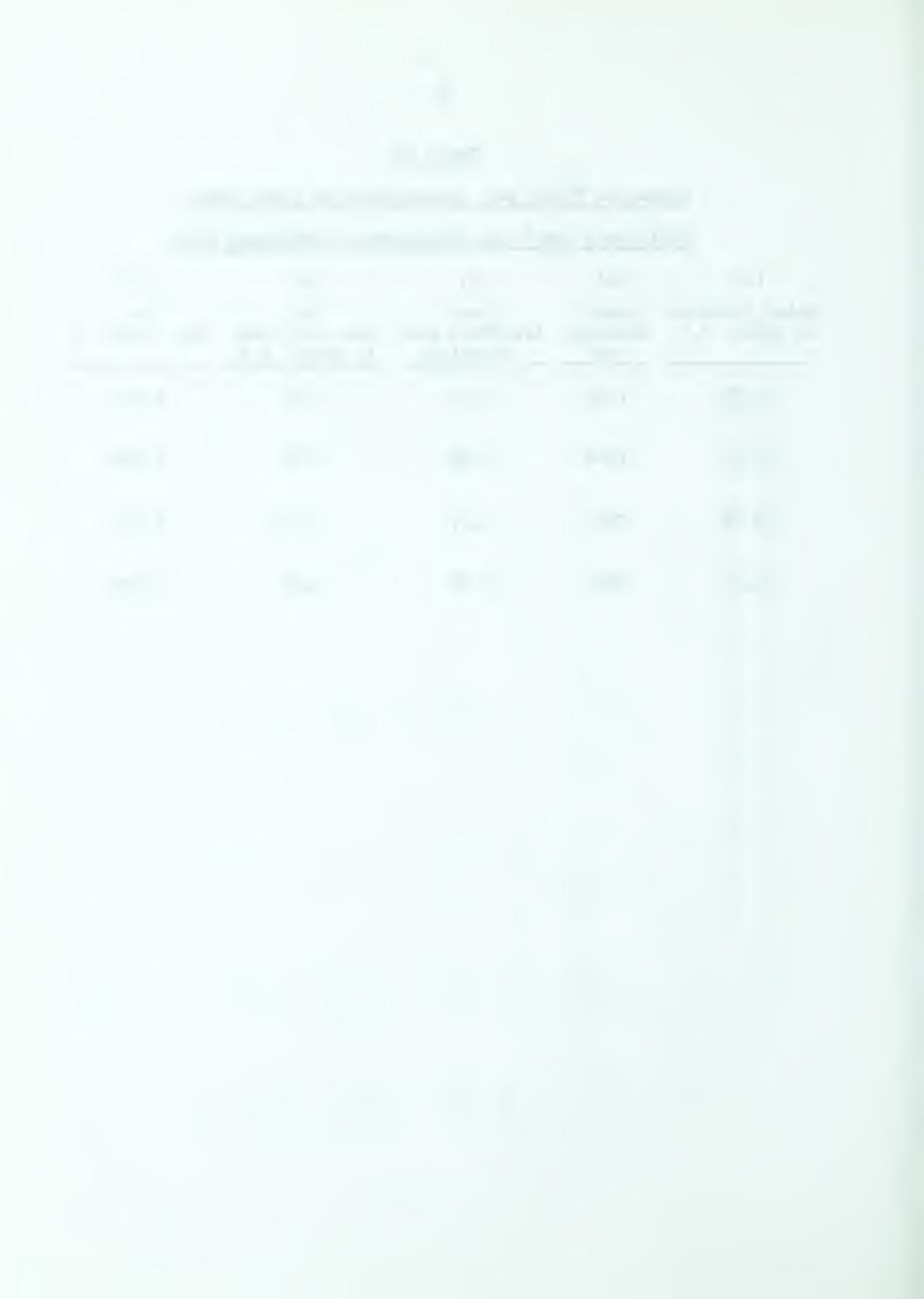
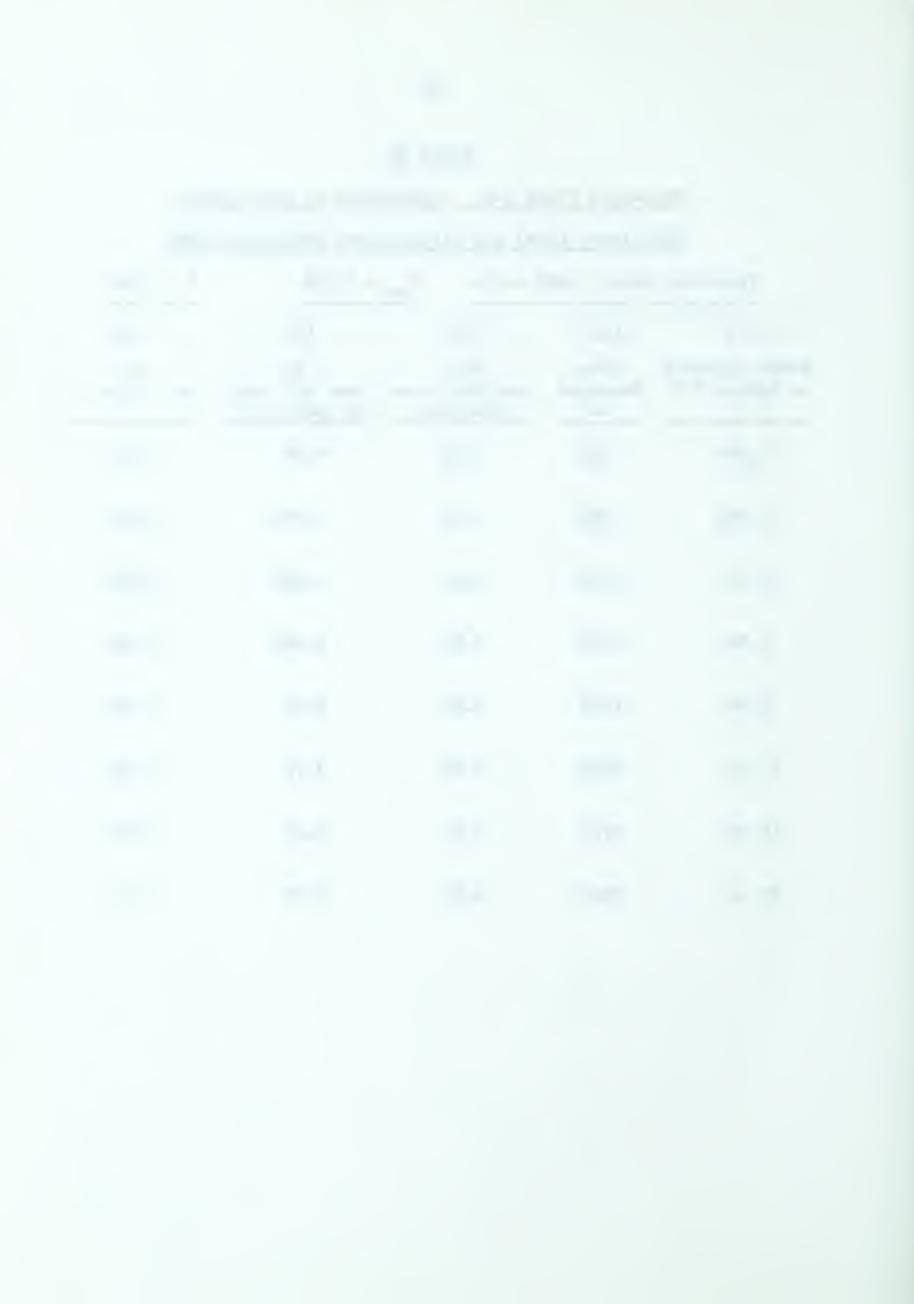


Table 30

Nine-Spot Flood 3-f: Calculation of Areal Sweep

Efficiency (Eas) and Displacement Efficiency (Ed)

Injection	Injection Rate = 1400 cc/hr $S_{cw} = 23.5\%$					
(1)	(2)	(3)	(4)	(5)		
Water Injected in Hydro. P.V.	Area Measured cm ²	Eas Area/Unit Area Fraction	Es Cum. Oil Prod. in Hydro. P.V.	Ed Col. 4/Col. 3		
0.904	596	1.28	0.88	0.612		
1.805	828	1.78	1.355	0.675		
2.71	953	2.04	1.625	0.706		
4.52	1238	2.65	2.062	0.691		
9.04	1809	3.87	2.87	0.682		
13.52	2365	5.06	3•77	0.660		
18.05	2755	5.90	4.43	0.666		
27.10	3200	6.85	5.52	0.715		



Table, 31

Nine-Spot Flood 4: Calculation of Areal Sweep Efficiency (Eas),

	(6)	$M = \frac{K_{TW}^{\mu\nu}}{K_{TO}^{\mu\nu}}$	6.05	26.91	26.97	7.08	10.45
	(8)	Krw	0.295	0.34	0.34	0.345	0.51
~ <u> </u>	(7)	Kro	0.39	0.39	0.39	0.39	0.39
atic (M	(<i>L</i>) (9)	₩ *	0.713 0.39	0.753 0.39 0.34	0.760	0.767 0.39 0.345	0.893 0.39 0.51
and Mobility R	(2)	Es Ed Oil Prod. Col. 4/Col. 3 ydro. P.V.	0.625	0.678	0,686	0.695	0,860
Displacement Efficiency (Ed) and Mobility Ratic (M).	(4)	Es Cum. Oil Prod. in Hydro. P.V.	0.858	1,185	1.580	1.975	2,70
	(3)	Area Eas Measured Area/Unit Area Cum. cm2 Fraction in Hy	1.38	1.76	2,30	2.83	3.15
	(2)	Area Measured cm ²	568	725	952	1170	1300
	(1)	Water Inj. Hydro. P.V.	4,06.0	1.805	4.52	40.6	22,50

 $\stackrel{*}{\overline{S}_W} = S_{CW} + (1 - S_{CW})Ed$

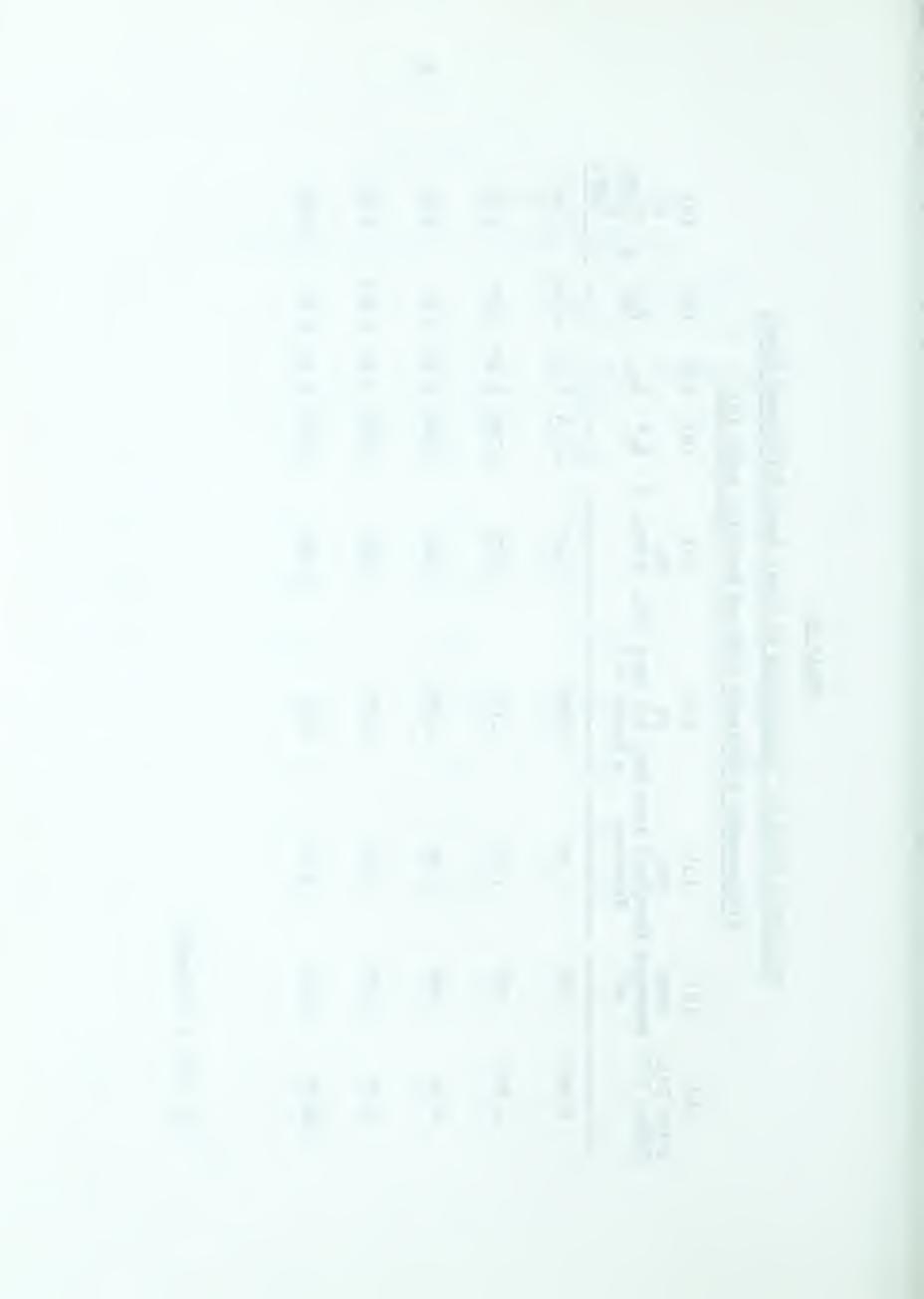


Table 32

Nine-Spot Flood 5: Calculation of Areal Sweep Efficiency (Eas),

Displacement Efficiency (Ed) and Mobility Ratio (M).

c = 12.405	$M = \frac{(9)}{\text{Krw}^{\text{M}}}$	9.75	11.20	10.92	10.92	10.35
0	(8) K _{rw}	0.33	0.38	0.37	0.37	0.35
	(7) Kro	0.42	0.42	0.42	0.42	0.42
	(9) * _M	0.745	0.793	0.782	0.787 0.42	0.765 0.42 0.35
$S_{cW} = 20.5\%$	(4) Es Oil Prod. Col. 4/Col. 3 /dro. P.V.	0,685	0.740	0.726	0.732	0.703
ທັ	• #	0,846	1.13	1.482	1.80	2.64
Injection Rate = 1680 cc/hr	(2) (3) Area Eas Measured Area/Unit Area Cum	1.24	1.53	2.04	2,46	3.75
ion Rate =	(2) Area Measured	510	, 631	842	1015	1550
Inject	(1) Water Inj. Hydro. P.V.	0.942	1.880	01.4	9,42	28.20

 $\overline{S}_{W} = S_{CW} + (1-S_{CW})Ed$



Table 33

Nine-Spot Flood 6: Calculation of Areal Sweep Efficiency (Eas),

Displacement Efficiency (Ed) and Mobility Ratio (M).

c = 0.5007	(6)	$M = \frac{K_{TW}^{UO}}{M}$	M.JOJ.	I I	1	0.75	0.568	0.675	1.022
) = D	(8)	Krw	1	1	1	99.0	0.50	0.595	006.0
	(7)	Kro	0.44	0.44	0.44	0.144	0.44	0.44	0.988 0.44
	(9)	* * *	1	ł	ł	0.943	0.884	0.923	0.988
$S_{cW} = 23.80\%$	(5)	Es Ed Oil Prod. Col. 4/Col. 3 dro. P.V.	3.3	1	1	0.925	0.850	0.901	0.986
ω	(†)		0.9825	1.67	2.14	2.85	4.125	5.02	6.425
Injection Rate = 1680 cc/hr	(3)	Area Eas Measured Area/Unit Area Cum. cm ² Fraction in H	0.84	1.53	2.06	3.08	4.84	5.56	6.52
	(2)	Area Measured	348	632	854	1270	1998	2295	2695
	(1)	Water Inj. Hydro. P.V.	.9825	1.963	2.95	4.92	9.825	14.72	29.50

 $* \frac{1}{S_{W}} = S_{CW} + (1 - S_{CW}) Ed$



Table 34

Calculation of Areal Sweep Efficiency (Eas) and Mobility Ratio (M)

at Breakthrough for all Floods

	* * * W		1.622	3.833	6.150	7.504	10.63	0.75
		nal						
	Eas Fraction	Diagonal Wells	2.33	2.16	1.74	1.40	1.001	1.552
	E E	Direct	1.14	0.980	0.922	1.01	0.80	0.962
	*	Diagonal	0.726	492.0	0.780	0.678	0.740	0.925
函	H	Direct	0.865	0,860	0.754	.0.625	0.685	0.925
Oil Rec. to B.T.	Diagonal Wells	154	146	120.5	48	63	117	
	Oil Rec.	Direct. Wells	9.68	74.6	9.19	95	46.7	72.5
	Hydro. P.V. of Unit	Area	91.0	88.6	88.6	98.6	85.0	81.5
	Flood No.		J-c	Ø	3-d	†	2	9

* Ed - From previous calculations

^{**} Eas - calculated from Oil Rec. = Ed x Eas x P.V. (Unit Area)

^{***} M - calculated as outlined previously

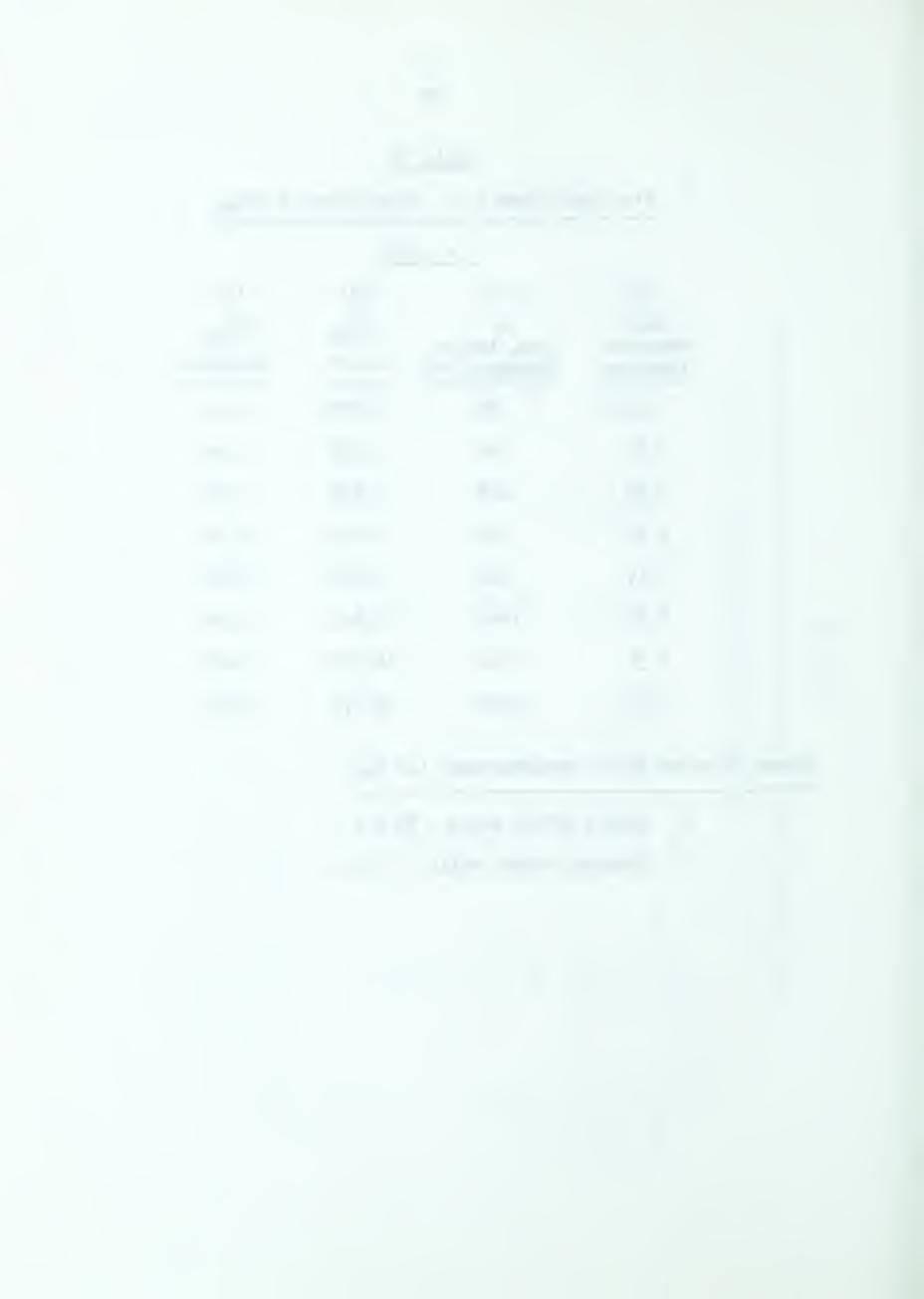


	C = 1.6	<u>579</u>	
(1) Eas Measured Fraction	(2) Q Cum. Water Injected (cc)	(3) Q/Q _{BT} Direct	(4) Q/Q _{BT} Diagonal
1.018	80	0.8925	0.46
2.07	160	1.685	0.92
2.98	240	2.678	1.38
4.22	7+00	4.463	2.30
6.17	800	8,925	4.60
6.86	1200	13.400	6.90
7.34	1600	16.850	9.20
7.84	2400	26.775	13.80

Volume Injected Before Breakthrough: (ie $Q_{\mbox{\footnotesize{BT}}}$)

^{1.} Direct offset wells - 89.6 cc.

^{2.} Diagonal offset wells - 174 cc.



 $\frac{\text{Table 36}}{\text{Nine-Spot Flood 2: Calculation of Q/Q}_{BT}}$

C = 3.52				
(1) Eas Measured Fraction	(2) Q Cum. Water Injected (cc)	(3) Q/Q _{BT} Direct	(4) Q/Q _{BT} Diagonal	
1.05	80	1.072	0.445	
2.03	160	2.144	0.89	
2.81	240	3.216	1.34	
3.94	400	5.360	2.23	
5.97	800	10.720	4.45	
7.10	1200	16.100	6.69	
7.62	1600	21.440	8.90	
8.40	2400	32.160	13.35	

Volume Injected Before Breakthrough (ie Q_{BT})

^{1.} Direct offset wells - 74.6 cc.

^{2.} Diagonal offset wells - 179.5 cc.

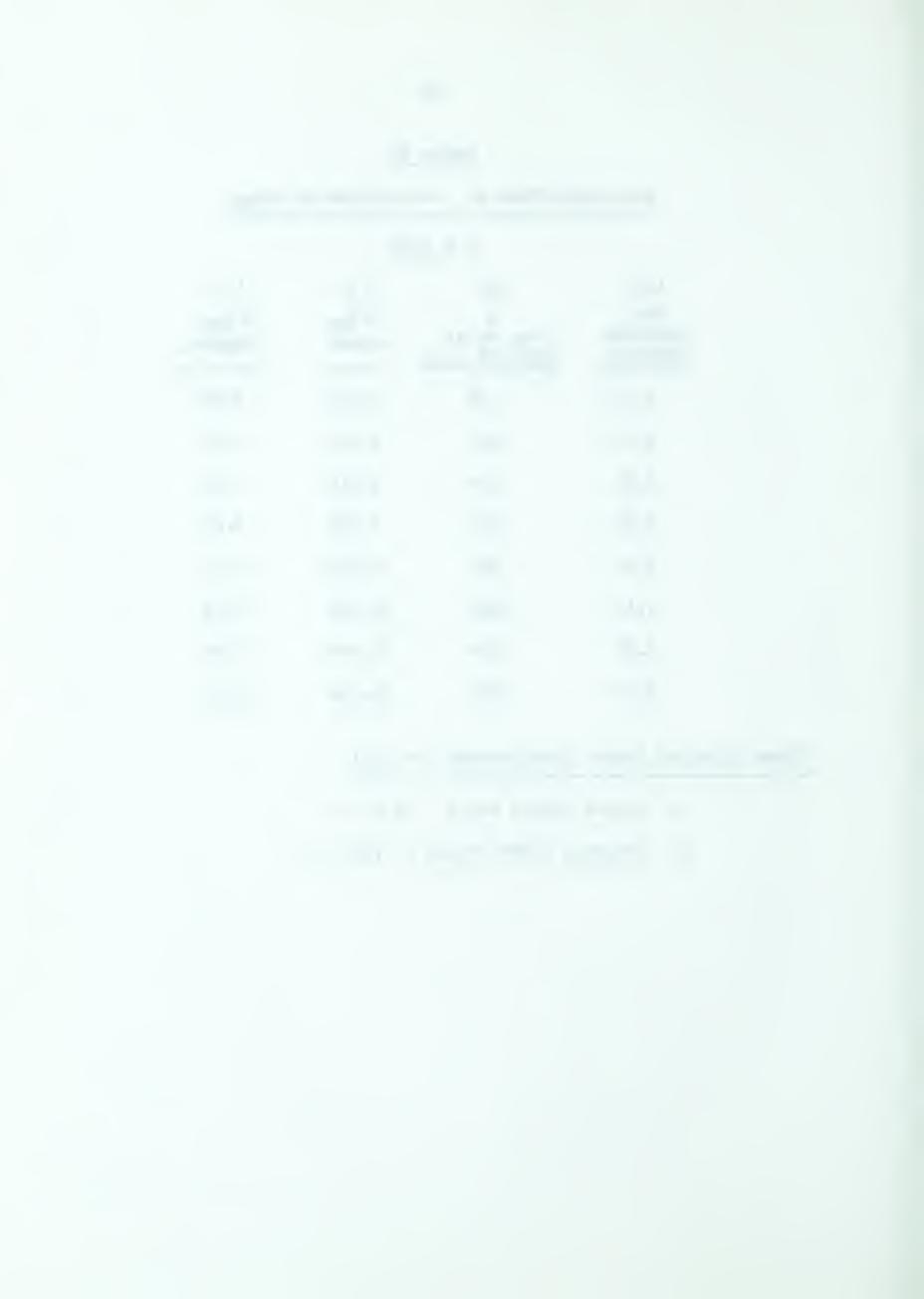


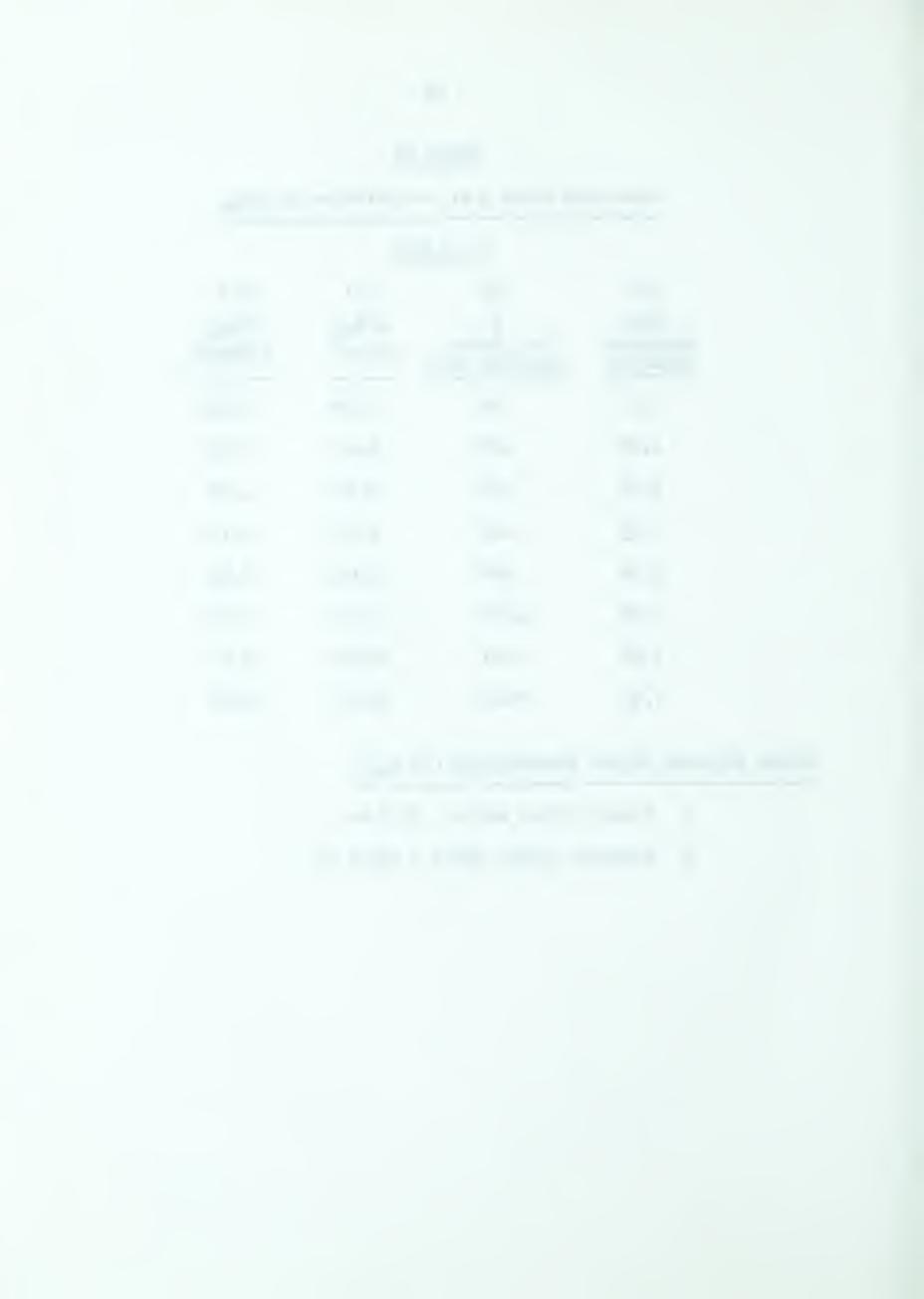
Table 37 Nine-Spot Flood 3-d: Calculation of $Q/Q_{\mbox{BT}}$

	c = 6.26	<u>65</u>	
(1)	(2)	(3)	(4)
Eas Measured Fraction	Q Cum. Water Injected (cc)	Q/Q _{BT} Direct	Q/Q _{BT} Diagonal
1.17	80	1.30	0.623
1.67	160	2.60	1.25
2.04	240	3.90	1.87
2.53	400	6.50	3.12
3.59	800	13.00	6.23
4.88	1200	19.50	9.35
5.95	1600	26.00	12.46
7.31	2400	39.00	18.69

Volume Injected Before Breakthrough (ie $Q_{\mbox{\footnotesize{BT}}}$)

^{1.} Direct offset wells - 61.6 cc.

^{2.} Diagonal offset wells - 128.5 cc.



	C = 8.00	<u>07</u>	
(1)	(2)	(3)	(4)
Eas Measured Fraction	Q Cum. Water Injected (cc)	Q/Q _{BT}	Q/Q _{BT}
1.38	80	1.43	0.816
1.755	160	2.86	1.632
2.30	400	7.15	4.08
2.83	800	14.30	8.16
3.15	2000	35.70	20.40

Volume Injected Before Breakthrough (ie $Q_{\mbox{\footnotesize{BT}}}$)

^{1.} Direct offset wells - 56 cc.

^{2.} Diagonal offset wells - 98 cc.



C = 12.405				
(1) Eas Measured Fraction	(2) Q Cum. Water Injected (cc)	(3) Q/Q _{BT} Direct	(4) Q/Q _{BT} Diagonal	
1.235	80	1.715	1.225	
1.53	160	3.43	2.45	
2.04	400	8.57	6.12	
2.46	800	17.15	12.25	
3.75	2400	51.50	36.70	

Volume Injected Before Breakthrough (ie $Q_{\overline{BT}}$)

^{1.} Direct offset wells - 46.7 cc.

^{2.} Diagonal offset wells - 65.4 cc.



 $$\operatorname{\underline{Table}}$\ 40$$ Nine-Spot Flood 6: Calculation of $\ensuremath{\mathrm{Q/Q_{BT}}}$

C = 0.5007				
(1)	(2)	(3)	(4)	
Eas Measured Fraction	Q Cum. Water Injected (cc)	Q/Q _{BT} Direct	Q/Q _{BT} Diagonal	
0.84	80	1.12	0.665	
1.53	160	2.21	1.33	
2.06	240	3.31	2.00	
3.08	400	5.52	3.34	
4.04	800	11.20	6.65	
5.56	1200	16.55	10.00	
6.52	2400	33.10	20.00	

Volume Injected Before Breakthrough (ie Q_{BT})

^{1.} Direct offset wells - 72.5 cc.

^{2.} Diagonal offset wells - 120.0 cc.

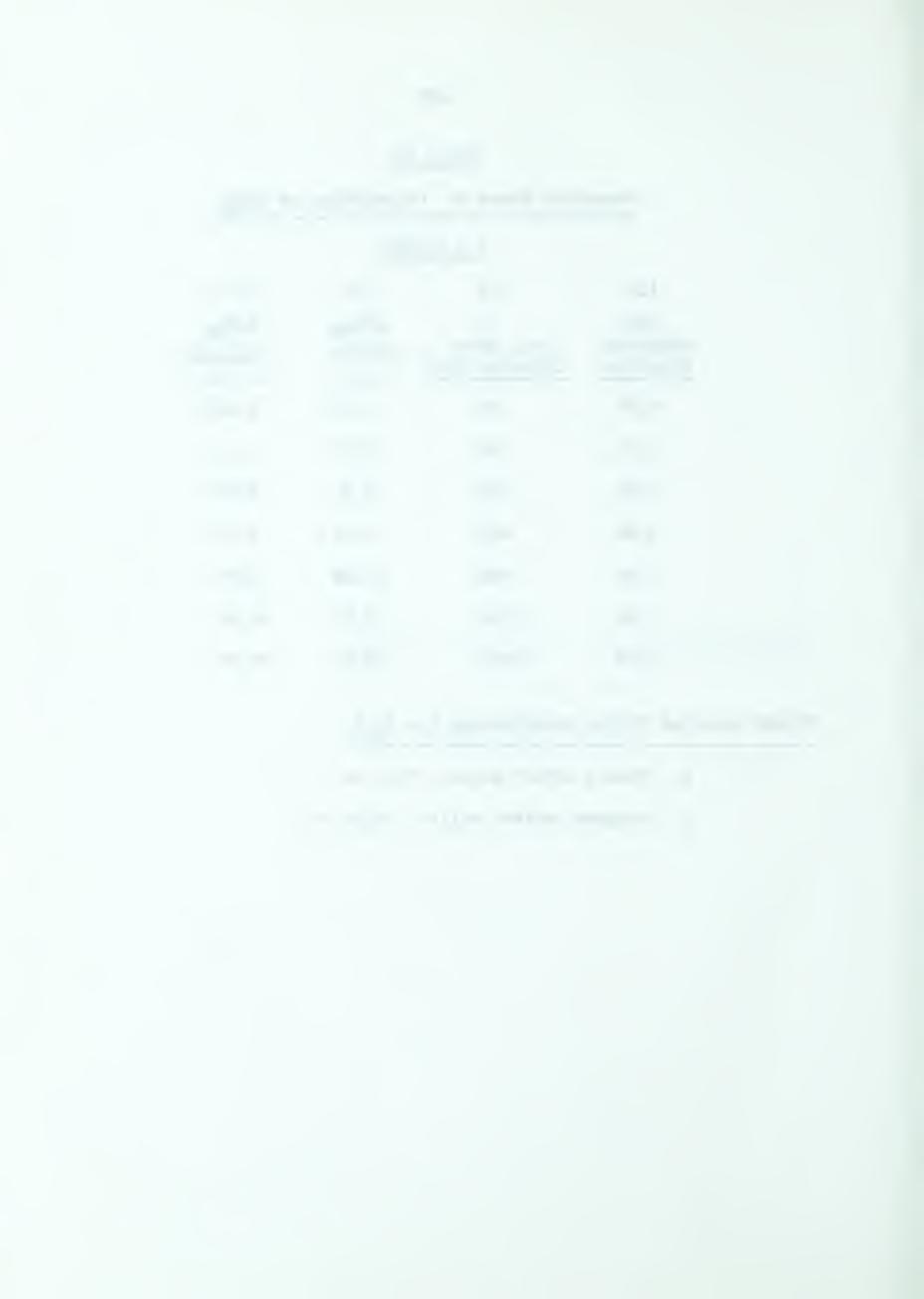


Table 41

Miscellaneous Data

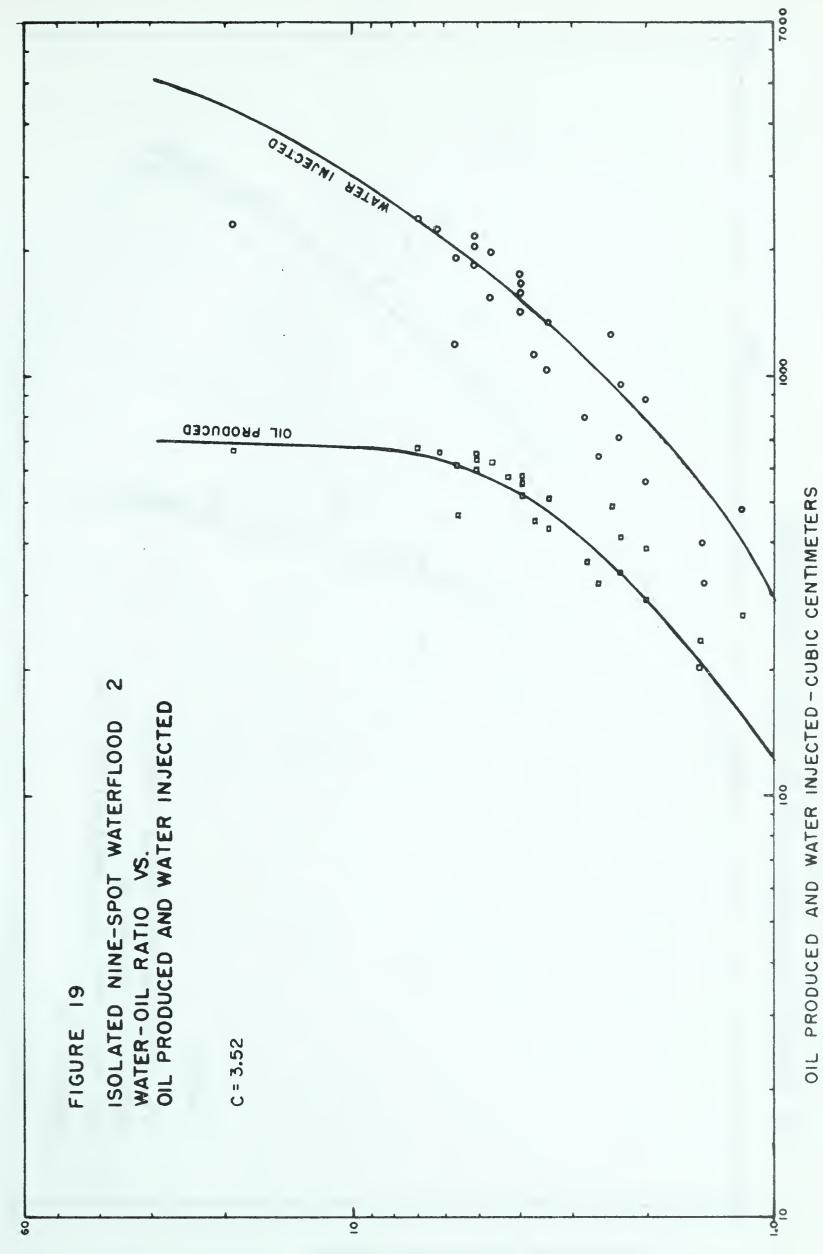
Fl	ood No.	Injection Rat	ce Model No.	S _{cw} %	Unit Area Hydrocarbon Pore Volume cc	μ _O cp	cp
	1	320	II	20.76	84.6	1.595	0.95
	1-a	560	II	19.69	85.8	1.595	0.95
	1 - b	1120	II	17.25	88.6	1.595	0.95
	1-c	1680	II	15.07	91.0	1.595	0.95
	1-d	2240	II	18.82	86.8	1.595	0.95
	1 - e	2800	II	20.25	85.2	1.595	0.95
	2	1120	I	23.50	88.6	3.342	0.95
	3-a	1120	I	23.50	88.6	5.592	0.95
	3-b	560	I	23.50	88.6	5.592	0.95
	3-c	320	I	23.50	88.6	5.592	0.95
	3-d	1680	I	23.50	88.6	5.592	0.95
	3 - e	2240	I	23.50	88.6	5.592	0.95
	3-f	1400	I	23.50	88.6	5.592	0.95
	4	1680	I	23.50	88.6	7.607	0.95
	5	1680	II	20.50	85.0	11.786	0.95
	6	1680	II	23.80	81.5	1.595	3.185



101,

OIL PRODUCED AND WATER INJECTED - CUBIC CENTIMETERS

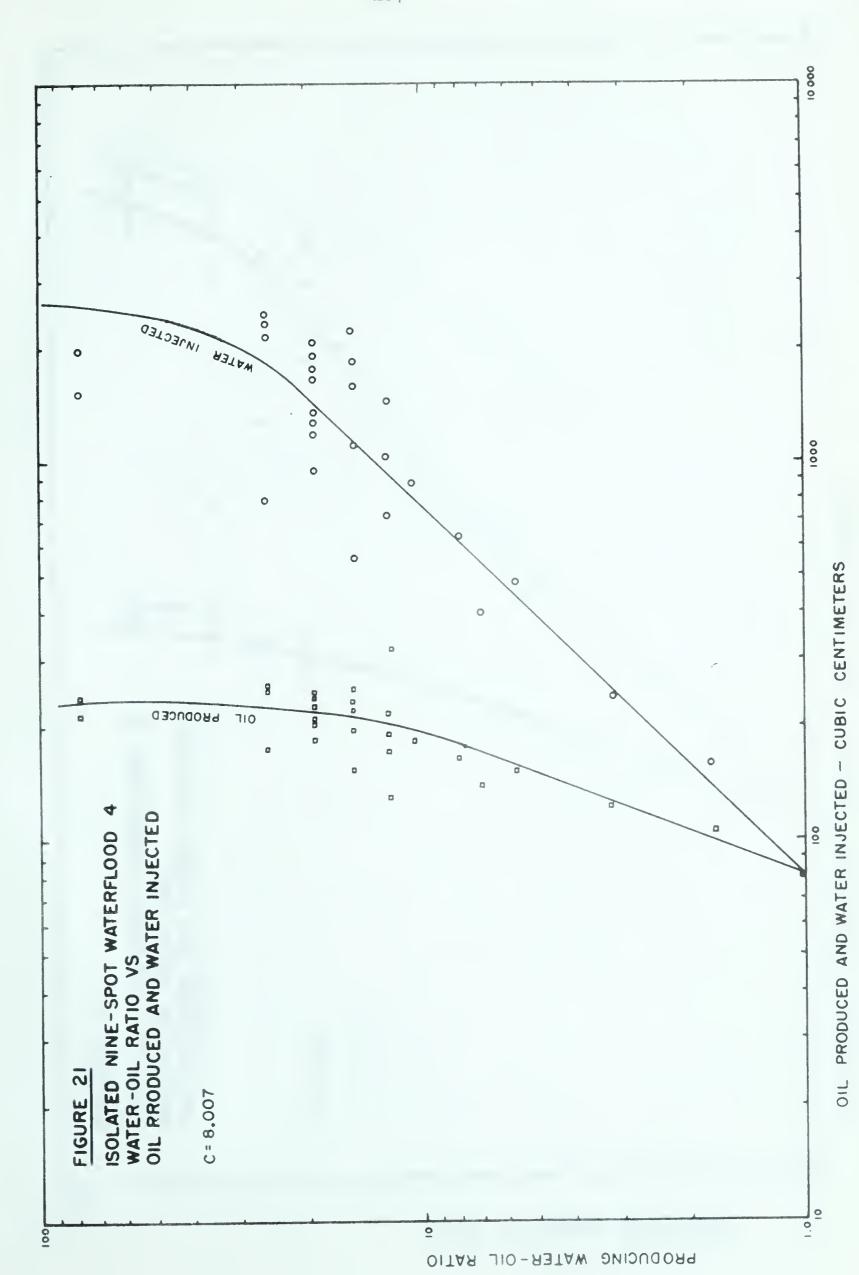






OIL PRODUCED AND WATER INJECTED - CUBIC CENTIMETERS







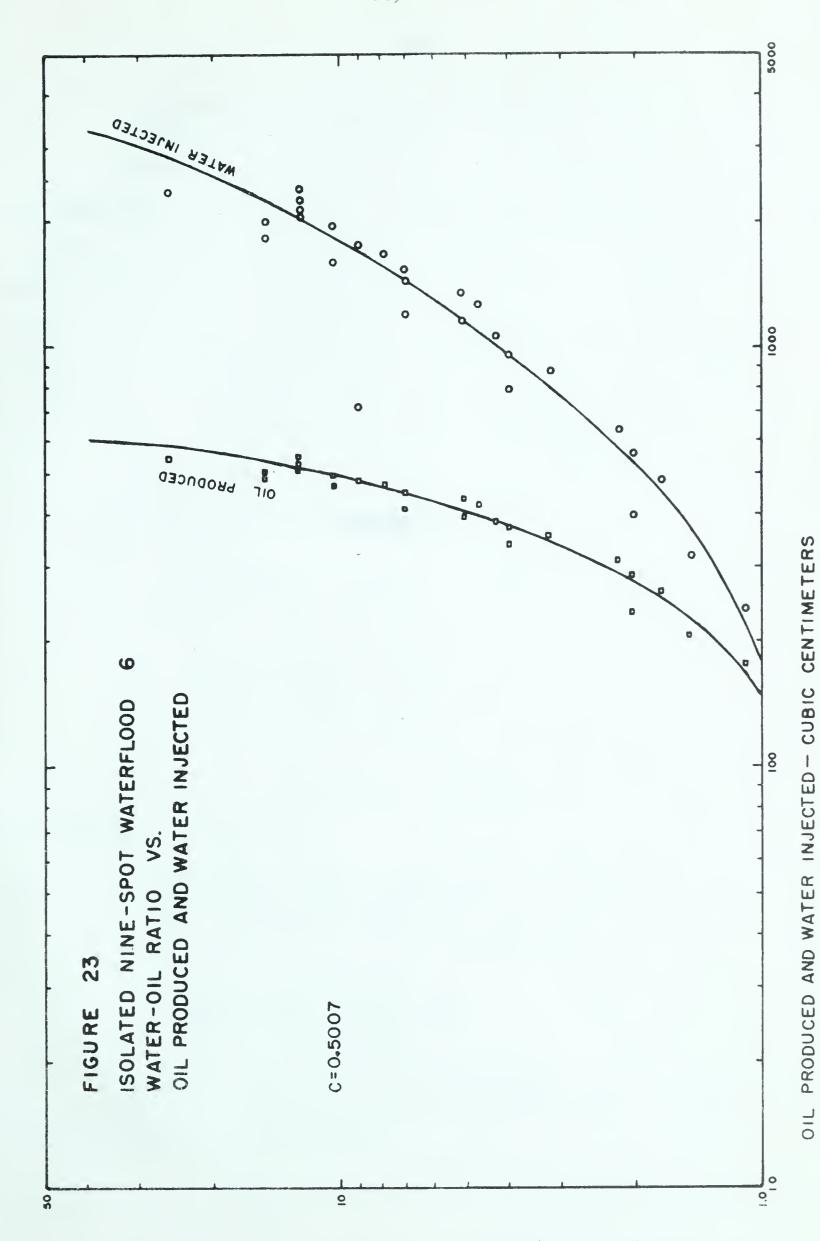
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OIL PRODUCED AND WATER INJECTED - CUBIC CENTIMETERS





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APPENDIX B



DERIVATION OF TWO-DIMENSIONAL SCALING COEFFICIENT

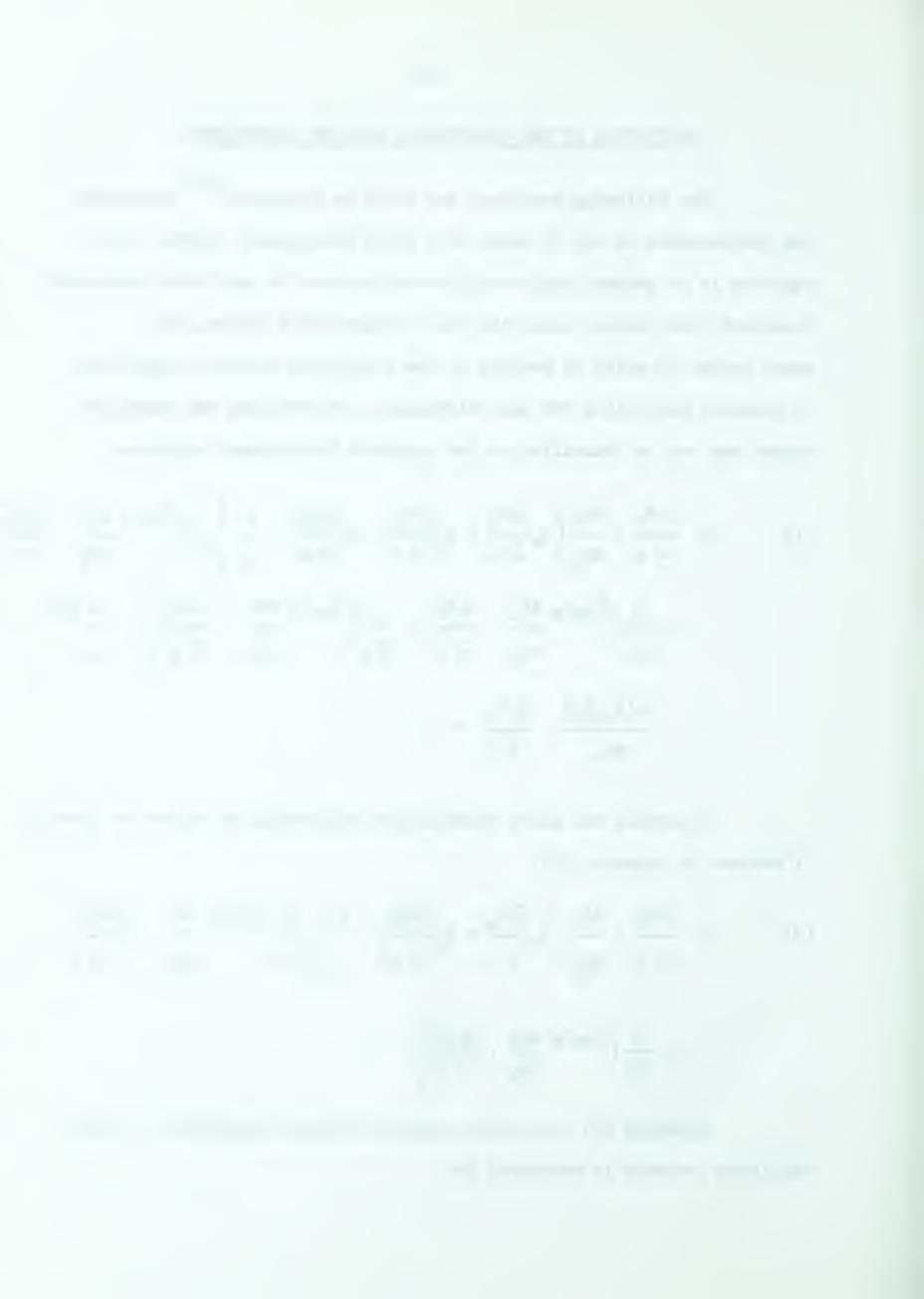
The following equation, set forth by Rapoport, (22) describes the displacement of oil by water in a three dimensional system. This equation is of general applicability with respect to any three dimensional transient flow process involving two incompressible fluids, the exact nature of which is defined by the prevailing boundary conditions. It accounts explicitly for the frictional, gravitational and capillary forces and can be classified as the complete displacement equation:

$$(1) \qquad \phi \frac{\partial S_{w}}{\partial t} + \frac{df_{w}}{dS_{w}} \left(q_{x} \frac{\partial S_{w}}{\partial x} + q_{y} \frac{\partial S_{w}}{\partial y} + q_{z} \frac{\partial S_{w}}{\partial z} \right) - \frac{K}{\mu_{o}} \left[\frac{\partial}{\partial x} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial S_{w}}{\partial x} \right) + \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial S_{w}}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial S_{w}}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial}{\partial z} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial z} \right) - \frac{K}{\mu_{o}} \frac{\partial$$

Accepting the above equation and neglecting the effect of gravity it reduces to equation (2):

(2)
$$\phi \frac{\partial S_{w}}{\partial t} + \frac{df_{w}}{dS_{w}} \left(q_{x} \frac{\partial S_{w}}{\partial x} + q_{y} \frac{\partial S_{w}}{\partial y} \right) - \frac{K}{\mu_{o}} \left[\frac{\partial}{\partial x} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial S_{w}}{\partial x} \right) + \frac{\partial}{\partial y} \left(K_{ro} f_{w} \frac{dP_{c}}{dS_{w}} \cdot \frac{\partial}{\partial x} \right) \right] = 0$$

Equation (2) represents complete flooding conditions in which capillary pressure is accounted for.



To obtain the dimensionless form of equation (2) the injection rate q will be considered a constant. Therefore only two variables remain to be normalized (ie: length and time). Defining

$$X = \frac{x}{L}$$
 and $Y = \frac{y}{L}$

 $X = \frac{X}{T}$ and $Y = \frac{Y}{T}$ - where X and Y represent distance expressed as a function of total length and width of the system.

$$T = \frac{tq}{L^2 \phi}$$

- where T is dimensionless time co-ordinate or cumulative injection in number of pore volumes.

Taking derivative of the above expression produces:

$$\frac{\partial X}{\partial S_W} = \frac{\partial X}{\partial S_W}$$
; $\frac{\partial Y}{\partial S_W} = \frac{\partial S_W}{\partial S_W}$ and $\frac{\partial T}{\partial S_W} = \frac{120}{12}$. $\frac{\partial S_W}{\partial S_W}$

substituting into equation (2) and using $c\mu_W$ for μ_O

(3)
$$\frac{\mathbf{q}}{\mathbf{L}^{2} \emptyset} \cdot \emptyset \frac{\partial \mathbf{S}_{\mathbf{W}}}{\partial \mathbf{T}} + \frac{1}{\mathbf{L}} \frac{\mathbf{df}_{\mathbf{W}}}{\mathbf{dS}_{\mathbf{W}}} \left(\mathbf{q}_{\mathbf{X}} \frac{\partial \mathbf{S}_{\mathbf{W}}}{\partial \mathbf{X}} + \mathbf{q}_{\mathbf{y}} \frac{\partial \mathbf{S}_{\mathbf{W}}}{\partial \mathbf{Y}} \right) - \frac{\mathbf{K}}{\mathbf{c} \mu_{\mathbf{W}}} \cdot \frac{1}{\mathbf{L}^{2}}$$

$$\left[\frac{\partial}{\partial \mathbf{X}} \left(\mathbf{K}_{\mathbf{r}0} \mathbf{f}_{\mathbf{W}} \frac{\mathbf{dP}_{\mathbf{C}}}{\mathbf{dS}_{\mathbf{W}}} \cdot \frac{\partial \mathbf{S}_{\mathbf{W}}}{\partial \mathbf{X}} \right) + \frac{\partial}{\partial \mathbf{Y}} \left(\mathbf{K}_{\mathbf{r}0} \mathbf{f}_{\mathbf{W}} \frac{\mathbf{dP}_{\mathbf{C}}}{\mathbf{dS}_{\mathbf{W}}} \cdot \frac{\partial \mathbf{S}_{\mathbf{W}}}{\partial \mathbf{Y}} \right) \right] = 0$$

Define (a) $\frac{q_x}{q/L} = Q_x$ and (b) $\frac{q_y}{q/L} = Q_y$ as velocity distribution functions (1) in the x and y direction respectively.

> - rate of water injection per unit sand thickness (cc/cm/sec)

 q_x, q_y - rate of flow per unit c.s.a. (cc/cm²/sec)

- principal dimension - size of nine-spot (cm)



Now introducing Leverett's J-function where

$$P_{C} = \frac{J(S_{W}) \sigma_{OW} \cos \theta}{\sqrt{K/\phi}}$$
 and taking derivative w.r.t. S_{W} get:

(c)
$$\frac{dP_{c}}{dS_{w}} = \frac{dJ(S_{w})}{dS_{w}} \cdot \frac{\sigma_{ow} \cos \theta \sqrt{\phi}}{\sqrt{K}}$$

Making the appropriate substitutions of (a), (b) and (c) into equation (3) results in:

$$(4) \qquad \frac{\partial S_{W}}{\partial T} + \frac{df_{W}}{dS_{W}} \left(Q_{X} \frac{\partial S_{W}}{\partial X} + Q_{Y} \frac{\partial S_{W}}{\partial Y} \right) - \frac{1}{C} \cdot \frac{\mathcal{O}_{OW} \cos \theta \sqrt{K\emptyset}}{q \mu_{W}} \cdot \frac{\partial S_{W}}{\partial Y}$$

$$= 0$$

$$\left[\frac{\partial}{\partial X} \left(K_{\text{ro}} f_{W} \frac{dJ(S_{W})}{dS_{W}} \cdot \frac{\partial S_{W}}{\partial X} \right) + \frac{\partial}{\partial Y} \left(K_{\text{ro}} f_{W} \frac{dJ(S_{W})}{dS_{W}} \cdot \frac{\partial S_{W}}{\partial Y} \right) \right] = 0$$

Equation (4) leads to the coefficient of
$$\frac{q~\mu_W}{\sigma_{ow}~\cos{\theta}\sqrt{\mathrm{K}~\phi}}$$

which can be used to correlate systems having only the same viscosity ratio, initial saturation distribution and pore size distribution. Thus this coefficient is known as the "capillary pressure coefficient" or scaling coefficient and was denoted by "C2" (proposed by Rapoport (23)).

If the appropriate units are used for "C2" it is a dimensionless coefficient. ie:

q -
$$cc/cm/sec (cm^2/sec)$$

$$\sigma_{ow}$$
 - dyne/cm (gram-cm/sec²-cm)



NOMENCLATURE

Subscripts o and w pertain to oil and water, respectively.

S_w - water saturation - dimensionless fraction (1)

x,y,z - spatial co-ordinates (cm)

t - time (sec)

L - principal dimension (cm)

 $Y = \frac{y}{t}$ $X = \frac{x}{t}$ - dimensionless space co-ordinates (1)

q - rate of water injection per unit sand thickness (cc/cm/sec)

porosity, dimensionless fraction (1)

K - absolute permeability (darcies)

σ - water-oil interfacial tension (dyne/cm)

 μ_{O}, μ_{W} - viscosity (cp)

c - oil-water viscosity ratio (1)

q_x,q_y - rate of flow per unit c.s.a. (cc/cm²/sec)

 $Q_{x}, Q_{y} = \frac{q_{xy}}{q/L}$ - velocity distribution function (1)

K_{ro}, K_{rw} - relative permeabilities dimensionless function of saturation (1)

T - dimensionless time (1)

 $\mathbf{F}_{\mathbf{W}} = \left[1 + \frac{K_{\mathbf{ro}}\mu_{\mathbf{W}}}{K_{\mathbf{rw}}\mu_{\mathbf{O}}}\right]^{-1}$ - dimensionless function of saturation

 $J(S_W) = \frac{P_C}{\sigma} \left(\frac{K}{\phi}\right)^{1/2}$ - capillary retention function, dimensionless function of saturation



θ	- water-oil-solid contact angle, dimensionless (1)
Pc	- capillary pressure, function of saturation (atm)
Δρ	- density difference between oil and water (gm/cm^3)
K_0, K_W	- effective permeability (darcy)
Eas	- areal sweep efficiency, dimensionless (1)
$\mathbf{E}_{\mathbf{d}}$	- displacement efficiency, dimensionless (1)
E	- total sweep efficiency, dimensionless (1)









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